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Human health risk assessment for nanoparticle-contaminated aquifer systems

Original Human health risk assessment for nanoparticle-contaminated aquifer systems / Tosco, T.; Sethi, R In: ENVIRONMENTAL POLLUTION ISSN 0269-7491 239:(2018), pp. 242-252. [10.1016/j.envpol.2018.03.041]
Availability: This version is available at: 11583/2784354 since: 2020-01-23T10:53:10Z
Publisher: Elsevier Ltd
Published DOI:10.1016/j.envpol.2018.03.041
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Human health risk assessment for aquifer systems at nanoparticle-contaminated sites Submitted to **Environmental Pollution** Revised manuscript - March 2018 Tiziana Tosco $^{(1)}$ , Rajandrea Sethi $^{(1)}$ \* (1) DIATI – Dipartimento di Ingegneria dell'Ambiente, del Territorio e delle Infrastrutture – Politecnico di Torino, C.so Duca degli Abruzzi 24, 10129 Torino, Italy \* Corresponding Author: phone +39 (011) 564 7735; e-mail: rajandrea.sethi@polito.it 

31 Abstract

32 Nanosized particles (NPs), such as TiO<sub>2</sub>, Silver, graphene NPs, nanoscale zero-valent iron, carbon 33 nanotubes, etc., are increasingly used in industrial processes, and releases at production plants and 34 from landfills are likely scenarios for the next years. As a consequence, appropriate procedures and 35 tools to quantify the risks for human health associated to these releases are needed. 36 The tiered approach of the standard ASTM procedure (ASTM-E2081-00) is today the most applied 37 for human health risk assessment at sites contaminated by chemical substances, but it cannot be 38 directly applied to nanoparticles: NP transport along migration pathways follows mechanisms 39 significantly different from those of chemicals; moreover, and also toxicity indicators (namely, reference dose and slope factor) are NP-specific. In this work a risk assessment approach modified 40 41 for NPs is proposed, with a specific application at Tier 2 to migration in groundwater. The standard 42 ASTM equations are modified to include NP-specific transport mechanisms. NPs in natural 43 environments are typically characterized by a heterogeneous set of NPs having different size, shape, 44 coating, etc. (all properties having a significant impact on both mobility and toxicity). To take into 45 account this heterogeneity, the proposed approach divides the NP population into classes, each 46 having specific transport and toxicity properties, and simulates them as independent species. The 47 approach is finally applied to a test case simulating the release of heterogeneous Silver NPs from a 48 landfill. The results show that taking into account the size-dependent mobility of the particles 49 provides a more accurate result compared to the direct application of the standard ASTM procedure. 50 In particular, the latter tends to underestimate the overall toxic risk associated to the nP release.

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52 Capsule

A risk assessment procedure for nanoparticle releases at contaminated sites is proposed. The standard human health risk assessment models for subsurface migration are adapted to nanoparticles

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#### 1. Introduction

The use of engineered nanoparticles (NPs) in industrial applications and commercial products have grown substantially in recent years. However, despite their great potential for technology, NPs can also represent a significant, and still largely unknown, environmental hazard. NP-containing products are already widely available on the market, or expected to be in few years, likely leading to the dissemination of large amounts of NPs in the environment. Despite the advanced stage of the research on their technological applications, the possible impacts of NPs on the environment are less studied, which may pose concerns on safety as well as social acceptance of NP-based products. In recent years, a growing body of studies have been devoted to the assessment of potential risks associated to the release of NPs, including the identification of preferential migration pathways, the estimation of NP concentration in the different environmental compartments, and the assessment of their toxicity toward human and ecological targets (Hendren et al., 2013; Garner and Keller, 2014). The majority of these studies focus on the fate of NPs gradually released from diffuse sources, eg. use of NPs-containing fertilizers and sludge in agriculture, direct release from consumer products (eg. paints, textiles, fuels, etc.), and incomplete removal of NPs in wastewater treatment plants (Gottschalk et al., 2009; Batley et al., 2013; Kaegi et al., 2013; Klitzke et al., 2015). A quantitative estimation of potential environmental concentrations of representative NPs from diffuse sources, and the associated toxicity risks, was proposed by several authors. However, comprehensive studies including several NPs and release scenarios are fewer, also due to the extreme complexity of the topic, eg. (Boxall et al., 2007; Hendren et al., 2013; Sun et al., 2014; Dale et al., 2015). The release from diffuse sources is relevant in terms of total mass and accumulation in the environment, but, at the moment, the resulting average NP environmental concentrations are modest, and far below toxicity limits (Batley et al., 2013; Garner and Keller, 2014). Conversely, releases from point sources can result in significantly higher concentrations (and consequently, higher potential risks) at a local scale. Typical release scenarios include leaching from landfills where NPs-containing products are disposed; releases at industrial sites where NPs are manufactured, due to continuous, unintentional losses during normal activities of the plant, or following major accidents which result in the release and consequent accumulation of NPs in the soil and subsoil; long-term remobilization of NPs delivered on purpose at contaminated sites for groundwater remediation.

The possible fate of significant amounts of engineered NPs released at point sources, and the associated risk posed to human health, have been scarcely faced by researchers at the moment. To this aim, long-term (chronic) effects could be quantified and evaluated using risk assessment procedures, similar to those conventionally employed in the management of sites contaminated by chemical compounds. The most widely used approach in this sense is the Risk-Based Corrective Action (RBCA) ASTM standard, which quantifies the toxic and carcinogenic risk arising for human receptors due to the exposure to the chemical substances released at contaminated sites (ASTM, 2015). Risk assessment approaches, procedures and computational tools are available and largely used for chemical substances. Extended and modified formulations of the analytical equations of the standard ASTM approach have been recently proposed to incorporate further processes (eg. biodegradation in the unsaturated zone) and tools (eg. sensitivity analysis) (Avagliano et al., 2005; Lemke and Bahrou, 2009; Baciocchi et al., 2010; Verginelli and Baciocchi, 2013). The short- and intermediate-term fate and toxicity of NPs released in major accidents has been recently faced by Nowack et al. (2014) as well as risks associated to the use of NPs as pesticides (Kookana et al., 2014). However, approaches and tools for the estimation of the risk associated to sites contaminated by NPs are almost lacking at the moment: few works were proposed to extend fate models of current risk assessment procedures to nanomaterials (Dale et al., 2014; Praetorius et al., 2014), and a comprehensive approach for the assessment of long-term risks is still missing.

Several challenges are to be faced for a successful adaptation of the ASTM procedure to NPs: on the one hand, particle-specific toxicity parameters (eg. Chronic Reference Dose RfD and Slope Factor SF), requested in the procedure, have been already determined for very few particles; on the other hand, the processes controlling NP migration in the environmental compartments may be significantly different from those associated to chemical substances. Moreover, both mobility and toxicity depend not only on the NP composition, but also on their size, shape, eventual coating, and environmental modifications which particles may undergo after release (eg. oxidation, dissolution, interaction with organic matter, etc.). In particular, a key property which poses major challenges in the adaptation of the ASTM transport models to NPs is particle heterogeneity. Even NPs which are fairly homogeneous when released may significantly change their properties over time, and result in a very heterogeneous population on the long term (Westerhoff and Nowack, 2012). Nanoparticles may be heterogeneous in size, shape, surface coating etc., which are all properties with a significant effect on the NP overall mobility in the subsurface. Among these properties, particle size is definitely a dominant one (Tufenkji and Elimelech, 2004). Particles having the same composition and shape, but different size, are characterized by a different mobility in groundwater.

The toxic effects of nanoparticles have been extensively investigated in recent years, both in vivo and in vitro, but very few toxicity indicators have been determined (Schilling et al., 2010; Shi et al., 2013). Sets of RfD and SF values for particles having the same composition but different size, or coating, are not available in the literature. Moreover, no standard classification of NPs as carcinogenic is available. Ecotoxicity have been quantitatively assessed in some cases for selected nanoparticles (eg. Ag, TiO<sub>2</sub>, fullerene, carbon nanotubes), while toxicity limits relevant to human risk assessment have not been standardized yet (Demir et al., 2013; Johnston et al., 2013; Comfort et al., 2014; Siripattanakul-Ratpukdi and Fürhacker, 2014). Values of RfD for Ag NPs have been proposed (Kim et al., 2010; Windler et al., 2013), while in other cases the use of the RfD of the corresponding bulk substances is recommended (Varner et al., 2010).

In this work, the framework for the development of risk assessment procedures for NPscontaminated sites is presented, discussing the modifications to the standard procedures and
mathematical tools already available for chemicals, and the main challenges still to be faced for the
application of such a procedure to real contaminated sites. In particular, the crucial role of particle
size is discussed, and an adaptation of the standard ASTM procedure at Tier 2 is proposed for NP
releases. NP-specific transport models are simplified and adapted to the analytical solutions in the
standard ASTM approach, and the selection of appropriate toxicity indicators is briefly discussed.

An example of risk assessment for a NP-contaminated site is finally presented.

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# 2. Development of a risk assessment procedure adapted to

## NPs

- 140 The ASTM procedure follows a tiered approach, with complexity increasing from Tier 1 to Tier 3.
- 141 Tier 1, based on a direct comparison of observed concentrations against screening levels reported in
- 142 look-up tables, is not site-specific, and is scarcely applied, apart from extremely simplified
- scenarios. In most cases, a site-specific procedure is adopted, based on the use of analytical or
- numerical solutions (Tier 2 or 3, respectively) to describe the migration of the contaminants from
- the source to the potential receptors through different migration pathways. Despite Tier 3 allows for
- the application of more realistic fate and transport models, Tier 2 is more commonly applied due to
- the simplicity of use and collectability of the site-specific data required for its application.
- Following the ASTM standard (ASTM, 2015), a risk analysis at Tier 2 and 3 is composed by three
- stages:

- Stage 1, including the identification of the release source and of the relevant migration pathways in the environmental matrices, from the source to the point of exposition (POE) where potential receptors are located.
- Stage 2, including predictive simulation of contaminant spreading along the migration pathways previously identified. Analytical (Tier 2) or numerical (Tier 3) models are applied to quantify the expected concentration at POE (C<sub>POE</sub>), provided that the concentration at the source (C<sub>0</sub>) is known;
- Stage 3, the estimation of the impact on potential receptors in terms of chronic toxicity and
   carcinogenic effects.
- In the next paragraphs, for each stage, the adaptations to extend the ASTM approach to NPcontaminated sites are discussed.

#### 2.1 Stage 1: Major migration pathways for NP release

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- The ASTM approach is typically applied to contaminated sites. In this case, three major exposure pathways are identified, namely exposure to contaminated soil, contaminated air, and contaminated groundwater. The first is associated to a direct contact of the potential receptor with the contaminated soil; it is therefore limited to on-site exposure, and the definition of migration models is not necessary. Since for most NPs a relatively fast precipitation onto the soil is expected (Garner and Keller, 2014), also migration through air is likely relevant only for on-site exposure.
- The subsoil very often represents the most likely migration scenario for the long-term NP fate.

  Consequently, in this work we focus on this scenario, and NP migration through the air will not be discussed. However, it is worth to mention that, under specific scenarios which may lead to NP dispersion in the air, adequate transport models should be developed and discussed following an approach similar to the one applied here for the subsurface.

# 2.2 Stage 2: Migration of the NPs from the source to the potential receptors

Particle transport in groundwater is controlled by mechanisms which can only be partially assimilated to those controlling the migration of chemical substances. In the standard ASTM

- procedure the migration of a contaminant from the source to the point of exposition of the potential receptor is schematized through the following steps (Figure 1):
- in the source area, the contaminant is dissolved from solid phase into pore water (from S<sub>soil</sub> to C<sub>leach</sub>); the process is quantified by the Soil-Water Partition Factor (K<sub>sw</sub>= S<sub>soil</sub>/C<sub>leach</sub>). In case of thick unsaturated zone and/or easily degradable contaminants, additional mitigation processes can be included and modeled at this stage, thus leading to a reduced concentration in the leachate while reaching groundwater (Connor et al., 2007; Verginelli and Baciocchi, 2013).
- 187 When reaching the water table, the leachate mixes with groundwater (from  $C_{leach}$  to  $C_0$ ); the 188 — process is quantified by the Leachate Dilution Factor (LDF =  $C_{leach2}/C_0$ ).
- The contaminant migrates through the aquifer toward the potential receptor (from C<sub>0</sub> to C<sub>POE</sub>); the process is represented by the Dilution Attenuation Factor (DAF=C<sub>0</sub>/C<sub>POE</sub>).
- The first two steps may be included in the so-called Leaching Factor LF= $1/(K_{sw} \cdot LDF)$ .
- 192 The overall attenuation from the source to the potential receptor is represented by the Natural
- 193 Attenuation Factor NAF [L<sup>3</sup>M<sup>-1</sup>]:

$$194 NAF = \frac{S_{soil}}{C_{POE}} = K_{sw} \cdot LDF \cdot DAF (1)$$

- where S<sub>soil</sub> is the contaminant concentration in solid phase at the source, expressed as mass of
- 196 contaminant per unit mass of soil [MM<sup>-1</sup>], and C<sub>POE</sub> is the contaminant concentration in water at
- 197 POE [ML<sup>-3</sup>].
- 198 At Tier 2, simplified scenarios for contaminant dissolution and transport are adopted, and analytical
- 199 transport models are applied to predict the concentrations at the potential receptors (C<sub>POE</sub>). A
- summary of Tier 2 analytical solutions is reported in Supporting Information. At Tier 3, more
- 201 complex scenarios can be considered, and numerical solutions are adopted to simulate the migration
- of the contaminants (Baciocchi et al., 2010; Pinedo et al., 2014; ASTM, 2015).
- To take into account the influence of NP heterogeneity (eg. NPs heterogeneous in size) the particle
- 204 population can be divided into classes, and the transport of each class modeled independently. As a
- consequence, one value of NAF is to be calculated per each class i, NAF<sub>i</sub>:

$$NAF_{i} = \frac{S_{soil,i}}{C_{POE,i}} = K_{sw,i} \cdot LDF_{i} \cdot DAF_{i}$$
(2)

207 Being particle transport class-dependent rather than mass-dependent, it is more convenient to

208 consider number concentrations rather than mass concentrations, thus

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$$C_i = m_i N_{w,i}$$
 and  $C = \sum_i m_i N_{w,i}$  (3a)

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$$S_i = \frac{1-\varepsilon}{\rho_s} m_i N_{s,i}$$
 and  $S = \frac{1-\varepsilon}{\rho_s} \sum_i m_i N_{s,i}$  (3b)

- where  $N_{w,i}$  and  $N_{s,i}$  are the number concentration of particles of the i-th class per unit volume of
- water and of solid phase, respectively [L<sup>-3</sup>],  $m_i$  is the mass of a particle of the i-th class [M],  $\rho_s$  is the
- solid matrix bulk density [ML<sup>-3</sup>], ε is the porosity [-]. The overall mass concentrations for NPs in
- 214 liquid and solid phase, C and S, can be obtained summing up mass concentrations of the individual
- classes, C<sub>i</sub> and S<sub>i</sub>.
- 216 Therefore, NAF<sub>i</sub> can be defined as

$$NAF_{i} = \frac{1 - \varepsilon}{\rho_{s}} \frac{N_{s,soil,i}}{N_{w,POF,i}}$$
(4)

218 Similar definitions can be written for K<sub>sw,i</sub>, LDF<sub>i</sub> and DAF<sub>i</sub> (Supporting Information).

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#### 2.2.1 Definition of DAF for nanoparticles

- 222 In the standard ASTM procedure, the spreading of chemical substances in groundwater (and
- consequently NAF) is quantified by analytical or numerical models describing the contaminant
- 224 transport due to advection, dispersion, sorption onto the solid matrix, degradation, and
- volatilization. Assuming first order degradation/volatilization and linear equilibrium sorption, the
- partial differential equation (PDE) describing the solute transport in groundwater is:

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$$\frac{\partial}{\partial t} (\varepsilon RC) + \nabla \cdot (uC) - \nabla \cdot (\varepsilon D\nabla C) + \varepsilon \lambda C = 0$$
 (5)

- where u is the specific discharge rate [LT<sup>-1</sup>], D is the hydrodynamic dispersion tensor [L<sup>2</sup>T<sup>-1</sup>],  $\lambda$  is
- 229 the first order degradation rate constant (describing either chemical degradation, biodegradation or
- volatilization) [T<sup>-1</sup>], and R is the retardation factor (describing linear equilibrium sorption onto the
- porous matrix). At Tier 2, the ASTM procedure suggests the use of the analytical solution of

Domenico (Domenico, 1987) for the calculation of C<sub>POE</sub>. In particular, the solution at steady state is usually adopted:

$$\frac{C_{POE}}{C_0} = \frac{1}{4} \exp \left[ \left( \frac{x}{2\alpha_x} \right) \left( 1 - \sqrt{1 + \frac{4\lambda\alpha_x}{v}} \right) \right] \cdot \left[ erf \left( \frac{y + \frac{L_w}{2}}{2\sqrt{\alpha_y x}} \right) - erf \left( \frac{y - \frac{L_w}{2}}{2\sqrt{\alpha_z x}} \right) \right] \cdot \left[ erf \left( \frac{z + \delta_{sw}}{2\sqrt{\alpha_z x}} \right) - erf \left( \frac{z - \delta_{sw}}{2\sqrt{\alpha_z x}} \right) \right] \quad (6)$$

where v is the seepage velocity  $u/\epsilon$  [LT<sup>-1</sup>],  $L_w$  and  $\delta_{sw}$  are the transversal and vertical extents of the contamination source (Figure 1) [L],  $\alpha_x$   $\alpha_y$  and  $\alpha_z$  are the horizontal, transversal and vertical dispersivities [L]. The Domenico transient solution is reported in the Supporting Information.

Two major points can be identified which make the direct application of Eq. 5 (and its analytical or numerical solutions) inappropriate to NPs as it is. These two aspects are the influence of heterogeneities within the NP population (above all, the heterogeneity in size), and the intrinsic difference of the mechanisms controlling the NP interactions with the porous medium, compared to solutes. The first aspect can be taken into account by dividing the NP population into classes, with different transport properties, and consequently calculating NAF<sub>i</sub> per each class, as defined in Eq. 2. Concerning the second aspect, NP fate in the subsoil follows mechanisms noticeably different from those typical of solutes. Particle transport is controlled by advection, dispersion and kinetic mass transfer between liquid and solid phase (attachment/detachment) (Kretzschmar et al., 1999; Tosco et al., 2009). Mechanical filtration of large particles or aggregates may also play a relevant role. In unsaturated soils, particle attachment at the air-water interface can also have a significant impact (Sim and Chrysikopoulos, 1999; Bradford and Torkzaban, 2008). A vast literature is available on the different processes and the corresponding mathematical formulations (Johnson et al., 1996; Bradford et al., 2002; Johnson et al., 2007; Petosa et al., 2010; Messina et al., 2015), and a review of the topic is beyond the purpose of this paper.

Considering the transport mechanisms led by Eq. 5, some are clearly inapplicable to NPs, eg. the contaminant volatilization. Also NP biodegradation is unlikely: bacteria-mediated transformations are expected for most NPs, but their effect is a modification of surface properties and transport behavior, rather than a "disappearance" of the particles (Lowry et al., 2012; Nowack et al., 2012; Schaumann et al., 2015). Moreover, the equilibrium sorption of a solute can only be partly assimilated to the kinetic deposition and release of NPs, as widely debated in the recent literature (Dale et al., 2014; Praetorius et al., 2014; Cornelis, 2015). As a consequence, the transport models adopted in the standard ASTM procedure cannot be directly applied to simulate the transport of

- NPs, but must be adapted and extended to include NP-relevant mechanisms of transport. Neglecting
- NP aggregation and/or breakage of aggregates, the model equation for the i-th class of NPs is

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$$\frac{\partial}{\partial t} \left( \varepsilon N_{w,i} \right) + \frac{\partial}{\partial t} \left[ (1 - \varepsilon) N_{s,i} \right] + \nabla \cdot \left( u N_{w,i} \right) - \nabla \cdot \left( \varepsilon D \nabla N_{w,i} \right) = 0$$
 (7)

- The second term of Eq. 7 represents the interactions of the suspended NPs with the porous matrix,
- and can be expressed, in a general form, as

$$266 \qquad \frac{\partial}{\partial t} \left[ (1 - \varepsilon) N_{s,i} \right] = \varepsilon k_{a,i} \psi_i N_{w,i} - k_{d,i} (1 - \varepsilon) N_{s,i} \tag{8}$$

- where  $k_{a,i}$  and  $k_{d,i}$  are respectively the attachment and detachment rates  $[T^{-1}]$  of the i-th class, and  $\psi_i$
- 268 is a kinetic function depending on the specific attachment mechanism (linear deposition, blocking,
- 269 ripening, straining...). The three parameters all depend on particle size.
- 270 An analytical solution to Eqs. 7-8 for 3D domains, equivalent to the Domenico's solution, is not
- available. Analytical solutions were developed for 1D domains (Šimůnek et al., 2008) and for
- simplified 3D (Sim and Chrysikopoulos, 1998), but for general 3D domains numerical solutions are
- 273 requested, eg. MNM3D (Bianco et al., 2016). Even if such models can provide an accurate and
- 274 physically meaningful description of particle transport processes, they are too complex for a direct
- application at Tier 2. For this reason, we propose here an adaptation of Domenico's analytical
- solution to solve Eqs. 7-8, for each class of NPs i, to simulate NP transport in 3D scenarios suitable
- for a Tier 2 risk analysis.
- 278 To this aim, Eqs. 7-8 must be first re-arranged to the structure of Eq. 5 (Table 1). For example,
- comparing Eqs. 7-8 to Eq. 5, it can be observed that linear irreversible attachment ( $\psi_i=1$ ,  $k_{d,i}=0$  in
- Eq. 8) can be formally simulated as a first order degradation without any simplifying assumption.
- 281 Conversely, NP deposition/release can be approximated as a sorption process only for those
- formulations leading to a dynamic equilibrium between solid and liquid phase (eg. blocking, linear
- reversible deposition), and only under specific simplifying assumptions.
- From a formal point of view, a dynamic equilibrium is possible when Eq. 7 can be re-arranged in
- 285 the form of an implicit kinetic formulation (Azizian, 2004):

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$$\frac{\partial}{\partial t} \left[ (1 - \varepsilon) N_{s,i} \right] = K_{eq,i} \left( N_{s,i}^* - N_{s,i} \right)$$
 (9)

- where  $N_{s,i}^*$  [-] is the NP concentration in the solid phase when the dynamic balance is reached, and
- $K_{eq,i}$  [ML- $^3$ T- $^1$ ] is the implicit rate constant. Both  $N_{s,i}$  and  $K_{eq,i}$  depend on the considered
- 289 deposition/release mechanism.
- 290 If Eq. 9 can be written, a retardation factor can be formally defined as:

$$R_{i} = 1 + \frac{1 - \varepsilon}{\varepsilon} \frac{N_{s,i}^{*}}{N_{w}}$$
 (10)

- 292 The approximation of dynamic equilibrium, and therefore the applicability of a retardation factor, is
- valid when the characteristic time of the attachment/detachment process is significantly lower than
- 294 the characteristic time of advection. Similarly to solute sorption (Azizian, 2004; Werner et al.,
- 295 2012), also for NPs it is possible to evaluate how far conditions are from equilibrium by means of
- the Damköler number:

$$297 Da_i = \frac{K_{eq,i}L}{u} (11)$$

- 298 where L is the scale of the problem (here, the x coordinate). Kinetic processes can be neglected for
- 299 Da>1.

- From a practical point of view, equilibrium is established and NP deposition can be approximated
- 301 by a retardation factor when Da>1, that is for  $L > u/(1-\varepsilon)k_{d2}$ .
- 302 If a particle size distribution is considered, R<sub>i</sub> is to be defined per each class. A summary of the
- values of  $\lambda_i$  and  $R_i$  for the most common deposition kinetics is provided in Table 1. Details on the
- applicability of this approximation, and a step-by-step procedure for the selection of the appropriate
- approximation are provided in the Supporting Information.
- 306 In conclusion, it is strongly recommended that, when developing a comprehensive NP risk
- assessment tool (likely, at Tier 3), the impact of a heterogeneous NP population is included in the
- 308 transport and fate models, namely using solutions to Eqs. 7-8 for a heterogeneous NP population
- 309 with class-dependent parameters, rather than using a homogeneous one. Nevertheless, for a first
- 310 screening, at Tier 2 simplifying assumptions can be made concerning NP transport on the long term
- and over large scales, and consequently the mathematical formulation adopted in standard ASTM at
- Tier 2 (i.e. using Eq. 6) can be adopted also for NPs without major modifications (see Paragraph 3).

#### 2.3 Stage 3: risk estimate

- 315 The standard ASTM procedure quantifies the risk associated to the chronic exposure to a
- 316 contaminant or, as in this case, to nanoparticles, through two indexes, namely the Hazard Quotient
- 317 (HQ) for toxic effects, and the Incremental Lifetime Cancer Risk (ILCR) for carcinogenic effects.
- 318 The two indexes cumulate the chronic effects generated by the different exposure pathways and
- 319 substances (ASTM, 2015).

- 320 For a single substance and for the exposure due to injection of groundwater, the HQ index is
- 321 calculated as the ratio of the average intake of substance at POE, and the Reference Dose:

$$322 HQ = \frac{C_{POE} \cdot E}{RfD} (12)$$

- 323 where E is the exposure rate (i.e. average amount of water ingested per day per unit body weight)
- 324 [L<sup>3</sup>M<sup>-1</sup>T<sup>-1</sup>] and RfD is the Reference Dose [L<sup>3</sup>M<sup>-1</sup>T<sup>-1</sup>], that is the maximum dose below which no
- 325 chronic toxic effect is observed (Connor et al., 2007; ASTM, 2015). RfD values are typically
- defined from NOAEL (Not Observed Adverse Effect Level) or LOAEL (Lowest Observed Adverse
- 327 Effects Level), and standardized in databases, eg. RAIS (http://rais.ornl.gov/tutorials/toxvals.html).
- 328 HQ<1 corresponds to an acceptable toxic risk, HQ>1 to an unacceptable toxic risk.
- 329 For carcinogenic effects, the ILCR index is calculated as the product of the average intake  $C_{POE} \cdot E$
- and the Slope Factor SF [-], determined from dose-response curves:

$$ILCR = C_{POE} \cdot E \cdot SF \tag{13}$$

- Figure 2 reports a comparison of different scenarios for the calculation of the toxic effects of NPs,
- assuming different approximations. Scenario A corresponds to the standard ASTM procedure for
- 334 chemical substances: transport models describe how the NP concentration decreases from the
- source to the POE, without taking into account any NP-dependent transport parameter. In this case
- Eq. 12 is applied to calculate the HQ index using a constant value of RfD. However, this approach
- 337 is too simplistic, and size-dependent transport of the NPs from the source to POE must be
- 338 considered (Scenario B). As evidenced in Figure 2, taking into account the NP size-dependent
- transport may result in significantly different values of HQ, even if the same NP mass at source is
- 340 considered.
- Both in the case of application of the (simplistic) Scenario A, and of Scenario B, the definition of
- RfD (and SF) values appropriate for NPs is likely the major challenge for the implementation of the

risk assessment procedure. Similarly to NP transport, also NP toxicity is known to be size dependent. Toxicity studies on silver NPs provided different values of RfD for particles of different size, particularly, higher toxicity for smaller particles (Kim et al., 2010; Windler et al., 2013; Hadrup and Lam, 2014). Also the eventual coating may affect NPs toxicity: coating by humic acid is reported to decrease toxicity of Silver NPs, while coating with citrate increases toxicity (Angel et al., 2013).

Size-dependent toxicity profiles would be crucial for the correct application of risk assessment to NPs. As reported for Scenario C in Figure 2, considering size-dependent RfD values, HQ may be significantly different from the values obtained in Scenarios A and B. If size-dependent toxicity values for NPs were available, a rigorous approach for the calculation of HQ and ILCR should take into consideration the particle size distribution at POE, and the toxicity indexes should be obtained by combining Eqs. 7-8 with Eqs. 12-13:

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$$HQ = \sum_{i} \left( \frac{C_{POE,i}}{RfD_{i}} \right) \cdot E = \sum_{i} \left( \frac{m_{i} \cdot N_{w,POE,i}}{RfD_{i}} \right) \cdot E$$
 (14)

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$$ILCR = \sum_{i} (C_{POE,i} \cdot SF_i) \cdot E = \sum_{i} (m_i \cdot N_{w,POE,i} \cdot SF_i) \cdot E$$
 (15)

Finally, the possible particle dissolution in the human body may also be an additional challenge when evaluating NP-related risk to human health: for eg., some particles (eg. Silver NPs) may be partly dissolved when ingested. For this reason, it would be recommended to calculate the risk associated to ingestion using both the limits for NPs, and the limits for the corresponding dissolved species.

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## 3. Application of the NP-modified risk assessment procedure

#### 3.1 Methods

The risk assessment procedure described in paragraph 2 was applied to a synthetic case of release of Silver nanoparticles (Ag-NPs) from a landfill. The application followed these steps:

- Laboratory results from a published work on Ag-NP transport (Wang et al., 2014) were considered, and NP transport parameters were obtained by least-squares fitting the experimental breakthrough curves;
- The dependency of NP transport parameters on flow velocity and particle size was modeled following the approach of a previous work (Tosco et al., 2014) and transport parameters for the synthetic landfill test case were obtained from column test results; transport mechanisms were approximated to degradation and sorption processes, as discussed in paragraph 2.2;
- NP release from the landfill and transport in groundwater was simulated under Scenarios A
   and B of Figure 2 and toxic risk was estimated.

#### 3.1.1 Column tests

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379 Experimental results of column transport tests of Ag-NPs (average size d<sub>p</sub>=16 nm) in natural soils reported by Wang et al. (2014), were modeled. In particular, two experimental breakthrough curves 380 381 (BTCs) for Ag-NPs injected in pure quartz sand, and a mixture of 20% quartz sand and 80% of 382 natural soil (average size d<sub>s</sub>=0.65 mm for both quartz sand and soil) were considered, herein named 383 "0%Soil" and "80%Soil", respectively. The NPs were injected at a concentration of 100 mg/l in fully saturated columns (inner diameter 1.1 cm, column length 10 cm, discharge rate 0.25 ml/min, 384 385 0.42). The **BTCs** inverse-fitted porosity were using the software **MNMs** 386 (www.polito.it/groundwater/software/MNMs) (Tosco and Sethi, 2009; Bianco et al., 2016). Two 387 linear interaction sites were considered, one irreversible (fitted parameter: ka,irr) and one reversible 388 (fitted parameters:  $k_{a,rev}$  and  $k_{d,rev}$ ). Thus Eqs. 7-8 become

$$\begin{cases}
\frac{\partial}{\partial t} \left( \varepsilon N_{w,i} \right) + \frac{\partial}{\partial t} \left[ (1 - \varepsilon) N_{s,irr,i} \right] + \frac{\partial}{\partial t} \left[ (1 - \varepsilon) N_{s,rev,i} \right] + \nabla \cdot \left( u N_{w,i} \right) - \nabla \cdot \left( \varepsilon D \nabla N_{w,i} \right) = 0 \\
\frac{\partial}{\partial t} \left[ (1 - \varepsilon) N_{s,irr,i} \right] = \varepsilon k_{a,irr,i} N_{w,i} \\
\frac{\partial}{\partial t} \left[ (1 - \varepsilon) N_{s,rev,i} \right] = \varepsilon k_{a,rev,i} N_{w,i} - k_{d,rev,i} (1 - \varepsilon) N_{s,rev,i}
\end{cases}$$
(16)

For the column tests, particles were assumed mono-dispersed and consequently only one class of NP size was considered (i=1). For the simulation of the release from the landfill, 20 classes were considered in Scenario B (i=1,...,20).

#### 3.1.2 Modeling attachment/detachment parameters

- An approach similar to Tosco et al. (2014) was adopted to model the dependency of k<sub>a,irr,i</sub> and k<sub>a,rev,i</sub>
- 396 from particle size and flow velocity. Briefly, the attachment rate is assumed proportional to the flow
- velocity v and the deposition efficiency  $\eta_0$ :

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$$398 k_{a,i} = A_i v \eta_{0,i} (17)$$

- where  $A_j$  is an empirical coefficient which incorporates dependences on other parameters [L<sup>-1</sup>].
- 400 The Yao model (Yao et al., 1971) was used to calculate  $\eta_{0,i}$ , which is function of several
- 401 parameters, including v and particle size.
- 402 Also the detachment rate depends on flow velocity (Tosco et al., 2014), thus

$$403 k_{d,i} = B_i v (18)$$

#### 3.1.3 Synthetic test case of Ag-NP release from a landfill

- 406 A landfill of longitudinal size W=80 m and transverse size L<sub>gw</sub>=80 m subject to effective recharge
- 407 I<sub>eff</sub>=450 mm/y was considered. The landfill is located above a 15 m thick unconfined aguifer, with
- 408 effective porosity  $\varepsilon$ =0.2, Darcy velocity u=7.6·10<sup>-7</sup> m/s, longitudinal, transversal and vertical
- dispersivities ( $\alpha_x$ ,  $\alpha_y$ ,  $\alpha_z$ ) equal to 10, 3.3 and 0.5 m respectively. The concentration of NPs in
- 410 landfill waste and leachate may significantly vary among sites (Gottschalk et al., 2009; Sun et al.,
- 411 2014). In this work, C<sub>leach</sub>=15 mg/l was assumed as representative value (Yang et al., 2012). No
- 412 attenuation was considered in the unsaturated zone for cautionary purposes, and only mixing with
- 413 groundwater (Eqs. S.3-S.4 in SI) was considered to obtain C<sub>0</sub>.
- Exposure E= 0.027 l/kg/d was used following the ASTM standard, corresponding to residential use.
- RfD was assumed constant for all particle classes, equal to  $3.0 \cdot 10^{-2}$  mg/kg/d, based on the work of
- 416 Kim et al. (Kim et al., 2010).

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#### 3.2. Results and Discussion

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#### 3.2.1 NP transport parameters: from column tests to simulated landfill release

423 The experimental data of Wang et al. (2014) were first modeled using the dual site linear attachment/detachment of Eq. 16 with i=1 (Figure 3 and Table 2). The two interactions mechanisms 424 425 (linear irreversible attachment and linear reversible attachment) were selected following a stepwise 426 approach, starting from the simplest model and increasing its complexity (and consequently number 427 of fitted parameters) until a satisfactory fitting of the experimental data was obtained. Briefly, the 428 simplest case of one linear irreversible interaction site (1 fitted parameter per each test, k<sub>a,irr</sub>) was 429 considered the first option for both tests. However, the fitting was not satisfactory (data not 430 reported). The same for one linear reversible site (2 fitted parameters, k<sub>a,rev</sub> and k<sub>d,rev</sub>). The third option, namely linear irreversible attached associated to a second site of linear irreversible 431 attachment (3 parameters: k<sub>a,irr</sub>, k<sub>a,rev</sub> and k<sub>d,rev</sub>) was the simplest providing a good fitting, with R<sup>2</sup> 432 433 parameter equal to 0.9888 and 0.8693 was obtained respectively for 0% Soil and 80% Soil. The fitted 434 attachment rate kairr for the first deposition mechanism (linear irreversible) is the same for both 435 column tests, while k<sub>a,rev</sub> and k<sub>d,rev</sub> for the second deposition mechanism (linear reversible) are 436 different. From a physical point of view, this finding suggests that irreversible attachment was not 437 affected by soil composition, but only by particle and soil size (and flow rate), and is therefore likely related to NP mechanical retention. Conversely, reversible attachment also depends on soil 438 439 composition.

- Eq. 17 was applied to fitted  $k_{a,irr}$  and  $k_{a,rev}$ , Eq. 18 to fitted  $k_{d,rev}$  obtained to determine the three parameters  $A_{irr}$ ,  $A_{rev}$  and  $B_{rev}$ . It is worth to mention that in the presence of linear (reversible or irreversible) deposition, the attachment rate is independent of the injected concentration. As a consequence, the parameters determined from these column tests (performed injecting Silver NPs at a concentration of 100 mg/l) can be assumed valid for the simulation of the leaching landfill, where the NP released concentration is 15 mg/l.
- Two alternative approaches were then considered to simulate NP release from the landfill, among those reported in Figure 2:
- Scenario A: NP size distribution was not considered; the released NPs are a homogeneous samples of Silver NPs having the same size as those of the column tests (i.e. 16 nm);

- Scenario B: An NP size distribution was assumed, in the range 5 to 200 nm, divided into 20 classes, with same average particle size of Scenario A (16 nm). The particle size distribution is reported in Figure 6 (blue curve at the source, i.e. X = 0).
- In both Scenarios, the same mass of particles (15 g/l) was released.
- The attachment and detachment rates  $(k_{a,irr}, k_{a,rev})$  and  $k_{d,rev}$  for the two Scenarios were calculated
- using the values of A<sub>irr</sub>, A<sub>rev</sub> and B<sub>rev</sub> (obtained from the column tests) in Eqs. 17-18. Following the
- 456 Yao model, the deposition efficiency (Figure 6), and consequently k<sub>a</sub>, is a function, among other
- parameters, of particle size and flow velocity; following Eq. 18, k<sub>d</sub> is independent of particle size,
- and is affected only by flow velocity. Consequently, for Scenario A, k<sub>a,irr</sub>, k<sub>a,rev</sub> and k<sub>d,rev</sub> are
- 459 constant parameters, and the only difference compared to the column tests is due only to the
- different flow velocity of the aquifer compared to the one applied in the column tests. For Scenario
- B, a different set of  $k_{a,irr,i}$  and  $k_{a,rev,i}$  is obtained for each class, while  $k_{d,red}$  is constant for all classes.
- The coefficients for both Scenarios are reported in Table 2.
- 463 Compared to the parameters fitted for column tests, the values obtained for Scenarios A and B for
- 464 the landfill synthetic case are roughly one order of magnitude lower, due to the different flow
- velocity of column tests ( $u=4.3 \cdot 10^{-5}$  m/s) and the landfill case ( $u=7.6 \cdot 10^{-7}$  m/s). Also particle size
- significantly influences the attachment/detachment coefficients: for Scenario B, k<sub>a,irr,i</sub> and k<sub>a,rev,i</sub>
- span over at least one order of magnitude, with particle size ranging from 15 to 200 nm, with
- evident implications on the relevance of considering particle size distribution when simulating NP
- 469 transport (paragraph 2.2.1). These two findings both suggest the importance of considering
- appropriate models and experimental conditions for the determination of NP transport parameters: if
- a risk analysis for an NP release from a landfill similar to this test case is to be performed, it is
- 472 crucial to determine particle transport parameters from experiments performed as close as possible
- 473 to the real site conditions (eg. flow velocity and NP type and size). If such conditions cannot be
- 474 reproduced in the laboratory, appropriate, well-established relationships like those of Eqs. 17-18 are
- 475 to be applied to transfer the NP parameters to the field scale conditions.

#### 3.2.2 NP risk assessment

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- 478 The Domenico solution was then applied for the calculation of C<sub>POE</sub> for the Ag-NPs in both
- 479 Scenarios A and B, and the modified ASTM procedure was applied for the risk assessment
- 480 (procedure fully described in SI in paragraph S2). The vertical extent of the mixing zone in the

aquifer ( $\delta_{gw}$ ) was calculated using Eq. S.4, resulting equal to 16.3 m (higher than the saturated 481 482 thickness b). As a consequence it was assumed  $\delta_{gw}$ =b and vertical dispersion was neglected (Connor 483 et al., 2007). Mixing of leachate with groundwater resulted in a dissolved concentration at source 484  $C_0=3.08 \text{ mg/l}.$ 485 Applying the approximations discussed in paragraph 2.2.1, for both Scenarios A and B irreversible 486 deposition was simulated as a first order degradation, reversible deposition as a linear sorption. The 487 corresponding  $\lambda_i$  and  $R_i$  were calculated using the equations reported in Table 1 and are reported in 488 Table 2. The applicability of this approximation was verified using Eq. 11. For both Scenarios, 489 Da>1 is verified for any x>8.2 cm, thus allowing the application of Domenico's solution all over the 490 domain. 491 Transport in groundwater was simulated for Scenarios A and B in both transient and steady state 492 conditions to calculate the C<sub>POE</sub> along the axis (y=0, z=0) where the highest concentrations are 493 found (Figure 4). Provided that the same concentration of Silver NPs is released at the source, under 494 Scenario A particles travel for a shorter distance: compare, for example, the concentration profiles 495 (left y-axis) along the plume axis at steady state in Figure 4 (to allow comparison of the two 496 Scenarios, the total mass concentration is here calculated for Scenario B using Eq. 3a). This 497 observed difference is due to the higher attachment efficiency, and consequently attachment rate, 498 characterizing 16 nm particles when compared to larger ones, which are present in the population of 499 Scenario B (see  $\eta_0$  trend in Figure 6). Conversely, for Scenario B, particles as a whole travel for 500 longer distances, due to the presence of (few) larger particles having a lower attachment efficiency. 501 These observations have a direct impact on the results in terms of toxic risk. For Scenario A, Eq. 12 502 was directly applied to calculate HQ, since only one class of particles was considered. For Scenario 503 B, the Domenico solution was applied independently for each NP class, and Eq. 14 was then used to 504 calculate HQ, assuming that RfD is the same for all classes. HQ values along the x-axis are reported 505 in Figure 4. Being the retardation factor R higher for 80% Soil than for 10% Soil, in transient 506 conditions (namely, 5 years after the initial release from the landfill) the extent of the area with HQ 507 above the threshold limit of 1 is significantly higher for the 0%Soil, as it can be observed from both 508 concentration profiles along the plume axis (Figure 4), maps (Figure 5) and numerical values of 509 length and area with HQ>1 (Table S.1 in SI). However, the HQ at the steady state, which is usually 510 considered for risk assessment, is the same for both 0%Soil and 80%Soil, since the irreversible 511 attachment coefficient, and consequently the parameter  $\lambda$ , is the same, and the retardation

coefficient R has no influence on the steady state concentration (see paragraph A.2).

The results evidence that for Scenario B the overall mobility of the Ag-NP is higher, thus resulting in larger areas where HQ>1. For example, at steady state, HQ values higher than 1 are found up to 85.6 m for Scenario A and 98.2 m for Scenario B downgradient the source of contamination (Figure 5 and Table S.1). Correspondingly, the area having HQ>1 is 16% larger for Scenario B compared to Scenario A. This is due to the different transport of different classes of NPs, which are characterized by different values of  $k_{aj}$ : the attachment efficiency (Figure 6) is higher for smaller particles, lower for larger particles. As a consequence, larger particles travel for longer distances, and the original particle size distribution at source (blue line in Figure 6) changes its shape along the x-axis, showing a more pronounced decrease in the concentration of smaller particles compared to larger ones. These results confirm that the adoption of size-dependent transport equations for NPs is worth to be applied, even in a simplified Tier 2 approach, and that the direct application of Scenario A is too simplistic.

#### 4. Conclusions

The ASTM approach for the Tier 2 risk assessment procedure for contaminated sites has been here adapted for application of releases of nanoparticles, and an example application to landfill leachate was presented. Even if particle transport in porous media is a complex phenomenon, the governing equations can be simplified under reasonable assumptions. It was demonstrated that particle transport described by a combination of a linear reversible and a linear irreversible attachment can be solved using the same equations of the transport of a dissolved contaminant subject to first order degradation rate and linear sorption, provided that the time scale of the dynamic attachment/detachment process is significantly smaller than the time scale of the transport in the porous medium. Moreover, it was demonstrated that considering the size-dependent transport of heterogeneous populations of NPs may lead to results, in terms of HQ values at POE, significantly different compared to the simplistic model where the particle size dependent transport is not considered. Similar considerations can be applied for other particle properties, eg. shape, surface coating, etc., which have an impact on NP mobility in the subsoil, and the risk assessment procedure for these cases could be the same here discussed for size-dependent particle transport.

Nevertheless, very few data are available at the moment on the influence of NP size, coating, shape etc. on their toxicity (particularly, chronic toxicity, requested in risk analysis). This represents the

engineered nanoparticles. In this sense, the availability of size-dependent (or, more in general parameter-dependent) reference doses is an unavoidable necessity, which has not been addressed at the moment.

It is finally worth to mention that the standard ASTM procedure do not take into account particles retained on the soil. However, it cannot be excluded that such NPs can be re-mobilized on a long term (Navarro et al., 2014), following for eg. changes in groundwater hydrochemical conditions. As a consequence, it is recommended that this issue is evaluated when dealing with sites contaminated by NPs, and the possible release of deposited NPs on a long time scale is carefully evaluated and

great challenge to the application of a risk assessment procedure to sites contaminated by

### **Acknowledgement**

eventually included in risk assessment scenarios.

The authors thank Mr. Federico Mondino for the collaboration in reviewing the literature on NP toxicity. This research did not receive any specific grant from funding agencies in the public, commercial, or not-for-profit sectors

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# **Figures**

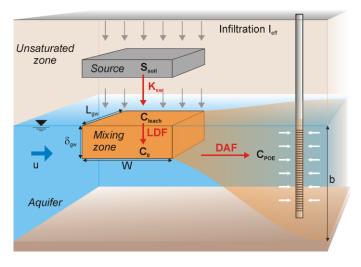


Figure 1: Scheme of particle release and transport.

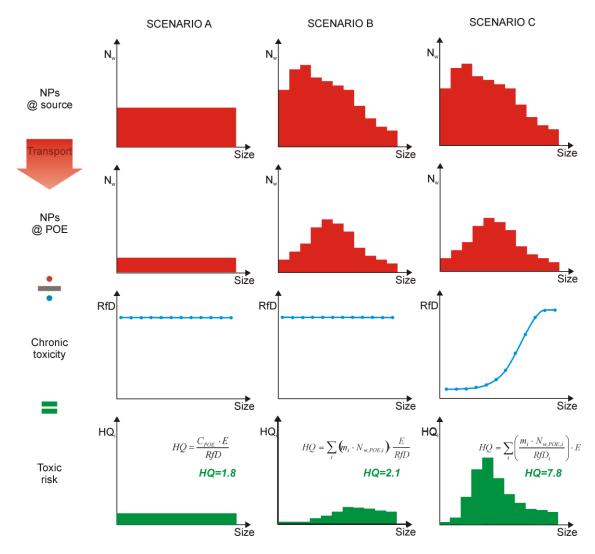


Figure 2: Comparison of three different scenarios for the application of NP-adapted risk assessment procedure: Scenario A, assuming no size-dependent transport nor toxicity; Scenario B, assuming size-dependent NP transport; Scenario C, assuming size-dependent transport and toxicity. The released concentration is the same in all scenarios.

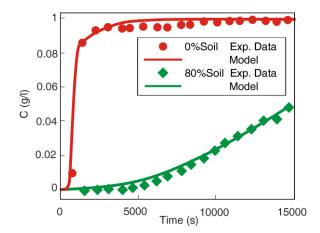


Figure 3: Experimental and simulated Ag-NP breakthrough curves for the experimental data of Wang et al. (2014) for 0%Soil and 80%Soil tests.

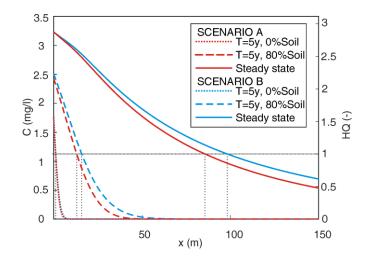


Figure 4: Synthetic test case for Ag-NPs release from a landfill: simulated Ag-NPs concentrations in groundwater and corresponding HQ values along the x axis (y=0, z=0) at steady state conditions (solid lines) and in transient conditions after 5 years for 0%Soil (dashed lines) and 80%Soil (dotted lines) for Scenario A (red) and Scenario B (blue).

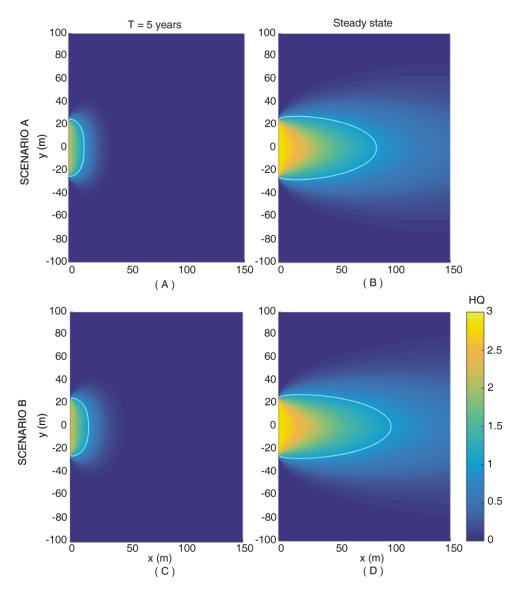


Figure 5: HQ maps calculated applying transient Domenico's solution after 5 years (Eq. S.6) for 0%Soil (A-C), and steady state solution (Eq. 6) (B-D). HQ is calculated assuming no size-dependent transport (A-B, corresponding to Scenario A in Figure 2) and size-dependent transport (C-D, corresponding to Scenario B in Figure 2). The white line corresponds to HQ=1.

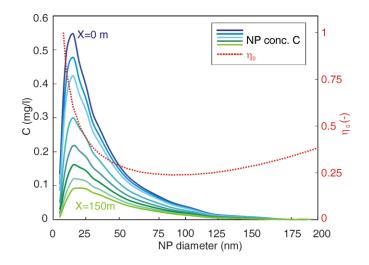


Figure 6: Synthetic test case for Ag-NPs release from a landfill: particle size distribution for Scenario B along the x axis y=0, z=0) at steady state, at different distances from the source (blue to green lines), and attachment efficiency as a function of particles size (red line).

## **Tables**

 Table 1: : Retention mechanisms for NP transport (1 or 2 interaction sites) and associated simplifying assumptions and parameter definition for the application of Domenico's solution

Retention mechanism(s)		Simplifying assumptions	Definition of Domenico's parameters	Applicabili Domenico's Transient (Eq. S.6)	-
1 site linear $\psi_i = 1$	Irreversible $k_{d,i} = 0$	None	$\lambda_i = \varepsilon k_{a,i}$ $R_i = 1$	Yes	Yes
	Reversible $k_{d,i} \neq 0$	$\frac{1}{K_{eq,i}} << \frac{x}{v}$	$R_{i} = 1$ $\lambda_{i} = 0$ $R_{i} = 1 + \frac{k_{a,i}}{k_{d,i}}$	Yes	Yes
1 site blocking $\psi_i = 1 - \frac{N_{s,i}}{N_{s \text{max}i}}$	Any (reversible or irreversible)	$\frac{1}{K_{eai}} << \frac{x}{v}$	$\lambda_i = 0$ $R_i \text{ n.d.}$	No	Yes
2 sites	Site 1: linear irrev. Site 2: linear rev.	$\frac{1}{K_{eq,i}} << \frac{x}{v}$	$\lambda_i = \mathcal{E}_{a1,i}$ $R_i = 1 + \frac{k_{a2,i}}{k_{d2,i}}$	Yes	Yes
	Site 1: linear irrev. Site 2: blocking	$\frac{1}{K_{eq,i}} << \frac{x}{v}$	$\lambda_i = \mathcal{E}k_{a1,i}$ $R_i \text{ n.d.}$	No	Yes
	J=1 linear rev. J=2 blocking	$\frac{1}{K_{eq,i}} << \frac{x}{v}$	$\lambda_i = 0$ $R_i \text{ n.d.}$	No	Yes

Table 2: Transport parameters for NPs in column tests and for the test case of Ag-NP release from a landfill

Parameter	Column tests		Scenario A		Scenario B	
	0%Soil	80%Soil	0%Soil	80%Soil	0%Soil	80%Soil
Site 1						
Attachment rate $k_{a1}$ (s <sup>-1</sup> )	$1.7 \cdot 10^{-7}$		3.4·10 <sup>-8</sup>		$1.3 \cdot 10^{-8} - 7.0 \cdot 10^{-8}$	
Degradation rate $\lambda = \varepsilon \cdot k_{a1} (s^{-1})$	1.5·10 <sup>-8</sup>		6.7·10 <sup>-9</sup>		$2.6 \cdot 10^{-9} - 1.4 \cdot 10^{-8}$	
Site 2						
Attachment rate k <sub>a2</sub> (s <sup>-1</sup> )	$3.0 \cdot 10^{-4}$	$1.0 \cdot 10^{-2}$	5.9·10 <sup>-5</sup>	$2.0 \cdot 10^{-3}$	$2.3 \cdot 10^{-5} - 1.2 \cdot 10^{-4}$	$4.5 \cdot 10^{-3} - 1.0 \cdot 10^{-2}$
Detachment rate $k_{d2}$ (s <sup>-1</sup> )	$7.0 \cdot 10^{-4}$	$5.0 \cdot 10^{-4}$	$5.0 \cdot 10^{-6}$	$3.6 \cdot 10^{-6}$	$5.0 \cdot 10^{-6}$	3.6·10 <sup>-6</sup>
Retardation coeff. R (-)	1.4	21.0	12.8	562.0	5.6-25.4	222-1160