Simulation of particle deposition in porous media: computational fluid dynamics and population balance modelling

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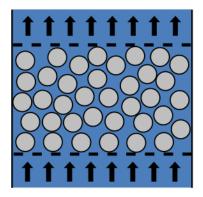
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Motivation of the work

Many fields of interest

- Packed bed reactors
- Filtration
- Chromatographic Separation
- Aquifer Remediation
- Enhanced Oil Recovery



- Fluid flowing through an arrangement of stationary solid grains.
- The flowing fluid can contain liquid droplets, gas bubbles or solid particles.

Computational models structure

POROUS MEDIUM GENERATION

- Experimental:
 - \cdot μ -CT, X-ray, SEM
- Algorithmic reconstruction:
 - \cdot DEM, particle-based
 - \cdot Rigid body simulation
 - \rightarrow Blender (opensource)

FLOW, TRANSPORT SIMULATION

- Computational Fluid Dynamics
 - · Ansys FLUENT (commercial)
 - · OpenFOAM
- (commercial) (opensource)

- \Rightarrow Model of porous medium with **Blender**
- \Rightarrow Meshing and CFD simulation with OpenFOAM

Dispersion in 3D Porous Media

Simulation Setup

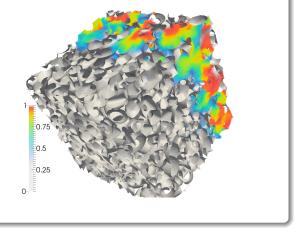
Geometry

- 2mm cubic sample
- 3000 grains
- 40M cells

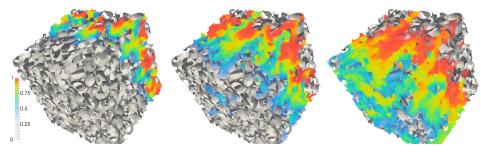
OPERATING CONDITIONS

- Particle diameter: $d_p = 1 \div 1000 \text{ nm}$
- Superficial velocity: $q = 10^{-6} \div 0.1 \text{ ms}^{-1}$
- $10^{-4} < \text{Re} < 300$

•
$$10^{-2} < \text{Pe} = \frac{qD_g}{\mathcal{D}_m} < 10^7$$



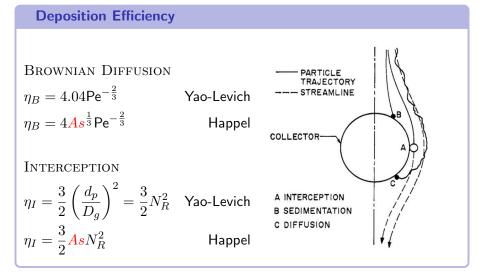
Hydrodynamic Dispersion



Snapshots of particle concentration at three different times

- Hydrodynamic dispersion enlarges and smoothens out the particle concentration front over time
- This effect increases for higher Péclet numbers

Particle Deposition



Particles Modeling

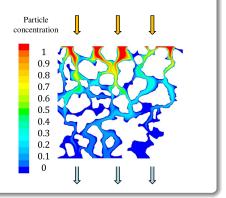
Particles are transported by convective and diffusive phenomena BOUNDARY CONDITION

- C = 1 at inlet
- C = 0 on grain surface (assumed "perfect sink" B.C.)
- **OPERATING CONDITIONS**
 - Particle diameter:

 $d_p = 1 \div 1000 \text{ nm}$

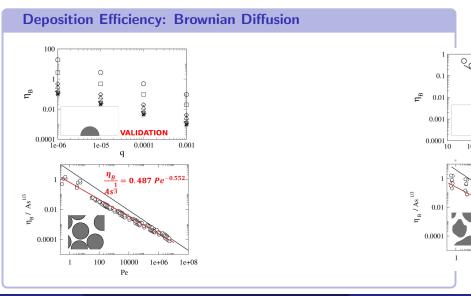
• Superficial velocity: $q = 10^{-6} \div 0.01 \text{ ms}^{-1}$

Collector deposition efficiency, η calculated with packed bed performance equation



$$\frac{dC}{dx} = -\frac{3}{2} \frac{1-\varepsilon}{\varepsilon D_g} \eta C$$

Results: Particle Deposition



Population Balance Modelling

Population balance equation

- \rightarrow evolution of the particle size distribution
- \rightarrow possibility of treating a polydisperse particle population

Solution of the PBE in the CFD code with the Method of Moments

$$\frac{\partial m_k}{\partial t} + \frac{\partial \mathbf{u} m_k}{\partial \mathbf{x}} = \frac{\partial}{\partial \mathbf{x}} \left(\Gamma_0 \frac{\partial m_{k-1}}{\partial \mathbf{x}} \right)$$

Deposition of polydisperse particle populations

Simulation Setup

Geometry

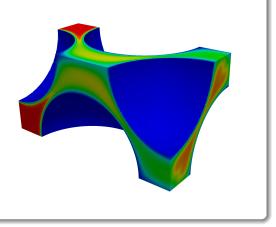
- Domain = one grain
- Face-centered cubic
- 260k cells

OPERATING CONDITIONS

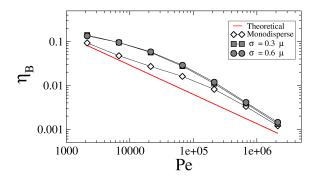
- Mean particle diameter: $\mu = 300 \text{ nm}$
- $10^{-3} < \text{Re} < 3$
- Two lognormal distributions:

$$\rightarrow \sigma = 0.3 \ \mu$$

$$\rightarrow \sigma = 0.6 \ \mu$$

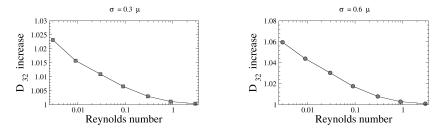


Results: Deposition rates of polydisperse particle populations



- Very different η-Pe relationship w.r.t to monodisperse case and theoretical prediction.
- Weak effect of particle population polidispersity.

Results: Increase in average diameter



- Higher σ means more deposition of smaller particles, hence an increase of average particle diameter.
- Behaviour of particle population changes in space during the evolution of the dispersion process
 - \rightarrow e.g. effect on reaction rates, dispersion coefficient, et c.

Conclusions

Micro-scale modeling is essential to the derivation of effective macro-scale models Classic deposition laws fail with:

- \rightarrow realistic (non-spherical) geometries
- \rightarrow polydisperse particle populations
 - Possibility of treating packings of arbitrary grain shape with BLENDER
 - Treatment of polydisperse particle populations via population balance modelling shows an improvement over theoretical predictions

Acknowledgements - People

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Computational Resources

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- CINECA

Thank you!