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An Integrated Device for the Solar-Driven Electrochemical Conversion of CO₂ to CO

- 3 Adriano Sacco,* Roberto Speranza, Umberto Savino, Juqin Zeng, M. Amin Farkhondehfal,
- 4 Andrea Lamberti,* Angelica Chiodoni, and Candido F. Pirri



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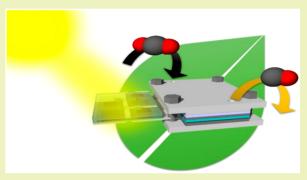
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Supporting Information

5 **ABSTRACT:** The conversion of carbon dioxide into value-added 6 products using sunlight, also called artificial photosynthesis, represents a 7 remarkable and sustainable approach to store solar energy, transforming 8 it into chemical energy. There are mainly two strategies to carry out this 9 process: the photocatalytic reduction of carbon dioxide (CO_2) or the 10 photovoltaic-powered electrochemical reduction of CO_2 . Herein, we 11 focus on the latter route, i.e., the development of a device coupling a 12 solar cell to an electrochemical reactor for CO_2 reduction. Different 13 literature works demonstrated the possibility to achieve such a coupling, 14 but no evidence of a real integration between the two systems has been 15 given up to now. In this work, we present an integrated device 16 constituted by a dye-sensitized solar module (based on a mesoporous



titanium dioxide photoanode) and an electrochemical cell (based on a copper—tin cathode). The integration of the two systems is accomplished through a common platinum-based electrode, which acts either as a cathode for the photovoltaic module and as an anode for the electrochemical reactor. The integrated system was characterized by a stable current of 3.6 mA under continuous solar irradiation, enabling the production of 80 mmol of carbon monoxide per day, with a solar-to-fuel efficiency equal to 0.97%.

21 KEYWORDS: Artificial photosynthesis, Integrated device, Dye-sensitized solar cells, Photovoltaic module, CO₂ reduction reaction,

22 Electrochemical conversion

23 INTRODUCTION

24 Artificial photosynthesis, i.e., the conversion of solar energy to 25 chemical energy, mimicking the plants' process of natural 26 photosynthesis, has attracted a lot of interest in the scientific 27 community. Essentially, two types of artificial photosynthesis 28 processes are studied by scientists, namely, photocatalytic 29 water splitting, i.e., the conversion of water into oxygen and 30 hydrogen, and the solar-driven carbon dioxide reduction 31 reaction (CO_2RR), i.e., the conversion of CO_2 to carbon-32 based value-added products. The latter is of particular interest 33 because it would allow attaining a triple goal: (1) storing the excess energy coming from the Sun that is not put in the 35 electric grid, (2) reduction of atmospheric CO_2 , i.e., the major 36 greenhouse gas, which can be used as a raw material, and (3) 37 production of valuable chemicals.

Apart from systems employing photoelectrodes, $^{7-9}$ there are 39 different examples in the literature dealing with solar-driven 40 CO $_2$ electroreduction obtained by coupling a photovoltaic 41 (PV) device with an electrochemical cell (EC). $^{10-17}$ As an 42 example, Kauffman et al. used a commercial 6 V Si solar 43 module to power a two-chamber electrochemical reactor with a 44 gold (Au) cathode and a platinum (Pt) anode which was able 45 to produce more than 400 L/(g $_{\rm Au}$ h) of carbon monoxide 46 (CO) with a selectivity of about 96%. 10 Schreier and co-

workers employed three series-connected perovskite solar cells 47 to power a single-chamber electrolyzer with a Au cathode 11 48 and studied a triple-junction GaInP/GaInAs/Ge PV device 49 coupled with a dual-chamber EC based on a SnO2-coated CuO 50 cathode and anode. 12 In both cases, a selectivity toward CO 51 larger than 80% was reached, with solar-to-CO efficiencies 52 equal to 6.5% and 13.4% for perovskite- and triple-junction- 53 based systems, respectively. A 1.4% solar-to-formate efficiency 54 was obtained by White et al. employing a poly-Si solar panel 55 and a three-cell electrolyzer stack composed of indium (In)- 56 based cathodes and iridium oxide (IrO₂)-based anodes. 13 57 Moreover, hydrocarbons and oxygenates can be produced by 58 solar-driven ${\rm CO_2}$ reduction, 16 with a conversion efficiency 59larger than 5% by using a III–V/Si tandem PV cell and a two- $_{\rm 60}$ chamber reactor with a nanostructured copper-silver (Cu- 61 Ag) bimetallic cathode and IrO₂ anode. A lower solar-to- 62 hydrocarbons efficiency equal to 2.3% was obtained by a low- 63

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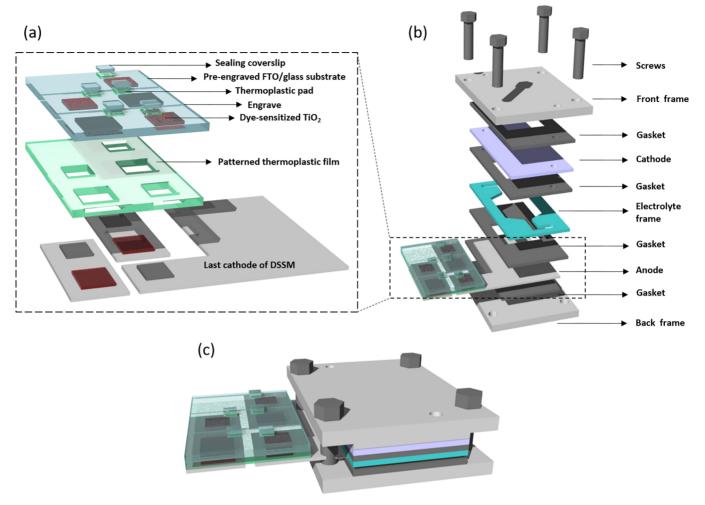


Figure 1. Scheme of the integrated PV-EC system: (a) solar module, (b) electrochemical reactor, and (c) integrated device.

cost all-Earth-abundant system, composed of a perovskite PV minimodule and a two-chamber EC based on nanostructured CuO for both the cathode and anode. In all of the above-mentioned and other works, 14,15,18,19 the PV cell/module is coupled to the electrochemical reactor through electrical wire connections, since the solar cell is external or attached to the electrolyzer. In this sense, we can speak of connected systems, that no real integrated systems (i.e., with shared electrodes between the PV and the EC) have been proposed in the literature so far.

In this work, we present, for the first time, an integrated device for the solar-driven electrochemical conversion of CO₂ to value-added products. To carry out the integration, we concluded that a third-generation PV technology, namely, dyesensitized solar cell (DSSC), makes use of Pt as the cathodic electrode; at the same time, Pt is widely used as the anode material in EC for CO₂ conversion. With these premises, we fabricated an integrated system in which the Pt electrode is shared between the dye-sensitized solar module (DSSM) and the electrochemical reactor, acting at the same time both as cathode for the solar device and as anode for the EC. The integrated system was able to carry out the unassisted CO₂ reduction to CO under simulated solar irradiation for more than 3 h.

■ RESULTS AND DISCUSSION

The PV module is composed of five series-connected DSSCs, 89 similar to our previous work,²¹ with an increase in the cell 90 number to five in order to achieve an operating voltage higher 91 than 2.5 V. The module employed a nanocrystalline TiO₂ 92 photoanode, Ru-based sensitizer, iodide/tri-iodide electrolyte, 93 and Pt cathode. Two different current collectors were selected 94 for module fabrication: transparent conductive substrate as the 95 front side (top of the device) and titanium foils as the back 96 side (bottom of the device). Details of the fabrication 97 procedure are reported in the Supporting Information. The 98 dimension of the last cathode of the cell series was chosen in 99 order to overpass the PV module footprint and act as the 100 anode for the EC. Concerning the EC, a single-chamber 101 configuration was employed, in which no membrane was used 102 to separate the anode and the cathode, as shown in Figure 1. 103 fl This configuration has been adopted in order to reduce the 104 total cell overpotential by eliminating the proton exchange 105 membrane (see Supporting Information for details). 11,22 A 106 Cu-Sn electrocatalyst recently proposed by our group, 23,24 107 characterized by a good selectivity toward CO, was used as the 108 cathodic material. The Cu-Sn cathode was prepared through a 109 cost-efficient electrodeposition route, as detailed in the 110 Supporting Information. The already mentioned Ti-supported 111 Pt was employed as the anode. A CO₂-saturated 0.1 M 112 KHCO₃ aqueous solution was chosen as the electrolyte. The 113

114 volume of the electrolyte was 7 mL, with a 3 mL headspace. A 115 scheme of the integrated device is depicted in Figure 1.

The performance of the two components of the system was 117 first investigated individually. Figure 2 shows the current—

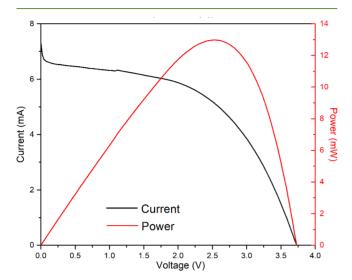


Figure 2. Current–voltage characteristic of the five-cell PV module under 1 sun illumination (left axis) and corresponding produced power (right axis).

118 voltage characteristic of the PV model acquired under AM1.5G 119 illumination. By comparing the curve in Figure 2 with the data 120 reported for our previously published DSSM,²¹ it can be 121 observed that the addition of the fifth solar cell in the PV 122 module leads to a boost of the voltage with respect to the four-123 cell module, with an open circuit value of 3.73 V, i.e., almost a 124 1 V increase. This improvement cannot be simply justified with 125 the addition of a cell since it is larger than the open circuit 126 voltage (V_{oc}) of a traditional DSSC (based on the combination 127 of TiO₂, Ru-based dye and I⁻/I₃⁻). Therefore, it must be 128 ascribed to the different architectures of the two DSSM. 129 Indeed, in the present study, Ti foils are used as current 130 collectors on one side of the module to allow integration with 131 the electrochemical reactor for CO₂ reduction, while gluorine-132 doped tin oxide (FTO)-coated glasses were used by Scalia et 133 al.²¹ This variation induces two main effects: (i) the reduction 134 of the series resistance (accounting for the transport resistance 135 of the substrate) due to a higher conductivity of Ti with 136 respect to FTO and (ii) the in situ formation of a TiO2 137 blocking layer on the Ti surface during the thermal treatment 138 for photoanode preparation. While the former can influence 139 the photogenerated current, the latter can be considered as the 140 main reason responsible for the increased $V_{
m oc}$ of the present 141 DSSM. In fact, it is well known that the introduction of a very 142 thin TiO₂ layer between the current collector and the 143 nanostructured photoanode film allows for preventing electron 144 recombination with a positive effect on the $V_{\rm oc}$. For what concerns the other parameters, both the PV modules exhibit 146 similar currents (short circuit value of about 7 mA) and fill 147 factors (0.48), thus leading to an enhanced photoconversion 148 efficiency of 2.68% for the novel five-cell device. It is worth 149 noting that a maximum power of 13 mW is produced by the 150 DSSM at 2.54 V and that power larger than 10 mW can be 151 obtained in the wide voltage range of 1.7-3.2 V.

The performance of the EC was assessed through 1 h $\rm CO_2$ ls3 electrolysis tests at different voltages. A micro-gas chromato-

graph (μ GC) was used for the online measurements of the 154 gaseous products, and a high-performance liquid chromato- 155 graph (HPLC) was used for the analysis of the liquid products 156 at the end of each test. During the experiments, a constant 157 CO₂ flow of 10 mL/min was maintained in order to saturate 158 the electrolyte and to carry the gaseous products to the μ GC. 159 Figure 3 reports the faradaic efficiency (FE) for the different 160 f3

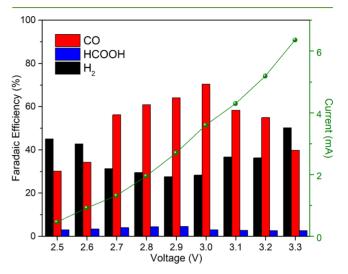


Figure 3. Faradaic efficiencies for CO, HCOOH, and H₂ formation in EC at various applied voltages during 1 h electrolysis (left axis) and corresponding measured currents (right axis).

reaction products as a function of the applied voltage. Only 161 CO and H_2 were detected as gaseous products, while just 162 formic acid (HCOOH) was identified as the liquid product. 163 With the exception of low ($\leq 2.6~\rm V$) and high ($\geq 3.3~\rm V$) 164 voltages, the CO₂RR outperforms the competing hydrogen 165 evolution reaction, thus confirming the goodness of our Cu-166 based electrocatalyst. 23,24 A maximum FE for CO production 167 of about 73% was obtained at 3.0 V, where the total measured 168 current is 3.6 mA (corresponding to a cathodic current density 169 of 6.4 mA/cm²). By comparing this data with those of the PV 170 module, an optimal operating point at 3.0 V can be envisaged 171 for the integrated system since the solar device produces a 172 similar current of 3.7 mA at this voltage.

Figure 4a shows the measured current-voltage characteristic 174 f4 of the PV module under 1 sun illumination superimposed to 175 that of the EC. As anticipated above, the theoretical operating 176 point, given by the intersection of the two curves, can be found 177 at 3.0 V. At this potential, the power produced by the PV 178 module is 11.5 mW, and the partial current (density) for CO 179 production is equal to 2.6 mA (4.7 mA/cm²). The electrolysis 180 experiment on the integrated PV-EC system was carried out 181 under 1 sun illumination for more than 3 h, during which the 182 produced gases were measured by μ GC (the liquid products 183 were measured after the test through HPLC). The results of 184 this measurement are reported in Figure 4b and c. The 185 integrated device is characterized by a constant voltage of 3.00 186 ± 0.06 V for all the period of investigation and a by 187 corresponding stable current density equal to 6.5 ± 0.4 mA/ 188 cm² after 30 min of operation (Figure 4b). It is worth noting 189 that such a stability is in line with or even better than those 190 reported for nonintegrated PV–EC systems. 7,14,18 In the initial 191 phase of the electrolysis, the decrease in the current density is 192 associated with the reduction of oxide species in the Cu-Sn 193

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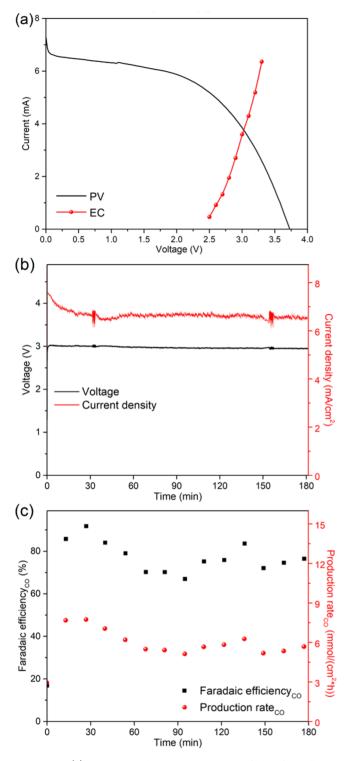


Figure 4. (a) Current—voltage characteristic of the five-cell PV module under 1 sun illumination and of the EC. (b) Voltage (left axis) and current density (right axis) during a 3 h test of the integrated PV—EC system under 1 sun illumination. (c) FE (left axis) and production rate (right axis) for CO during a 3 h test of the integrated PV—EC system under 1 sun illumination.

194 cathode. ^{23,24} In accordance with the analysis conducted on the 195 bare EC, only CO and HCOOH were detected as CO₂RR 196 products, with average FE values equal to about 78% and 2%, 197 respectively. The FE for CO is plotted as a function of the 198 electrolysis time in Figure 4c. It can be observed that it remains

stable during 3 h of operation, thus proving that sunlight and 199 $\rm CO_2$ can be efficiently and continuously converted by our 200 integrated device, similarly to PV–EC coupled systems present 201 in the literature. A CO production rate of about 80 202 mmol/day (considering 24 h of continuous operation) was 203 obtained along the 3 h test.

The obtained data was employed to calculate the solar-to- 205 CO efficiency $\eta_{\rm STC}$ of our integrated system, according to the 206 formula

$$\eta_{\rm STC} = \frac{E_{\rm CO_2/CO}^0 \cdot J \cdot \rm FE_{\rm CO}}{W_{\rm sol}} \tag{1)}_{208}$$

where $E^0_{\rm CO_2/CO}$ is the standard cell potential when the EC $_{209}$ conducts the CO $_2$ RR to CO (equal to 1.34 V), J is the current $_{210}$ density of the PV module, FE $_{\rm CO}$ is the faradaic efficiency for $_{211}$ CO, and $W_{\rm sol}$ is the solar irradiance. $_{11}$ A solar-to-CO efficiency $_{212}$ equal to 0.79% is found for our integrated PV—EC system. $_{213}$ This efficiency can be further increased considering also H $_2$ as $_{214}$ a secondary product (for example, for the production of $_{215}$ syngas), $_{27}$ leading to a total solar-to-fuel efficiency of 0.97%. $_{216}$ The obtained values are comparable to the efficiencies $_{217}$ presented in the literature for coupled PV—EC systems. $_{14}$ $_{218}$ Better results have been also reported. $_{11,17,18}$ However, it has $_{219}$ to be highlighted that the performance of our integrated PV— $_{220}$ EC system can be improved since different aspects can be $_{221}$ optimized:

- (i) An additional PV cell can be added to the module in 223 order to enlarge the voltage window of the module and 224 shift the operating point in a region of higher cell 225 efficiency.
- (ii) Adapting the active area of the PV module to the 227 electrocatalyst one can be done in order to match the 228 two currents.

These aspects have already been taken into consideration in 230 a new work which is in progress in our lab. Nevertheless, the 231 present work demonstrates the feasibility of an integrated PV— 232 EC system that enables the solar-driven electrochemical 233 conversion of CO₂.

CONCLUSION

An integrated system composed of a third-generation PV 236 module and an EC for the electroreduction of CO_2 under solar 237 illumination has been presented here. The PV module is based 238 on a series of five DSSCs, while the EC is based on a Cu-Sn 239 electrocatalyst. The integration of the two devices has been 240 achieved through a common Pt-based electrode, which works 241 both as a cathode for the PV module and as an anode for the 242 EC.

A stable voltage of 3 V has been obtained from the 244 integrated system under 1 sun illumination for 3 h, during 245 which CO production with a FE of 78% was achieved as a 246 result of the unassisted $\rm CO_2RR$. This represents the first 247 integrated artificial photosynthesis device for the solar-driven 248 electrochemical conversion of $\rm CO_2$. This system is currently 249 under optimization in our laboratory in order to improve the 250 overall device efficiency.

ASSOCIATED CONTENT

Supporting Information

The Supporting Information is available free of charge at 254 https://pubs.acs.org/doi/10.1021/acssuschemeng.0c02088.

Experimental section, measurements of membrane overpotential, scheme of DSSM, scheme of EC, and pictures of the integrated PV–EC device (PDF)

259 AUTHOR INFORMATION

260 Corresponding Authors

Adriano Sacco — Center for Sustainable Future Technologies @
Polito, Istituto Italiano di Tecnologia, 10144 Torino, Italy;
orcid.org/0000-0002-9229-2113; Phone: +39 011
5091912; Email: adriano.sacco@iit.it; Fax: +39 011
5091901

Andrea Lamberti — Center for Sustainable Future Technologies

@Polito, Istituto Italiano di Tecnologia, 10144 Torino, Italy;

Applied Science and Technology Department, Politecnico di

Torino, Corso Duca degli Abruzzi, 10129 Torino, Italy;

orcid.org/0000-0003-4100-9661; Phone: +39 011

0907394; Email: andrea.lamberti@polito.it; Fax: +39 011

0907399

273 Authors

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288

289

Roberto Speranza — Center for Sustainable Future Technologies @Polito, Istituto Italiano di Tecnologia, 10144 Torino, Italy; Applied Science and Technology Department, Politecnico di Torino, Corso Duca degli Abruzzi, 10129 Torino, Italy

Umberto Savino — Center for Sustainable Future Technologies

@Polito, Istituto Italiano di Tecnologia, 10144 Torino, Italy;
Applied Science and Technology Department, Politecnico di
Torino, Corso Duca degli Abruzzi, 10129 Torino, Italy

Jugin Zeng — Center for Sustainable Future Technologies @

Juqin Zeng – Center for Sustainable Future Technologies @ Polito, Istituto Italiano di Tecnologia, 10144 Torino, Italy

M. Amin Farkhondehfal – Center for Sustainable Future Technologies @Polito, Istituto Italiano di Tecnologia, 10144 Torino, Italy

Angelica Chiodoni – Center for Sustainable Future Technologies @Polito, Istituto Italiano di Tecnologia, 10144 Torino, Italy

Candido F. Pirri – Center for Sustainable Future Technologies
 @Polito, Istituto Italiano di Tecnologia, 10144 Torino, Italy;
 Applied Science and Technology Department, Politecnico di
 Torino, Corso Duca degli Abruzzi, 10129 Torino, Italy

294 Complete contact information is available at:

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296 Author Contributions

297 The manuscript was written through contributions of all 298 authors. All authors have given approval to the final version of 299 the manuscript.

300 Notes

301 The authors declare no competing financial interest.

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