POLITECNICO DI TORINO Repository ISTITUZIONALE

Comparison of Chloroaluminate Melts for Aluminum Graphite Dual-Ion Battery Application

Original Comparison of Chloroaluminate Melts for Aluminum Graphite Dual-Ion Battery Application / Elia, G. A.; Hoeppner, K.; Hahn, R In: BATTERIES & SUPERCAPS ISSN 2566-6223 ELETTRONICO 4:2(2021), pp. 368-373. [10.1002/batt.202000244]
Availability: This version is available at: 11583/2959176 since: 2022-03-23T10:51:25Z
Publisher: Wiley-VCH Verlag
Published DOI:10.1002/batt.202000244
Terms of use:
This article is made available under terms and conditions as specified in the corresponding bibliographic description in the repository
Publisher copyright
(Article begins on payt negal)

(Article begins on next page)





Comparison of Chloroaluminate Melts for Aluminum Graphite Dual-Ion Battery Application

Giuseppe Antonio Elia,*[a, c, d] Katrin Hoeppner, [a, b] and Robert Hahn[b]

Herein, we report a comparison of aluminum graphite dual-ion cells (AGDICs) electrochemical characteristics employing the conventional 1-ethyl-3-methylimidazolium chloride:aluminum trichloride (EMIMCI:AICI₃) electrolyte and two popular deep eutectic solvents (DESs), namely urea:AICI₃ and acetamide:AICI₃. The three electrolytes' characteristics have been evaluated in terms of Al-stripping deposition capability and cycling behavior

in AGDICs. The results evidence the EMIMCI:AICI₃'s Al-stripping deposition and rate capability in AGDICs superior characteristics addressed to the lower viscosity and higher conductivity with respect to the urea:AICI₃ and acetamide:AICI₃. On the other hand, the urea:AICI₃ guarantees a much higher columbic efficiency in AGDICs, thanks to the superior electrochemical window stability.

1. Introduction

Batteries and, in general, electrochemical storage systems are considered the key enabling technology to green energy economy transition. Lithium-ion battery (LIB) is the most mature technology, being the selected power source for electromobility, thanks to the elevated energy density and good cycle life. However, long-term, large-scale application of LIBs appears to be problematic due to the natural scarcity and limited production capacity of key materials containing Co and Ni.[1] Resources availability concerns pushed the research to explore alternative technologies based on abundant and widely available elements. Aluminum is one of the possible choices, having the advantages of being lightweight, low cost, and abundant (the most abundant metal in the Earth's crust).[2,3] Several secondary electrochemical cells using aluminum anode and chloroaluminate melt electrolytes have been proposed, [4-8] among them the most promising in terms of cycle life and rate capability are the aluminum graphite dual-ion batteries (AGDIBs). [3,4,9-12] AGDIBs are expected to achieve 65 Wh kg⁻¹, 92 Wh I⁻¹ in terms of energy density (values evaluated on active

materials only), guarantee a cycle life of more than 10000 cycles with an overall cost of 0.03 €/kWh/cycle. [3,11] To tackle the cost factor of AGDIBs, several groups proposed the use of a new class of ionic liquids called deep eutectic solvents (DESs), or ionic liquid analogs (ILAs), formed through a mixture of a strongly Lewis acid metal halide (AICI₃) and a Lewis basic ligand (urea, acetamide).[13-16] The substitution of the imidazolium cation of the conventional AlCl₃-ImidazoliumCl chloroaluminate with a cheaper and widely available chemical such as urea can substantially impact the system's overall cost. The retail price comparison of the three compounds indicates that EMIMCI is about ten times more expensive. Clearly, the retail price does not necessarily correspond to the product cost in high volume; however, it is an indication. The application of this class of electrolytes in AGDIBs is widely reported.[17-24] However, a clear comparison of DES electrolytes against the state of the art AICl₃-ImidazoliumCl chloroaluminate electrolyte is not available for AGDIB systems. For this reason, here we report a comparison of the electrochemical characteristics of AGDICs employing two of the most widely used DES electrolyte, the urea: AICI3 and the acetamide: AICI3 against the conventional 1ethyl-3-methylimidazolium chloride: aluminum trichloride (EMIMCI: AICI₃) system.

[a] Dr. G. A. Elia, K. Hoeppner Technische Universität Berlin Research Center of Microperipheric Technologies Gustav-Meyer-Allee 25, 13355 Berlin, Germany

[b] K. Hoeppner, Dr. R. Hahn
 Fraunhofer-Institut für Zuverlässigkeit und Mikrointegration
 Gustav-Meyer-Allee 25, 13355 Berlin, Germany

 [c] Dr. G. A. Elia

Helmholtz Institute Ulm (HIU)
Helmholtzstrasse 11, 89081 Ulm, Germany
[d] Dr. G. A. Elia
Karlsruhe Institute of Technology (KIT)
P.O. Box 3640, 76021 Karlsruhe, Germany

P.O. Box 3640, 76021 Karlsruhe, Germany
E-mail: elia@kit.edu

An invited contribution to a joint Special Collection between

© 2020 The Authors. Batteries & Supercaps published by Wiley-VCH GmbH. This is an open access article under the terms of the Creative Commons Attribution License, which permits use, distribution and reproduction in any medium, provided the original work is properly cited.

ChemElectroChem and Batteries & Supercaps dedicated to research Beyond

2. Results and Discussion

Figure 1 reports the molecular structure of the three solvents used in this study. Figure 2 reports the CV results comparison of the Al stripping deposition process on Ni substrate employing (a) EMIMCI:AlCl₃-1:1.5, (b) Acetamide:AlCl₃-1:1.5, and (c) Urea:AlCl₃-1:1.5 electrolytes. The highest current peak value, of almost 3 mA cm⁻², is recorded employing the EMIMCI:AlCl₃-1:1.5 (Figure 2a), while using Acetamide:AlCl₃-1:1.5 (Figure 2b), the current peak value is about 1.3 mA cm⁻². The lower Al stripping deposition current peak of 0.47 mA cm⁻² is recorded using the Urea:AlCl₃-1:1.5 electrolyte (Figure 2c). The difference in the peak current intensity between the three electrolyte systems can be ascribed to the electron transfer kinetics, and

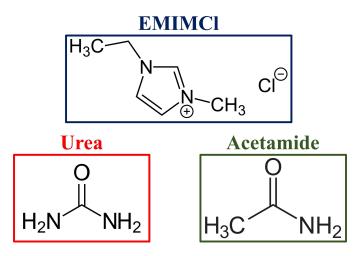


Figure 1. EMIMCI, Urea and Acetamide solvent molecular structure

active species concentrations, and diffusivity.^[25] Indeed the higher current peak of the EMIMCI:AICI3 relates well with its higher conductivity and lower viscosity (high active species diffusivity). However, the different ionic speciation influences on the stripping deposition kinetics cannot be excluded.[13-16] The EMIMCI: AICI₃ ions speciation includes AICI₄ and AI₂CI₇, while in the urea and acetamide compositions, we have the formation of $[AlCl_2 \cdot (ligand)_n]^+$ cations, suggested to be involved in the aluminum deposition process.[13-16] The Al deposition faradic efficiency, calculated for the second cycle, is 99.76% for EMIMCI:AICI₃, 91.62% for Urea:AICI₃ and 86.01% for Acetamide:AICI₃. The comparison suggests the EMIM-CI:AICI₃-1:1.5 electrolyte as the most efficient media for the AI stripping deposition process.

Figures 3(a-b) show the voltage vs. time curves of galvanostatic cycling tests performed on symmetrical Al/Al cells using the three investigated electrolytes, carried to evaluate the longterm stability of the Al/electrolyte interphase in dynamic condition. The Al/EMIMCI:AlCl₃/Al cell (blue curve) has the lowest polarization, thus agreeing with the results reported in Figure 2. All the systems are characterized by stable overall overvoltage upon cycling, suggesting a stable Al/electrolyte interphase and an excellent capability to sustain long term cycling. In particular, the Urea:AICl₃ system reveals a remarkable reduction of the cell overpotential during the first 5 days of measurement. This result is not in line with the CV reported in Figure 2c, where the current decreases upon cycling. The difference can be related to the different cell configuration and metal substrate used for the test. Figure 3c shows the comparison of the electrochemical stability of the three investigated electrolytes upon oxidation, evidencing the superior stability of the Urea:AlCl₃ system. The EMIMCI:AlCl₃ electrolyte also shows good stability, slightly inferior with respect to the Urea: AICI₃, while the Acetamide: AICI₃ shows the lowest stability, with a relevant current flow ($\geq 1 \,\mu\text{A}\,\text{cm}^{-2}$) starting already at 2.2 V vs. Al/Al³⁺.

The overall electrochemical characterization indicates the EMIMCI: AICI₃ as the most efficient media for the AI stripping deposition process; however, the Urea:AICI₃ electrolyte has better electrochemical anodic stability. The better characteristics of the EMIMCI: AICI3 electrolyte can be addressed to its higher ionic conductivity and lower viscosity in comparison with the urea and acetamide based electrolytes (Table 1).

AGDICs have been assembled to better overview the characteristics of the electrolytes. Figure 4 reports the galvanostatic cycling evaluation of the three investigated electrolytes in AGDIC, employing natural graphite (NG) electrodes with relevant loading, i.e., $\approx 5 \text{ mg cm}^{-2}$. Figure 4a reports the voltage signature of the first (dis-)charge cycle, revealing that the three systems are operating at a different average discharge voltage; 1.91 V for the EMIMCI: AICI₃, 1.73 V for the Acetamide:AICl₃ and 1.77 V for the Urea:AICl₃ (see Table 2). The higher discharge voltage of the cell using the EMIMCI: AICI₃ can be attributed to the electrolyte's higher conductivity and a lower viscosity. [5,17,19,22] Moreover, better Al stripping deposition properties of the EMIMCI: AICI₃ can lead to improved performance. However, the different ionic speciation of DESs and the presence of [AlCl₂(ligand)₂]⁺ species may influence the operating voltage. [17,22,26] The electrolyte composition has a relevant influence also in the AGDIC delivered capacity. The cell employing EMIMCI:AICI3 electrolyte shows the highest capacity (\approx 110 mAh g⁻¹) with respect to the cells using Acetamide:AlCl₃ (\approx 103 mAh g⁻¹) and Urea: AlCl₃ (\approx 91 mAh g⁻¹) (Table 2). In this case, the different ionic speciation of the three electrolyte systems can also influence the formation of the graphite intercalation compounds (GIC), lowering the delivered capacity.[17,22,26,27] The rate capability test reported in Figure 4b confirms the superior characteristics of the EMIMCI:AICI₃ in respect to the other compositions. The cell employing EMIMCI: AICI₃ electrolyte is only slightly affected by the current increase, while elevated current rate ($\geq 200 \text{ mAg}^{-1}$) substantially reduces the other cells' delivered capacity. The urea and acetamide based electrolytes maintain good performance at 200 mAg⁻¹, while at 1000 mAg⁻¹, the capacity drops to less than $45\,\%$ of the reference one for the urea, and almost to zero for the acetamide. The cell's better rate capability using the EMIMCI: AICI₃ can be attributed to the electrolyte's higher conductivity and lower viscosity (Table 1).^[5,17,19,22] Nonetheless, the urea composition shows the best columbic efficiency characteristic, as evidenced in Figure 4c, with values close to 100%.

Table 1. Viscosity, conductivity, and density of the EMIMCI:AICI₃ 1:1.5, Urea: AICI₃ 1:1.5, Acetamide: AICI₃ 1:1.5 electrolytes. Data from Refs. [5, 22, 31-33]. Electrolyte Viscosity Conductivity Density Ref. [MPa s] $[mS cm^{-1}]$ composition $[a m L^{-1}]$ 60°C 20°C 60°C Temperature 20°C 60°C 20°C **EMIMCI** 19.42 8.23 9.19 20.08 1.3408 1.3052 [31] AICI₂ 1:1.5 Urea 218 27 1.6 4.1 1.564 1.5921 [22, 32]AICI₃ 1:1.5 23 Acetamide 116 0.6 2.9 1.484 1.525 [5,33] AICI₂

www.batteries-supercaps.org

1:1.5



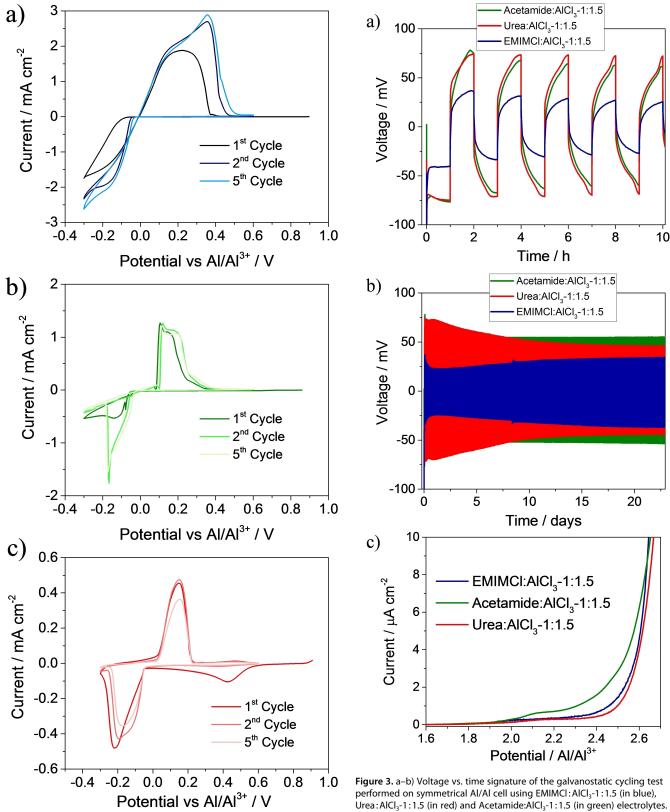


Figure 2. Cyclic voltammetry signatures obtained in a three-electrode configuration using Ni as working electrode and Al as counter and reference and employing a) EMIMCI:AlCl₃-1:1.5, b) Acetamide:AlCl₃-1:1.5, c) Ure-a:AlCl₃-1:1.5 electrolytes. Measurement obtained with a scan rate of 0.1 mV s⁻¹ at room T.

Figure 3. a–b) Voltage vs. time signature of the galvanostatic cycling test performed on symmetrical Al/Al cell using EMIMCl:AlCl₃-1:1.5 (in blue), Urea:AlCl₃-1:1.5 (in red) and Acetamide:AlCl₃-1:1.5 (in green) electrolytes. Measurement performed at 0.1 mAcm⁻² current, with a stripping deposition time of 1 h at room T. The test first 10 h are reported in (a), in (b) the full test performed for 24 days. c) Current vs. voltage signature of the linear sweep voltammetry test obtained in a three-electrode configuration using glassy carbon as working electrode and Al as counter and reference and employing EMIMCl:AlCl₃-1:1.5 (in blue), Urea:AlCl₃-1:1.5 (in red), and Acetamide:AlCl₃-1:1.5 (in green) electrolytes. Measurements obtained using a scan rate of 0.1 mVs⁻¹ at room T.



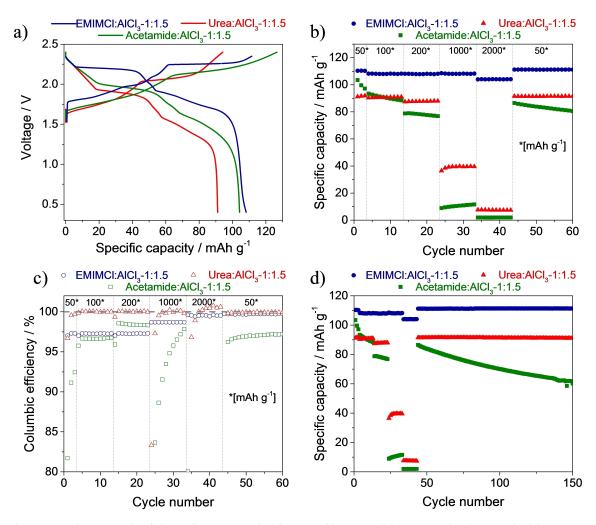


Figure 4. Galvanostatic cycling test results of Al/NG cells using EMIMCI: $AlCl_3$ -1:1.5 (in blue), Urea: $AlCl_3$ -1:1.5 (in red) and Acetamide: $AlCl_3$ -1:1.5 (in green) electrolytes. a) First cycle voltage profile. b) Capacity vs. cycle number behavior of the multi-rate test. c) Coulombic efficiency vs. cycle number behavior of the multi-rate test. d) Extended cycling behavior results. Measurements obtained cycling the cells within the 0.4–2.4 V voltage window end employing specific currents of 50, 100, 200, 1000, 2000 mA g⁻¹ at room T.

Table 2. Discharge energy, average discharge voltage, cell polarization, energy efficiency, columbic efficiency, and discharge capacity of the 1^{st} , 5^{th} , and 100^{th} cycle of the AGDICs using the three investigated electrolyte systems. The evaluation was obtained from the cycling test analysis reported in figure 3, for cycles performed at 50 mAg^{-1} current.

, ,	3						
Electrolyte composition	Cycle number	Discharge energy [Wh kg ⁻¹]	Average discharge voltage [V]	Polarization [V]	Energy efficiency [%]	Columbic efficiency [%]	Discharge capacity [mAhg ⁻¹]
EMIMCI	1 st	206.60	1.91	0.16	90.43	97.02	110.37
AICI ₃	5 th	205.56	1.90	0.30	86.39	97.30	108.23
	100 th	211.66	1.90	0.24	88.63	99.76	111.39
	1 st	157.72	1.73	0.24	85.32	96.70	91.20
Urea	5 th	152.94	1.69	0.27	86.14	100.06	90.49
AICI₃	100 th	151.33	1.66	0.30	84.88	99.99	91.35
Acetamide AICI ₃	1 st	184.83	1.77	0.26	71.88	81.70	103.49
	5 th	156.69	1.69	0.39	78.57	96.68	92.70
	100 th	103.05	1.47	0.71	66.11	97.84	70.08

The Acetamide:AICl₃ system reports the lowest columbic efficiency (Table 2). The columbic efficiency behavior of the AGDICs links well with the anodic electrochemical stability of the various electrolytes (Figure 3c). The superior Urea:AICl₃ stability against oxidation guarantees the best coulombic

efficiency in AGDICs; result in agreement with other reports. The Acetamide: AICl₃ system shows a columbic efficiency of about 96–97%, thus in line with this composition's lower anodic stability. The lower columbic efficiency of the Acetamide: AICl₃ is reflected in the poor capacity retention in



Al/NG cells, retaining less than the 60% after 150 cycles (Figure 4d). On the contrary, EMIMCI:AlCI₃ and Urea:AlCI₃ does not evidence a relevant capacity decay during the test's 150 cycles.

3. Conclusions

The overall comparison between the standard EMIMCI:AICI3 electrolyte and Urea: AICI₃ and Acetamide: AICI₃ DES electrolytes has been reported. The comparison evidences the superior characteristics of the EMIMCI:AICI₃ electrolyte as media for the Al stripping deposition process. Additionally, the standard EMIMCI: AICI₃ electrolyte reveals better characteristics in AG-DICs in terms of rate capability. The better features of the EMIMCI: AICI₃ over the Urea: AICI₃ and Acetamide: AICI₃ DES are mostly addressed to the former's lower viscosity and higher conductivity. However, AGDICs employing Urea:AICl₃ system have better columbic efficiency, around 99.9% for the urea with respect to the 97% of the EMIMCI:AICI₃. Indeed this is beneficial for practical cell application where the amount of electrolyte is limited, and a columbic efficiency of 97% is impractical. Additionally, the urea-based electrolyte is expected to be characterized by lower cost, considering that urea is a very common chemical widely produced and used as fertilizer. Nonetheless, the elevated viscosity and low conductivity result in a significant limitation in the AGDIB system's best characteristics, the outstanding rate capability. Improvements in the DES attributes need to be achieved to push the concept to practical application consideration.

Experimental Section

The electrolytes prepared in a 1: 1.5-mol ratio, 1-ethyl-3-methylimidazolium chloride:aluminum trichloride (EMIMCI):AICI₂, Urea:AICl₃, and Acetamide:AICl₃ are provided by IOLITEC. The water content of the electrolytes is lower than 100 ppm. The electrochemical measurements were performed using Teflon Swagelok® type T cells.^[6,28-30] All potentials quoted in this manuscript refer to the quasi reference Al/Al³⁺ electrode. The investigated electrolytes' capability to sustain the reversible aluminum stripping deposition process has been investigated by cyclic voltammetry (CV) of threeelectrode cells using Ni foil as a working electrode and Al as counter and reference. The test has been performed at a scan rate of 0.1 mV s $^{-1}$ within the -0.3 V and 0.6 V vs. Al/Al $^{3+}$ voltage window. The cycling stability of the aluminum metal in the various electrolytes was evaluated by continuous stripping/deposition tests on symmetrical Al/Al cells (Al 99.99% Alfa Aesar) employing a current of 0.1 mAcm⁻² and a stripping/deposition time of 1 h through a Maccor 4000 battery test system. The investigated electrolytes' anodic stability has been evaluated by linear sweep voltammetry (LSV) using a three-electrode cell comprising a glassy carbon working electrode and Al-metal as counter and reference. The measurements have been performed using a scan rate of 0.1 mV s⁻¹. The evaluation of the investigated electrolytes' electrochemical behavior in Al cells has been performed assembling AGDICs comprising natural graphite (NG) positive electrodes. The natural graphite powder (NG) was provided by PLANO GmbH. NG electrodes with a loading of about 5 mg cm⁻² have been employed for the electrochemical characterization. The detailed electrode

preparation procedure has been described in our previous paper.^[11] The cycling test of the Al/NG cells has been performed using a multi-rate procedure using 50, 100, 200, 1000, 2000 mAg⁻¹ within the 0.4–2.4 voltage window. The specific capacity and current are referred to the mass of the graphite.

Acknowledgments

The European Commission funded this research within the H2020 ALION project under contract 646286 and the German Federal Ministry of Education and Research in the AlSiBat project under contract 03SF0486 and the project ALIBATT under contract 03XP0128E. Open access funding enabled and organized by Projekt DEAL.

Conflict of Interest

The authors declare no conflict of interest.

- [1] D. Larcher, J.-M. Tarascon, Nat. Chem. 2015, 7, 19.
- [2] G. A. Elia, K. Marquardt, K. Hoeppner, S. Fantini, R. Lin, E. Knipping, W. Peters, J.-F. Drillet, S. Passerini, R. Hahn, Adv. Mater. 2016, 28, 7564.
- [3] G. A. Elia, K. V Kravchyk, M. V Kovalenko, J. Chacón, A. Holland, R. G. A. Wills, J. Power Sources 2021.
- [4] M.-C. Lin, M. Gong, B. Lu, Y. Wu, D.-Y. Wang, M. Guan, M. Angell, C. Chen, J. Yang, B.-J. Hwang, H. Dai, *Nature* 2015, 520, 324.
- [5] J. Lampkin, H. Li, L. Furness, R. Raccichini, N. Garcia-Araez, ChemSuschem 2020, 13, 3514.
- [6] W. Wang, Z. Cao, G. A. Elia, Y. Wu, W. Wahyudi, E. Abou-Hamad, A.-H. Emwas, L. Cavallo, L.-J. Li, J. Ming, ACS Energy Lett. 2018, 3, 2899.
- [7] J. Bitenc, N. Lindahl, A. Vizintin, M. E. Abdelhamid, R. Dominko, P. Johansson, Energy Storage Mater. 2020, 24, 379.
- [8] M. Walter, K. V. Kravchyk, C. Böfer, R. Widmer, M. V. Kovalenko, Adv. Mater. 2018, 30, 1.
- [9] S. Wang, K. V. Kravchyk, A. N. Filippin, U. Müller, A. N. Tiwari, S. Buecheler, M. I. Bodnarchuk, M. V. Kovalenko, Adv. Sci. 2018, 5, 1700712.
- [10] S. Wang, K. V. Kravchyk, F. Krumeich, M. V. Kovalenko, ACS Appl. Mater. Interfaces 2017, 9, 28478.
- [11] G. A. Elia, N. A. Kyeremateng, K. Marquardt, R. Hahn, *Batteries Supercaps* **2019**, *2*, 83.
- [12] G. A. Elia, G. Greco, P. H. Kamm, F. García-Moreno, S. Raoux, R. Hahn, Adv. Funct. Mater. 2020, 2003913.
- [13] H. M. A. Abood, A. P. Abbott, A. D. Ballantyne, K. S. Ryder, Chem. Commun. 2011, 47, 3523.
- [14] Y. Fang, K. Yoshii, X. Jiang, X.-G. Sun, T. Tsuda, N. Mehio, S. Dai, Electrochim. Acta 2015, 160, 82.
- [15] G. Pulletikurthi, B. Bödecker, A. Borodin, B. Weidenfeller, F. Endres, Prog. Nat. Sci. Mater. Int. 2015, 25, 603.
- [16] Y. Fang, X. Jiang, X.-G. Sun, S. Dai, Chem. Commun. 2015, 51, 13286.
- [17] M. Angell, C.-J. Pan, Y. Rong, C. Yuan, M.-C. Lin, B.-J. Hwang, H. Dai, Proc. Natl. Acad. Sci. 2017, 114, 834.
- [18] H. Jiao, C. Wang, J. Tu, D. Tian, S. Jiao, Chem. Commun. 2017, 53, 2331.
- [19] J. Li, J. Tu, H. Jiao, C. Wang, S. Jiao, J. Electrochem. Soc. 2017, 164, A3093.
- [20] Y. Bian, Y. Li, Z. Yu, H. Chen, K. Du, C. Qiu, G. Zhang, Z. Lv, M.-C. Lin, ChemElectroChem 2018, 5, 3607.
- [21] C. Xu, J. Li, H. Chen, J. Zhang, ChemNanoMat 2019, 5, 1367.
- [22] M. Angell, G. Zhu, M. Lin, Y. Rong, H. Dai, Adv. Funct. Mater. 2020, 30, 1901928.
- [23] H. Xu, T. Bai, H. Chen, F. Guo, J. Xi, T. Huang, S. Cai, X. Chu, J. Ling, W. Gao, Z. Xu, C. Gao, Energy Storage Mater. 2019, 17, 38.
- [24] C. Li, J. Patra, J. Li, P. C. Rath, M. H. Lin, J. K. Chang, *Adv. Funct. Mater.* **2020**, *30*, 1.
- [25] L. R. Bard, J. Allen and Faulkner, *Electrochemical Methods: Fundamentals and Applications.*; Wiley, **2001**.



- [26] H. M. A. Abood, A. P. Abbott, A. D. Ballantyne, K. S. Ryder, Chem. Commun. 2011, 47, 3523.
- [27] G. A. Elia, G. Greco, P. H. Kamm, F. García-Moreno, S. Raoux, R. Hahn, Adv. Funct. Mater. 2020, 2003913.
- [28] G. A. Elia, I. Hasa, G. Greco, T. Diemant, K. Marquardt, K. Hoeppner, R. J. Behm, A. Hoell, S. Passerini, R. Hahn, J. Mater. Chem. A 2017, 5, 9682.
- [29] G. Greco, D. Tatchev, A. Hoell, M. Krumrey, S. Raoux, R. Hahn, G. A. Elia, J. Mater. Chem. A 2018, 6, 22673.
- [30] G. A. Elia, J.-B. Ducros, D. Sotta, V. Delhorbe, A. Brun, K. Marquardt, R. Hahn, ACS Appl. Mater. Interfaces 2017, 9, 38381.
- [31] Y. Zheng, K. Dong, Q. Wang, J. Zhang, X. Lu, J. Chem. Eng. Data 2013, 58. 32.
- [32] C. Liu, W. Chen, Z. Wu, B. Gao, X. Hu, Z. Shi, Z. Wang, J. Mol. Liq. 2017, 247, 57
- [33] P. Hu, W. Jiang, L. Zhong, S. Zhou, Chin. J. Chem. Eng. 2019, 27, 144.

Manuscript received: October 13, 2020 Revised manuscript received: November 6, 2020 Accepted manuscript online: November 6, 2020 Version of record online: November 23, 2020