

Comparison of Chloroaluminate Melts for Aluminum Graphite Dual-Ion Battery Application

Original

Comparison of Chloroaluminate Melts for Aluminum Graphite Dual-Ion Battery Application / Elia, G. A.; Hoeppe, K.; Hahn, R.. - In: BATTERIES & SUPERCAPS. - ISSN 2566-6223. - ELETTRONICO. - 4:2(2021), pp. 368-373. [10.1002/batt.202000244]

Availability:

This version is available at: 11583/2959176 since: 2022-03-23T10:51:25Z

Publisher:

Wiley-VCH Verlag

Published

DOI:10.1002/batt.202000244

Terms of use:

This article is made available under terms and conditions as specified in the corresponding bibliographic description in the repository

Publisher copyright

(Article begins on next page)

Special
Collection

Comparison of Chloroaluminate Melts for Aluminum Graphite Dual-Ion Battery Application

Giuseppe Antonio Elia,^{*,[a, c, d]} Katrin Hoepfner,^[a, b] and Robert Hahn^[b]

Herein, we report a comparison of aluminum graphite dual-ion cells (AGDICs) electrochemical characteristics employing the conventional 1-ethyl-3-methylimidazolium chloride:aluminum trichloride (EMIMCl:AlCl₃) electrolyte and two popular deep eutectic solvents (DESs), namely urea:AlCl₃ and acetamide:AlCl₃. The three electrolytes' characteristics have been evaluated in terms of Al-stripping deposition capability and cycling behavior

in AGDICs. The results evidence the EMIMCl:AlCl₃'s Al-stripping deposition and rate capability in AGDICs superior characteristics addressed to the lower viscosity and higher conductivity with respect to the urea:AlCl₃ and acetamide:AlCl₃. On the other hand, the urea:AlCl₃ guarantees a much higher columbic efficiency in AGDICs, thanks to the superior electrochemical window stability.

1. Introduction

Batteries and, in general, electrochemical storage systems are considered the key enabling technology to green energy economy transition. Lithium-ion battery (LIB) is the most mature technology, being the selected power source for electromobility, thanks to the elevated energy density and good cycle life. However, long-term, large-scale application of LIBs appears to be problematic due to the natural scarcity and limited production capacity of key materials containing Co and Ni.^[1] Resources availability concerns pushed the research to explore alternative technologies based on abundant and widely available elements. Aluminum is one of the possible choices, having the advantages of being lightweight, low cost, and abundant (the most abundant metal in the Earth's crust).^[2,3] Several secondary electrochemical cells using aluminum anode and chloroaluminate melt electrolytes have been proposed,^[4-8] among them the most promising in terms of cycle life and rate capability are the aluminum graphite dual-ion batteries (AGDIBs).^[3,4,9-12] AGDIBs are expected to achieve 65 Wh kg⁻¹, 92 Wh l⁻¹ in terms of energy density (values evaluated on active

materials only), guarantee a cycle life of more than 10000 cycles with an overall cost of 0.03 €/kWh/cycle.^[3,11] To tackle the cost factor of AGDIBs, several groups proposed the use of a new class of ionic liquids called deep eutectic solvents (DESs), or ionic liquid analogs (ILAs), formed through a mixture of a strongly Lewis acid metal halide (AlCl₃) and a Lewis basic ligand (urea, acetamide).^[13-16] The substitution of the imidazolium cation of the conventional AlCl₃-ImidazoliumCl chloroaluminate with a cheaper and widely available chemical such as urea can substantially impact the system's overall cost. The retail price comparison of the three compounds indicates that EMIMCl is about ten times more expensive. Clearly, the retail price does not necessarily correspond to the product cost in high volume; however, it is an indication. The application of this class of electrolytes in AGDIBs is widely reported.^[17-24] However, a clear comparison of DES electrolytes against the state of the art AlCl₃-ImidazoliumCl chloroaluminate electrolyte is not available for AGDIB systems. For this reason, here we report a comparison of the electrochemical characteristics of AGDIBs employing two of the most widely used DES electrolyte, the urea:AlCl₃ and the acetamide:AlCl₃ against the conventional 1-ethyl-3-methylimidazolium chloride: aluminum trichloride (EMIMCl:AlCl₃) system.

2. Results and Discussion


Figure 1 reports the molecular structure of the three solvents used in this study. Figure 2 reports the CV results comparison of the Al stripping deposition process on Ni substrate employing (a) EMIMCl:AlCl₃-1:1.5, (b) Acetamide:AlCl₃-1:1.5, and (c) Urea:AlCl₃-1:1.5 electrolytes. The highest current peak value, of almost 3 mA cm⁻², is recorded employing the EMIMCl:AlCl₃-1:1.5 (Figure 2a), while using Acetamide:AlCl₃-1:1.5 (Figure 2b), the current peak value is about 1.3 mA cm⁻². The lower Al stripping deposition current peak of 0.47 mA cm⁻² is recorded using the Urea:AlCl₃-1:1.5 electrolyte (Figure 2c). The difference in the peak current intensity between the three electrolyte systems can be ascribed to the electron transfer kinetics, and


[a] Dr. G. A. Elia, K. Hoepfner
Technische Universität Berlin
Research Center of Microperipheric Technologies
Gustav-Meyer-Allee 25, 13355 Berlin, Germany

[b] K. Hoepfner, Dr. R. Hahn
Fraunhofer-Institut für Zuverlässigkeit und Mikrointegration
Gustav-Meyer-Allee 25, 13355 Berlin, Germany

[c] Dr. G. A. Elia
Helmholtz Institute Ulm (HIU)
Helmholtzstrasse 11, 89081 Ulm, Germany

[d] Dr. G. A. Elia
Karlsruhe Institute of Technology (KIT)
P.O. Box 3640, 76021 Karlsruhe, Germany
E-mail: elia@kit.edu

 An invited contribution to a joint Special Collection between ChemElectroChem and Batteries & Supercaps dedicated to research Beyond Lithium-Ion Batteries

 © 2020 The Authors. Batteries & Supercaps published by Wiley-VCH GmbH. This is an open access article under the terms of the Creative Commons Attribution License, which permits use, distribution and reproduction in any medium, provided the original work is properly cited.

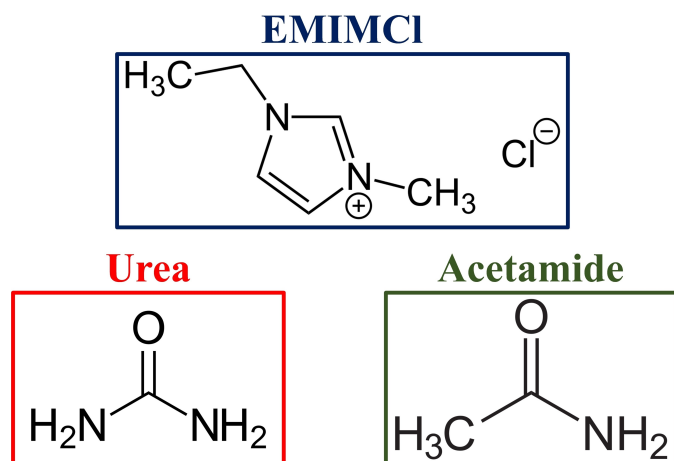


Figure 1. EMIMCl, Urea and Acetamide solvent molecular structure

active species concentrations, and diffusivity.^[25] Indeed the higher current peak of the EMIMCl:AlCl₃ relates well with its higher conductivity and lower viscosity (high active species diffusivity). However, the different ionic speciation influences on the stripping deposition kinetics cannot be excluded.^[13–16] The EMIMCl:AlCl₃ ions speciation includes AlCl₄[−] and Al₂Cl₇[−], while in the urea and acetamide compositions, we have the formation of [AlCl₂·(ligand)_n]⁺ cations, suggested to be involved in the aluminum deposition process.^[13–16] The Al deposition faradic efficiency, calculated for the second cycle, is 99.76% for EMIMCl:AlCl₃, 91.62% for Urea:AlCl₃ and 86.01% for Acetamide:AlCl₃. The comparison suggests the EMIMCl:AlCl₃-1:1.5 electrolyte as the most efficient media for the Al stripping deposition process.

Figures 3(a–b) show the voltage vs. time curves of galvanostatic cycling tests performed on symmetrical Al/Al cells using the three investigated electrolytes, carried to evaluate the long-term stability of the Al/electrolyte interphase in dynamic condition. The Al/EMIMCl:AlCl₃/Al cell (blue curve) has the lowest polarization, thus agreeing with the results reported in Figure 2. All the systems are characterized by stable overall overvoltage upon cycling, suggesting a stable Al/electrolyte interphase and an excellent capability to sustain long term cycling. In particular, the Urea:AlCl₃ system reveals a remarkable reduction of the cell overpotential during the first 5 days of measurement. This result is not in line with the CV reported in Figure 2c, where the current decreases upon cycling. The difference can be related to the different cell configuration and metal substrate used for the test. Figure 3c shows the comparison of the electrochemical stability of the three investigated electrolytes upon oxidation, evidencing the superior stability of the Urea:AlCl₃ system. The EMIMCl:AlCl₃ electrolyte also shows good stability, slightly inferior with respect to the Urea:AlCl₃, while the Acetamide:AlCl₃ shows the lowest stability, with a relevant current flow ($\geq 1 \mu\text{A cm}^{-2}$) starting already at 2.2 V vs. Al/Al³⁺.

The overall electrochemical characterization indicates the EMIMCl:AlCl₃ as the most efficient media for the Al stripping deposition process; however, the Urea:AlCl₃ electrolyte has

better electrochemical anodic stability. The better characteristics of the EMIMCl:AlCl₃ electrolyte can be addressed to its higher ionic conductivity and lower viscosity in comparison with the urea and acetamide based electrolytes (Table 1).

AGDICs have been assembled to better overview the characteristics of the electrolytes. Figure 4 reports the galvanostatic cycling evaluation of the three investigated electrolytes in AGDIC, employing natural graphite (NG) electrodes with relevant loading, i.e., $\approx 5 \text{ mg cm}^{-2}$. Figure 4a reports the voltage signature of the first (dis-)charge cycle, revealing that the three systems are operating at a different average discharge voltage; 1.91 V for the EMIMCl:AlCl₃, 1.73 V for the Acetamide:AlCl₃ and 1.77 V for the Urea:AlCl₃ (see Table 2). The higher discharge voltage of the cell using the EMIMCl:AlCl₃ can be attributed to the electrolyte's higher conductivity and a lower viscosity.^[5,17,19,22] Moreover, better Al stripping deposition properties of the EMIMCl:AlCl₃ can lead to improved performance. However, the different ionic speciation of DESs and the presence of [AlCl₂(ligand)₂]⁺ species may influence the operating voltage.^[17,22,26] The electrolyte composition has a relevant influence also in the AGDIC delivered capacity. The cell employing EMIMCl:AlCl₃ electrolyte shows the highest capacity ($\approx 110 \text{ mAh g}^{-1}$) with respect to the cells using Acetamide:AlCl₃ ($\approx 103 \text{ mAh g}^{-1}$) and Urea:AlCl₃ ($\approx 91 \text{ mAh g}^{-1}$) (Table 2). In this case, the different ionic speciation of the three electrolyte systems can also influence the formation of the graphite intercalation compounds (GIC), lowering the delivered capacity.^[17,22,26,27] The rate capability test reported in Figure 4b confirms the superior characteristics of the EMIMCl:AlCl₃ in respect to the other compositions. The cell employing EMIMCl:AlCl₃ electrolyte is only slightly affected by the current increase, while elevated current rate ($\geq 200 \text{ mA g}^{-1}$) substantially reduces the other cells' delivered capacity. The urea and acetamide based electrolytes maintain good performance at 200 mA g^{-1} , while at 1000 mA g^{-1} , the capacity drops to less than 45% of the reference one for the urea, and almost to zero for the acetamide. The cell's better rate capability using the EMIMCl:AlCl₃ can be attributed to the electrolyte's higher conductivity and lower viscosity (Table 1).^[5,17,19,22] Nonetheless, the urea composition shows the best columbic efficiency characteristic, as evidenced in Figure 4c, with values close to 100%.

Table 1. Viscosity, conductivity, and density of the EMIMCl:AlCl₃ 1:1.5, Urea:AlCl₃ 1:1.5, Acetamide:AlCl₃ 1:1.5 electrolytes. Data from Refs. [5,22,31–33].

Electrolyte composition	Viscosity [MPa s]		Conductivity [mS cm ^{−1}]		Density [g mL ^{−1}]		Ref.
	20 °C	60 °C	20 °C	60 °C	20 °C	60 °C	
EMIMCl AlCl ₃ 1:1.5	19.42	8.23	9.19	20.08	1.3408	1.3052	[31]
Urea AlCl ₃ 1:1.5	218	27	1.6	4.1	1.564	1.5921	[22,32]
Acetamide AlCl ₃ 1:1.5	116	23	0.6	2.9	1.484	1.525	[5,33]

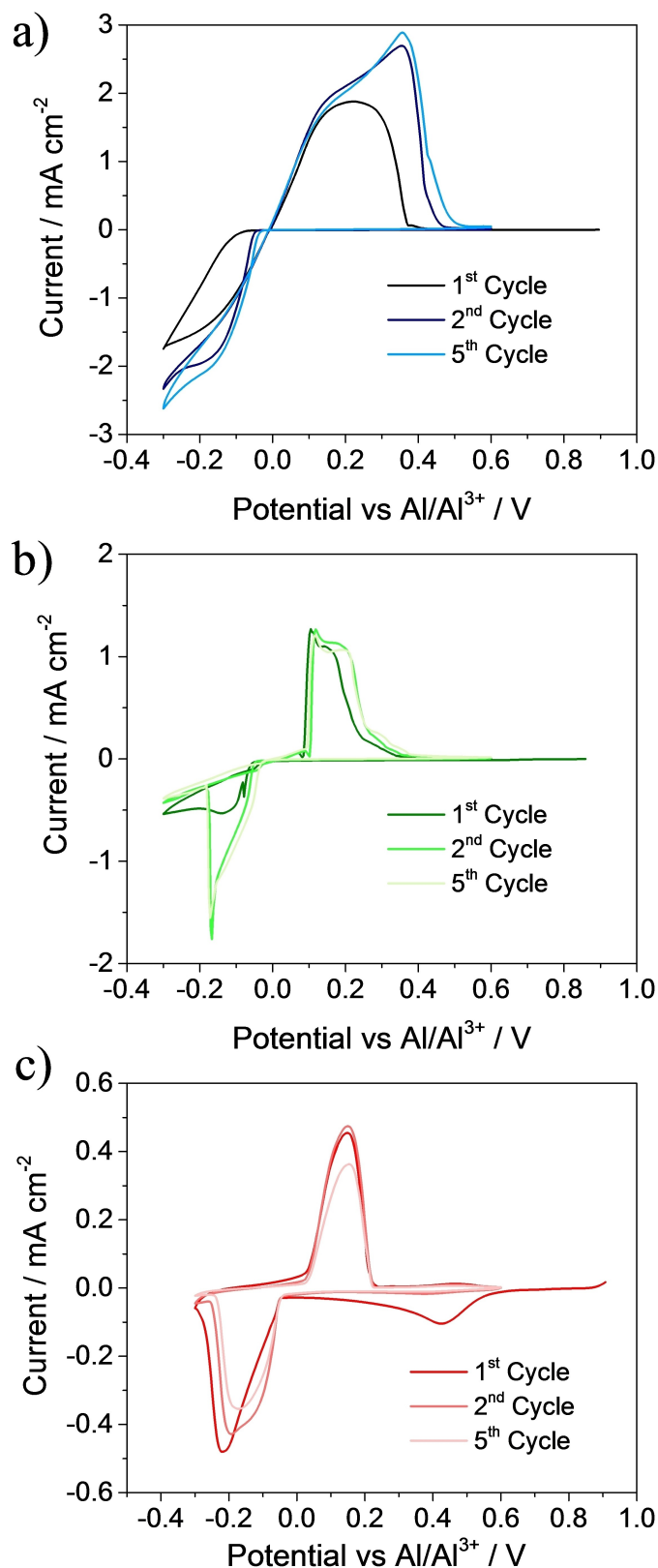


Figure 2. Cyclic voltammograms signatures obtained in a three-electrode configuration using Ni as working electrode and Al as counter and reference and employing a) EMIMCl:AlCl₃-1:1.5, b) Acetamide:AlCl₃-1:1.5, c) Urea:AlCl₃-1:1.5 electrolytes. Measurement obtained with a scan rate of 0.1 mVs⁻¹ at room T.

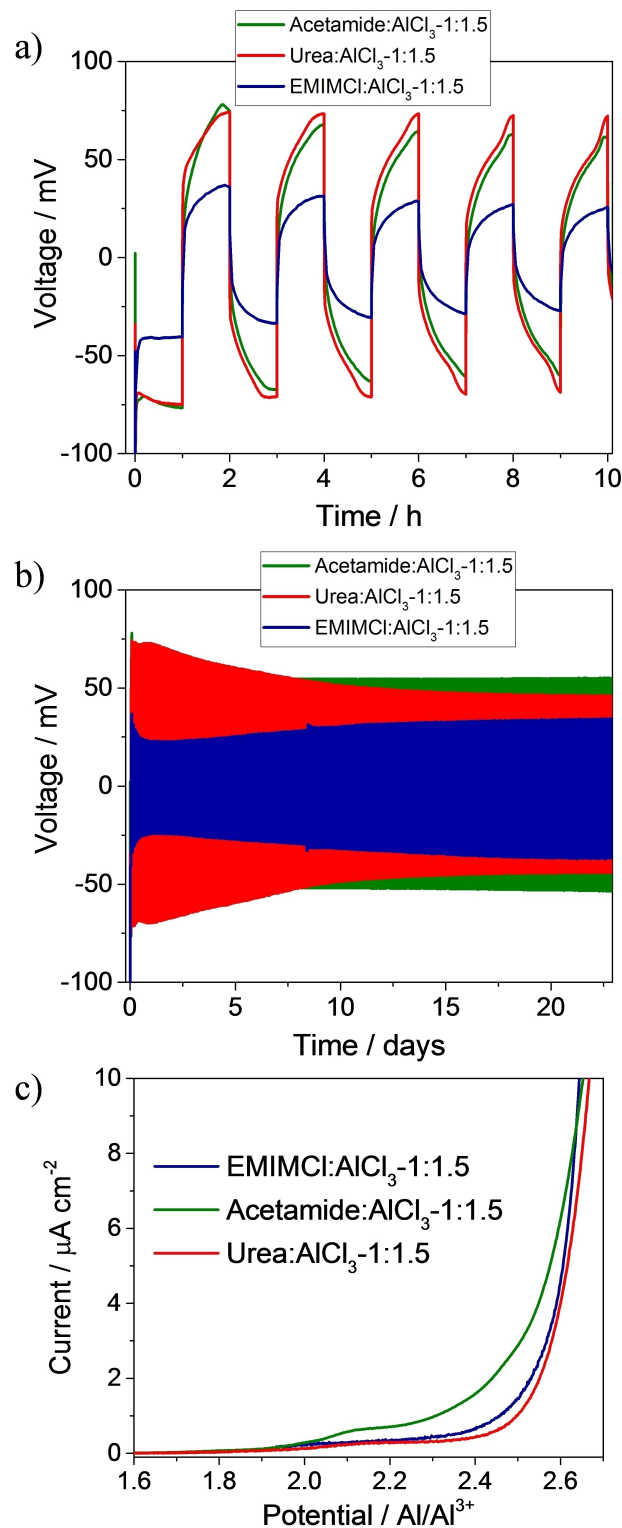


Figure 3. a–b) Voltage vs. time signature of the galvanostatic cycling test performed on symmetrical Al/Al cell using EMIMCl:AlCl₃-1:1.5 (in blue), Urea:AlCl₃-1:1.5 (in red) and Acetamide:AlCl₃-1:1.5 (in green) electrolytes. Measurement performed at 0.1 mA cm⁻² current, with a stripping deposition time of 1 h at room T. The test first 10 h are reported in (a), in (b) the full test performed for 24 days. c) Current vs. voltage signature of the linear sweep voltammogram test obtained in a three-electrode configuration using glassy carbon as working electrode and Al as counter and reference and employing EMIMCl:AlCl₃-1:1.5 (in blue), Urea:AlCl₃-1:1.5 (in red), and Acetamide:AlCl₃-1:1.5 (in green) electrolytes. Measurements obtained using a scan rate of 0.1 mVs⁻¹ at room T.

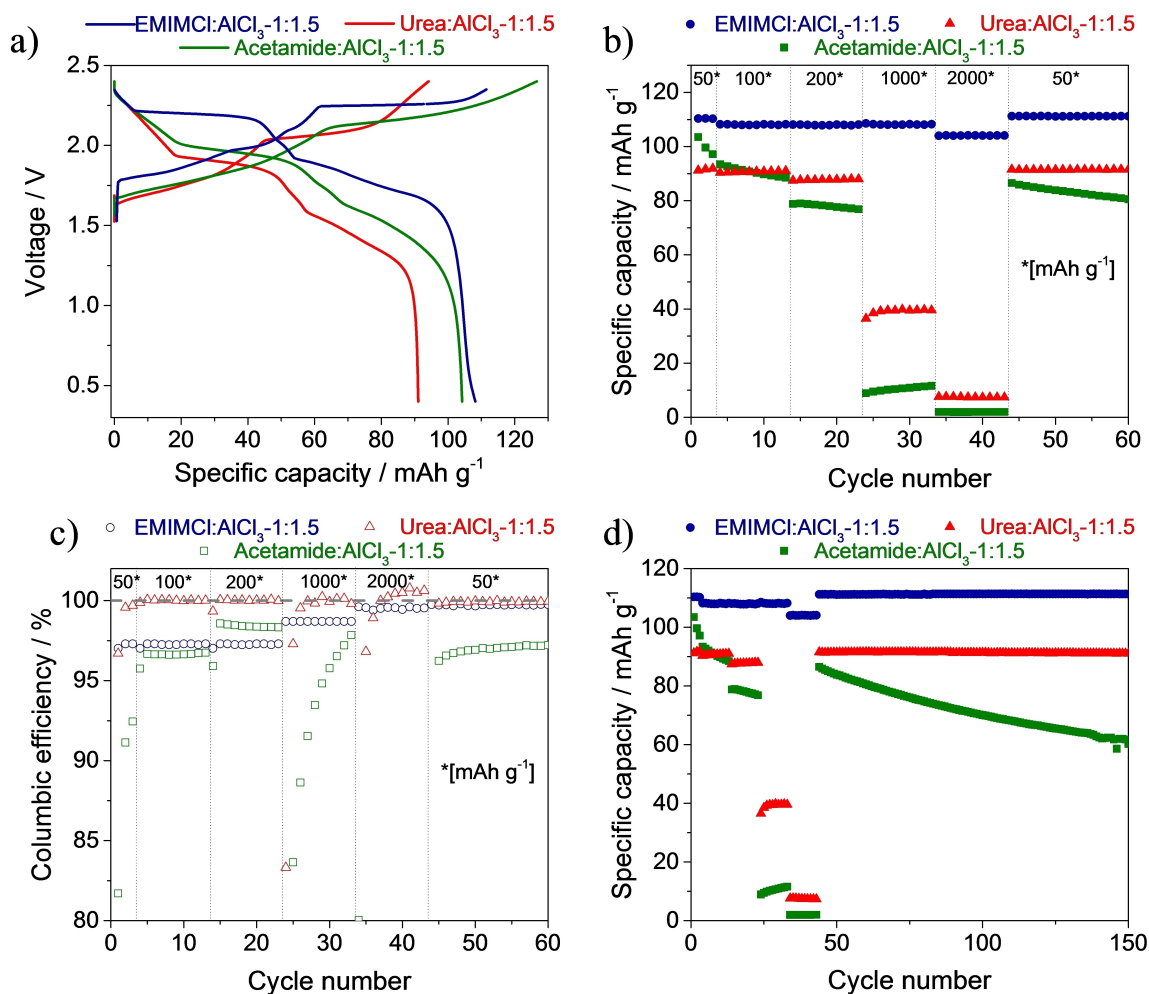


Figure 4. Galvanostatic cycling test results of Al/NG cells using EMIMCl:AlCl₃-1:1.5 (in blue), Urea:AlCl₃-1:1.5 (in red) and Acetamide:AlCl₃-1:1.5 (in green) electrolytes. a) First cycle voltage profile. b) Capacity vs. cycle number behavior of the multi-rate test. c) Coulombic efficiency vs. cycle number behavior of the multi-rate test. d) Extended cycling behavior results. Measurements obtained cycling the cells within the 0.4–2.4 V voltage window end employing specific currents of 50, 100, 200, 1000, 2000 mA g⁻¹ at room T.

Table 2. Discharge energy, average discharge voltage, cell polarization, energy efficiency, columbic efficiency, and discharge capacity of the 1st, 5th, and 100th cycle of the AGDICs using the three investigated electrolyte systems. The evaluation was obtained from the cycling test analysis reported in figure 3, for cycles performed at 50 mA g⁻¹ current.

Electrolyte composition	Cycle number	Discharge energy [Wh kg ⁻¹]	Average discharge voltage [V]	Polarization [V]	Energy efficiency [%]	Columbic efficiency [%]	Discharge capacity [mAh g ⁻¹]
EMIMCl AlCl ₃	1 st	206.60	1.91	0.16	90.43	97.02	110.37
	5 th	205.56	1.90	0.30	86.39	97.30	108.23
	100 th	211.66	1.90	0.24	88.63	99.76	111.39
Urea AlCl ₃	1 st	157.72	1.73	0.24	85.32	96.70	91.20
	5 th	152.94	1.69	0.27	86.14	100.06	90.49
	100 th	151.33	1.66	0.30	84.88	99.99	91.35
Acetamide AlCl ₃	1 st	184.83	1.77	0.26	71.88	81.70	103.49
	5 th	156.69	1.69	0.39	78.57	96.68	92.70
	100 th	103.05	1.47	0.71	66.11	97.84	70.08

The Acetamide:AlCl₃ system reports the lowest columbic efficiency (Table 2). The columbic efficiency behavior of the AGDICs links well with the anodic electrochemical stability of the various electrolytes (Figure 3c). The superior Urea:AlCl₃ stability against oxidation guarantees the best columbic

efficiency in AGDICs; result in agreement with other reports.^[17,22] The Acetamide:AlCl₃ system shows a columbic efficiency of about 96–97%, thus in line with this composition's lower anodic stability. The lower columbic efficiency of the Acetamide:AlCl₃ is reflected in the poor capacity retention in

Al/NG cells, retaining less than the 60% after 150 cycles (Figure 4d). On the contrary, EMIMCl:AlCl₃ and Urea:AlCl₃ does not evidence a relevant capacity decay during the test's 150 cycles.

3. Conclusions

The overall comparison between the standard EMIMCl:AlCl₃ electrolyte and Urea:AlCl₃ and Acetamide:AlCl₃ DES electrolytes has been reported. The comparison evidences the superior characteristics of the EMIMCl:AlCl₃ electrolyte as media for the Al stripping deposition process. Additionally, the standard EMIMCl:AlCl₃ electrolyte reveals better characteristics in AGDIBs in terms of rate capability. The better features of the EMIMCl:AlCl₃ over the Urea:AlCl₃ and Acetamide:AlCl₃ DES are mostly addressed to the former's lower viscosity and higher conductivity. However, AGDIBs employing Urea:AlCl₃ system have better columbic efficiency, around 99.9% for the urea with respect to the 97% of the EMIMCl:AlCl₃. Indeed this is beneficial for practical cell application where the amount of electrolyte is limited, and a columbic efficiency of 97% is impractical. Additionally, the urea-based electrolyte is expected to be characterized by lower cost, considering that urea is a very common chemical widely produced and used as fertilizer. Nonetheless, the elevated viscosity and low conductivity result in a significant limitation in the AGDIB system's best characteristics, the outstanding rate capability. Improvements in the DES attributes need to be achieved to push the concept to practical application consideration.

Experimental Section

The electrolytes prepared in a 1: 1.5-mol ratio, 1-ethyl-3-methylimidazolium chloride:aluminum trichloride (EMIMCl):AlCl₃, Urea:AlCl₃, and Acetamide:AlCl₃ are provided by IOLITEC. The water content of the electrolytes is lower than 100 ppm. The electrochemical measurements were performed using Teflon Swagelok® type T cells.^[6,28–30] All potentials quoted in this manuscript refer to the *quasi reference* Al/Al³⁺ electrode. The investigated electrolytes' capability to sustain the reversible aluminum stripping deposition process has been investigated by cyclic voltammetry (CV) of three-electrode cells using Ni foil as a working electrode and Al as counter and reference. The test has been performed at a scan rate of 0.1 mVs⁻¹ within the -0.3 V and 0.6 V vs. Al/Al³⁺ voltage window. The cycling stability of the aluminum metal in the various electrolytes was evaluated by continuous stripping/deposition tests on symmetrical Al/Al cells (Al 99.99% Alfa Aesar) employing a current of 0.1 mAcm⁻² and a stripping/deposition time of 1 h through a Maccor 4000 battery test system. The investigated electrolytes' anodic stability has been evaluated by linear sweep voltammetry (LSV) using a three-electrode cell comprising a glassy carbon working electrode and Al-metal as counter and reference. The measurements have been performed using a scan rate of 0.1 mVs⁻¹. The evaluation of the investigated electrolytes' electrochemical behavior in Al cells has been performed assembling AGDIBs comprising natural graphite (NG) positive electrodes. The natural graphite powder (NG) was provided by PLANO GmbH. NG electrodes with a loading of about 5 mg cm⁻² have been employed for the electrochemical characterization. The detailed electrode

preparation procedure has been described in our previous paper.^[11] The cycling test of the Al/NG cells has been performed using a multi-rate procedure using 50, 100, 200, 1000, 2000 mA g⁻¹ within the 0.4–2.4 voltage window. The specific capacity and current are referred to the mass of the graphite.

Acknowledgments

The European Commission funded this research within the H2020 ALION project under contract 646286 and the German Federal Ministry of Education and Research in the AISiBat project under contract 03SF0486 and the project ALIBATT under contract 03XP0128E. Open access funding enabled and organized by Projekt DEAL.

Conflict of Interest

The authors declare no conflict of interest.

- [1] D. Larcher, J.-M. Tarascon, *Nat. Chem.* **2015**, *7*, 19.
- [2] G. A. Elia, K. Marquardt, K. Hoepfner, S. Fantini, R. Lin, E. Knipping, W. Peters, J.-F. Drillet, S. Passerini, R. Hahn, *Adv. Mater.* **2016**, *28*, 7564.
- [3] G. A. Elia, K. V. Kravchik, M. V. Kovalenko, J. Chacón, A. Holland, R. G. A. Wills, *J. Power Sources* **2021**.
- [4] M.-C. Lin, M. Gong, B. Lu, Y. Wu, D.-Y. Wang, M. Guan, M. Angell, C. Chen, J. Yang, B.-J. Hwang, H. Dai, *Nature* **2015**, *520*, 324.
- [5] J. Lampkin, H. Li, L. Furness, R. Raccichini, N. Garcia-Araez, *ChemSusChem* **2020**, *13*, 3514.
- [6] W. Wang, Z. Cao, G. A. Elia, Y. Wu, W. Wahyudi, E. Abou-Hamad, A.-H. Emwas, L. Cavallo, L.-J. Li, J. Ming, *ACS Energy Lett.* **2018**, *3*, 2899.
- [7] J. Bitenc, N. Lindahl, A. Vizintin, M. E. Abdelhamid, R. Dominko, P. Johansson, *Energy Storage Mater.* **2020**, *24*, 379.
- [8] M. Walter, K. V. Kravchik, C. Böfer, R. Widmer, M. V. Kovalenko, *Adv. Mater.* **2018**, *30*, 1.
- [9] S. Wang, K. V. Kravchik, A. N. Filippin, U. Müller, A. N. Tiwari, S. Buecheler, M. I. Bodnarchuk, M. V. Kovalenko, *Adv. Sci.* **2018**, *5*, 1700712.
- [10] S. Wang, K. V. Kravchik, F. Krumeich, M. V. Kovalenko, *ACS Appl. Mater. Interfaces* **2017**, *9*, 28478.
- [11] G. A. Elia, N. A. Kyeremateng, K. Marquardt, R. Hahn, *Batteries Supercaps* **2019**, *2*, 83.
- [12] G. A. Elia, G. Greco, P. H. Kamm, F. Garcia-Moreno, S. Raoux, R. Hahn, *Adv. Funct. Mater.* **2020**, 2003913.
- [13] H. M. A. Abood, A. P. Abbott, A. D. Ballantyne, K. S. Ryder, *Chem. Commun.* **2011**, *47*, 3523.
- [14] Y. Fang, K. Yoshii, X. Jiang, X.-G. Sun, T. Tsuda, N. Mehio, S. Dai, *Electrochim. Acta* **2015**, *160*, 82.
- [15] G. Pulletikurthi, B. Bödecker, A. Borodin, B. Weidenfeller, F. Endres, *Prog. Nat. Sci. Mater. Int.* **2015**, *25*, 603.
- [16] Y. Fang, X. Jiang, X.-G. Sun, S. Dai, *Chem. Commun.* **2015**, *51*, 13286.
- [17] M. Angell, C.-J. Pan, Y. Rong, C. Yuan, M.-C. Lin, B.-J. Hwang, H. Dai, *Proc. Natl. Acad. Sci.* **2017**, *114*, 834.
- [18] H. Jiao, C. Wang, J. Tu, D. Tian, S. Jiao, *Chem. Commun.* **2017**, *53*, 2331.
- [19] J. Li, J. Tu, H. Jiao, C. Wang, S. Jiao, *J. Electrochem. Soc.* **2017**, *164*, A3093.
- [20] Y. Bian, Y. Li, Z. Yu, H. Chen, K. Du, C. Qiu, G. Zhang, Z. Lv, M.-C. Lin, *ChemElectroChem* **2018**, *5*, 3607.
- [21] C. Xu, J. Li, H. Chen, J. Zhang, *ChemNanoMat* **2019**, *5*, 1367.
- [22] M. Angell, G. Zhu, M. Lin, Y. Rong, H. Dai, *Adv. Funct. Mater.* **2020**, *30*, 1901928.
- [23] H. Xu, T. Bai, H. Chen, F. Guo, J. Xi, T. Huang, S. Cai, X. Chu, J. Ling, W. Gao, Z. Xu, C. Gao, *Energy Storage Mater.* **2019**, *17*, 38.
- [24] C. Li, J. Patra, J. Li, P. C. Rath, M. H. Lin, J. K. Chang, *Adv. Funct. Mater.* **2020**, *30*, 1.
- [25] L. R. Bard, J. Allen and Faulkner, *Electrochemical Methods: Fundamentals and Applications*; Wiley, **2001**.

- [26] H. M. A. Abood, A. P. Abbott, A. D. Ballantyne, K. S. Ryder, *Chem. Commun.* **2011**, 47, 3523.
- [27] G. A. Elia, G. Greco, P. H. Kamm, F. García-Moreno, S. Raoux, R. Hahn, *Adv. Funct. Mater.* **2020**, 2003913.
- [28] G. A. Elia, I. Hasa, G. Greco, T. Diemant, K. Marquardt, K. Hoepfner, R. J. Behm, A. Hoell, S. Passerini, R. Hahn, *J. Mater. Chem. A* **2017**, 5, 9682.
- [29] G. Greco, D. Tatchev, A. Hoell, M. Krumrey, S. Raoux, R. Hahn, G. A. Elia, *J. Mater. Chem. A* **2018**, 6, 22673.
- [30] G. A. Elia, J.-B. Ducros, D. Sotta, V. Delhorbe, A. Brun, K. Marquardt, R. Hahn, *ACS Appl. Mater. Interfaces* **2017**, 9, 38381.
- [31] Y. Zheng, K. Dong, Q. Wang, J. Zhang, X. Lu, *J. Chem. Eng. Data* **2013**, 58, 32.
- [32] C. Liu, W. Chen, Z. Wu, B. Gao, X. Hu, Z. Shi, Z. Wang, *J. Mol. Liq.* **2017**, 247, 57.
- [33] P. Hu, W. Jiang, L. Zhong, S. Zhou, *Chin. J. Chem. Eng.* **2019**, 27, 144.

Manuscript received: October 13, 2020
Revised manuscript received: November 6, 2020
Accepted manuscript online: November 6, 2020
Version of record online: November 23, 2020