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Article

# Convective Heat Transfer Enhancement through Laser-Etched Heat Sinks: Elliptic Scale-Roughened and Cones Patterns

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**Abstract:** The efficient dissipation of localized heat flux by convection is a key request in several engineering applications, especially electronic ones. The recent advancements in manufacturing processes are unlocking the design and industrialization of heat exchangers with unprecedented geometric characteristics and, thus, performance. In this work, laser etching manufacturing technique is employed to develop metal surfaces with designed microstructured surface patterns. Such precise control of the solid-air interface (*artificial roughness*) allows to manufacture metal heat sinks with enhanced thermal transmittance with respect to traditional flat surfaces. Here, the thermal performance of these laser-etched devices is experimentally assessed by means of a wind tunnel in a fully turbulent regime. At the highest Reynolds number tested in the experiments ( $Re_L \approx 16,500$ ), elliptic scale-roughened surfaces show thermal transmittances improved by up to 81% with respect to heat sinks with flat surface. At similar testing conditions, cones patterns provide an enhancement in Nusselt number and thermal transmittance of up to 102% and 357%, respectively. The latter results are correlated with the main geometric and thermal fluid dynamics descriptors of the convective heat transfer process in order to achieve a predictive model of their performance. The experimental evidence shown in this work may encourage and guide a broader use of micro-patterned surfaces for enhancing convective heat transfer in heat exchangers.

**Keywords:** convective heat transfer; heat transfer enhancement; heat sink; electronics cooling; microstructured surface; laser etching

## 1. Introduction

The heat dissipation in electronic devices has substantial importance because it significantly affects performance, eventually leading to malfunctioning or failures if not correctly managed [1]. In fact, the operating temperature of electronic systems, which is usually regulated by proper cooling technologies, influences the length of their trouble-free operation and durability. Nowadays, electronic equipment such as microprocessors or batteries produce increasingly higher quantities of waste heat [2,3]. At the same time, the progressive reduction in size of electronic devices implies less space available for cooling purposes. While these factors indicate an improvement in electronics

performance and usability, they have stimulated the investigation of more efficient heat dissipation technologies in miniaturized applications [4,5].

Heat sinks are devices allowing to transfer the heat generated by mechanical or electrical equipment to a fluid, e.g., gas or liquid coolants, thus managing to regulate their temperature at optimal levels [6]. Heat sinks are typically made of copper or aluminum and are designed to maximize the surface in contact with the cooling medium, aiming to optimize the heat exchange. These heat exchangers are widely used with high-performing microprocessors [7], high-power semiconductor devices (e.g., power transistors [8]), and optoelectronics (e.g., lasers and light emitting diodes [9]) to dissipate the heat generated during their operation.

Several coolants have been employed with heat sinks, namely gas [10], liquid [11,12], or two-phase [13,14] ones, as well as nanofluids [15,16]. Even if solutions with liquid and phase-change coolants have been proved to be very efficient, their use in commercial appliances widely spread on the market is limited by the cost and complexity. Instead, air-based cooling solutions are generally more suitable for everyday devices, thanks to their reliability and cheapness. Among this category, innovative configurations have been lately studied to enhance the heat transfer capability and include the use of unshrouded plate fins [10], pin fin arrays [17,18], ribs [19–21], dimples [22,23], carbon nanotubes structures [24], arrays of protrusions [25,26], Pitot tubes [27], innovative roughened surfaces [28,29], porous media [30,31], phase-change materials [32,33], or metal foams [34,35].

Recent innovations in the field of manufacturing are allowing the design of heat sinks with unprecedented geometries and surface features [36]. Heat sinks with enhanced thermal performance given by micro-protruded patterns and artificial roughness have been lately manufactured by direct metal laser sintering (DMLS). For example, we have experimentally demonstrated that both flat and finned heat sinks can be produced by DMLS with controllable surface roughness, and this leads to augmented convective heat transfer coefficients with respect to the typically smooth surfaces obtained by milling or extrusion processes [37,38]. In detail, DMLS technique allows to obtain an average surface roughness of up to 36  $\mu\text{m}$  (far superior to standard milling, i.e., 1  $\mu\text{m}$ ), which provides an improvement in the convective heat transfer coefficient of up to 73% and 40% (compared to milled samples) for flat and finned heat sinks, respectively [37]. Laser etching is another promising manufacturing technique. In this process, a galvanometric head is used to precisely control the position of a laser beam, which focuses its radiation to a micro-sized spot. Thanks to this manufacturing technique, a broad variety of microstructured patterns can be engraved on metal surfaces at relatively low operating costs [39]. Laser etching has been previously employed to manufacture metal heat sinks with micro-fins characterized by lengths in the range 200–1100  $\mu\text{m}$ , which showed enhanced convective heat transfer coefficient with respect to smooth heat sinks [40].

The present work is focused on the experimental test and model prediction of the thermal transmittance of surface micro-patterned copper heat sinks manufactured by laser etching. Two sets of surface patterns are assessed following a proper design of experiments, namely elliptic scale roughened-surfaces (ESR) and cones ones, with different geometric characteristics. On the one side, while ESR samples have been object of some investigations in the recent literature [41,42] in the channel flow configuration, here, a flush-mounted configuration is studied experimentally for the first time. On the other side, to the best of our knowledge, heat sinks with cones microstructures on the surface have been first proposed in this work. The target is to evaluate whether and by how much the use of these designed micro-patterns increases the convective heat exchange through flush-mounted heat sinks and to correlate their thermal transmittance with the geometric and thermal fluid dynamics characteristics of the heat transfer process.

## 2. Materials and Methods

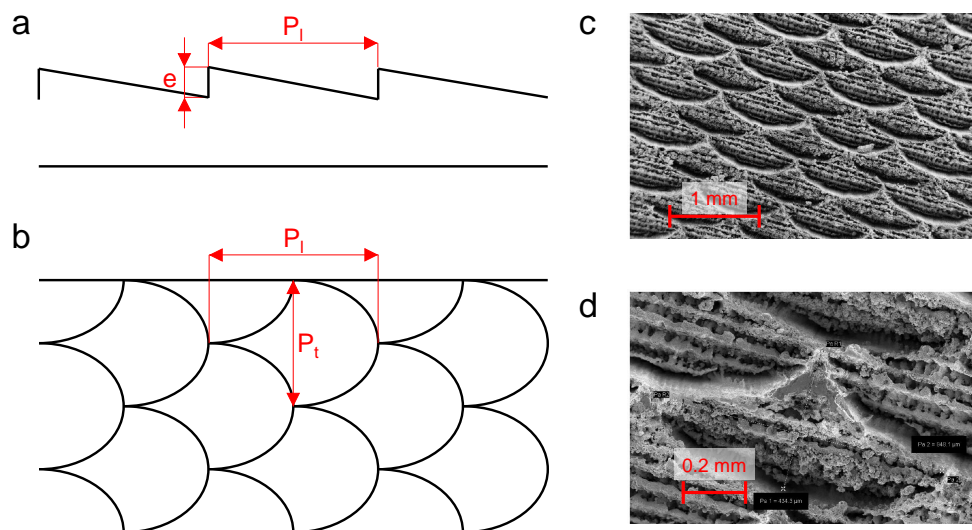
Smooth copper samples with  $11.1 \times 11.1 \times 5 \text{ mm}^3$  size and  $11.1 \times 11.1 \text{ mm}^2$  heat transfer surface ( $A_H$ ) are engraved with microstructured patterns by laser etching. A diode-pumped solid-state (DPSS) laser system characterized by emission at 532 nm, 10 W power, 25  $\mu\text{m}$  spot size, and  $3000 \text{ mm s}^{-1}$

scan speed has been employed for the laser etching process by Microla Optoelectronics S.r.l. [40]. Short pulse duration (nanoseconds) are employed to achieve a good match between the desired geometric characteristics and the real sample.

The geometric design parameters of both ESR and cones patterns have been chosen according to a suitable design of experiment (DoE). In particular, the Taguchi method has been applied to reduce the number of tests at the minimum while obtaining the maximum information about the geometric factors of the patterns that affect the convective heat transfer process [43]. Hence, nine samples with ESR micro-patterns and nine with cones micro-patterns have been designed, manufactured, and tested. The convective heat transfer coefficient of each sample has been experimentally evaluated in the flush-mounted configuration in a calibrated wind tunnel.

### 2.1. Elliptic Scale-Roughened Patterns

The general geometric configuration of the ESR (also known as *shark skin-like*) surface is depicted in Figure 1a,b. The design parameters of this pattern are the longitudinal ( $P_l$ ) and transverse ( $P_t$ ) axes of the ellipse and the maximum height of the scale ( $e$ ). In Figure 1c,d, the geometric configuration of a representative ESR sample as captured by field emission scanning electron microscopy (FESEM) is reported (ZEISS SUPRA 40).



**Figure 1.** Elliptic scale-roughened patterns: (a) Schematics of the lateral and (b) top view of the elliptic scale roughened-surface (ESR) pattern. (c) Image of the laser-etched ESR pattern as obtained by field emission scanning electron microscopy (FESEM) at 100 $\times$  and (d) 350 $\times$  magnification: The FESEM pictures are provided by Microla Optoelectronics S.r.l., using 30  $\mu\text{m}$  aperture size, 5 mm working distance, and 5 kV electron high tension.

The Taguchi method [44] is employed for defining the most adequate set of geometric characteristics of the ESR patterned samples to be tested. To improve the generality of the analysis, the following three dimensionless parameters have been considered in the design of experiments:  $r_p$ , the eccentricity of the ellipse;  $A/A_n$ , the ratio between the heat transfer surface of the ESR patterned sample ( $A$ ) and that of the smooth one ( $A_n$ ); and  $V/(AY_0)$ , the ratio between the volume of the specimen ( $V$ ) and the product between the heat transfer surface and average viscous length ( $Y_0$ ) [45] for the tested flush-mounted configuration.

The ratio  $r_p$  represents the eccentricity of the elliptic cell of the shark-like pattern, namely

$$r_p = \frac{P_l}{P_t}. \quad (1)$$

Low values of  $r_p$  correspond to elongated scale configurations, and high values correspond to squeezed ones.

The ratio  $A/A_n$  quantifies the heat transfer surface augmentation provided by the laser etching process compared to the initial smooth surface of the sample, and it can be calculated from the geometry of the pattern as

$$\frac{A}{A_n} = 1 + \pi \left( \frac{3}{8} \frac{P_t + P_l}{P_t P_l} - \frac{1}{4\sqrt{P_t P_l}} \right) e, \tag{2}$$

where  $A/A_n \geq 1$ .

The third dimensionless parameter  $V/(AY_0)$ , instead, can be geometrically computed as

$$\frac{V}{AY_0} = \frac{\left(\frac{3}{4} - \frac{\pi}{8}\right) e}{\left[1 + \pi e \left(\frac{3}{8} \frac{P_t + P_l}{P_t P_l} - \frac{1}{4\sqrt{P_t P_l}}\right)\right] Y_0} \tag{3}$$

for the considered ESR patterns. Notice that  $V/A$  indicates the amount of material used for the sample realization with respect to the actual area available for heat dissipation in the flush-mounted configuration: low values of this ratio indicate a small amount of material for the specimen realization, thus leading to lower costs. The average viscous length ( $Y_0$ ) can be calculated as the mean value of the viscous length ( $y_0$ ) over the range of fluid flows assessed in the experiments [46], that is

$$Y_0 = \frac{1}{Re_{D,max} - Re_{D,min}} \int_{Re_{D,min}}^{Re_{D,max}} y_0(Re_D) dRe_D, \tag{4}$$

where

$$Re_D = \frac{uD}{\nu}, \tag{5}$$

where  $D$  is the hydraulic diameter of the wind tunnel [47] and  $\nu$  is the kinematic viscosity of the fluid.

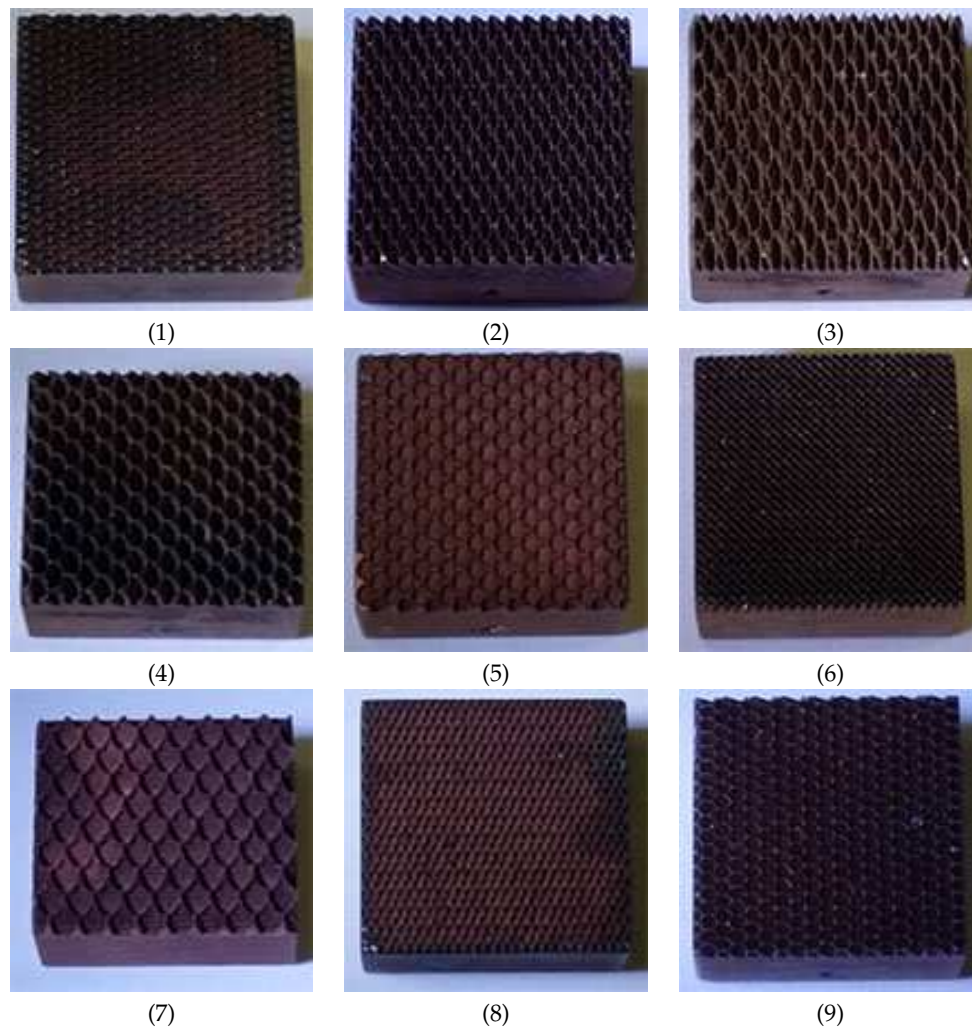
Following the Taguchi method (3 parameters, 3 levels, and 9 tests), we define an adequate design of experiments by considering the possible levels of  $r_p$ ,  $A/A_n$ , and  $V/(AY_0)$  reported in Table 1. As a result, Table 2 shows the full experimental configuration for the nine manufactured samples, which are also depicted in Figure 2.

**Table 1.** Considered levels of parameters for the design of experiments of the ESR patterned samples.

Parameter Level	$r_p$	$A/A_n$	$V/(AY_0)$
Low	0.500	1.700	1.193
Medium	1.000	2.050	2.087
High	2.000	2.400	2.982

**Table 2.** Design parameters and geometric characteristics of the ESR patterned samples manufactured by laser etching technique: The characteristics of the samples have been defined according to the Taguchi method and the target levels in Table 1.

Sample	$r_p$	$A/A_n$	$V/(AY_0)$	$e$ [mm]	$P_t$ [mm]	$P_l$ [mm]
1	0.509	1.648	1.229	0.285	1.052	0.535
2	0.526	1.975	2.098	0.583	1.396	0.734
3	0.543	2.254	3.103	0.984	1.790	0.972
4	0.998	1.693	2.161	0.515	1.167	1.165
5	1.003	1.965	2.922	0.808	1.312	1.316
6	1.054	2.416	1.250	0.425	0.459	0.484
7	2.012	1.731	2.804	0.683	1.130	2.274
8	1.961	1.945	1.228	0.336	0.433	0.849
9	1.987	2.318	2.085	0.680	0.626	1.244



**Figure 2.** Pictures of the nine ESR patterned samples manufactured by laser etching technique.

## 2.2. Cones Patterns

The general geometric configuration of cones patterned surface is depicted in Figure 3a,b. The design parameters of this pattern are the height ( $H$ ) and radius ( $r$ ) of the cones and the pitch ( $p$ ). In Figure 3c,d, the geometric configuration of a representative surface covered by cones as captured by FESEM is reported.

Again, the generality of the analysis is pursued by introducing three dimensionless parameters of the cones patterned samples:  $\lambda_p$  (the plane solidity),  $A/A_n$ , and  $V/(AY_0)$ .

The plane solidity quantifies the density of the cones with respect to the available surface, being defined as the fraction of the smooth surface area covered by protrusions:

$$\lambda_p = \frac{\pi r^2}{3p^2}. \quad (6)$$

where  $\lambda_p$  is expected to strongly influence the convective heat transfer mechanism: low values should lead to enhanced heat transfer due to perturbation of the boundary layer, whereas high values should cause stagnation phenomena, thus inducing a reduction in the convection [48].

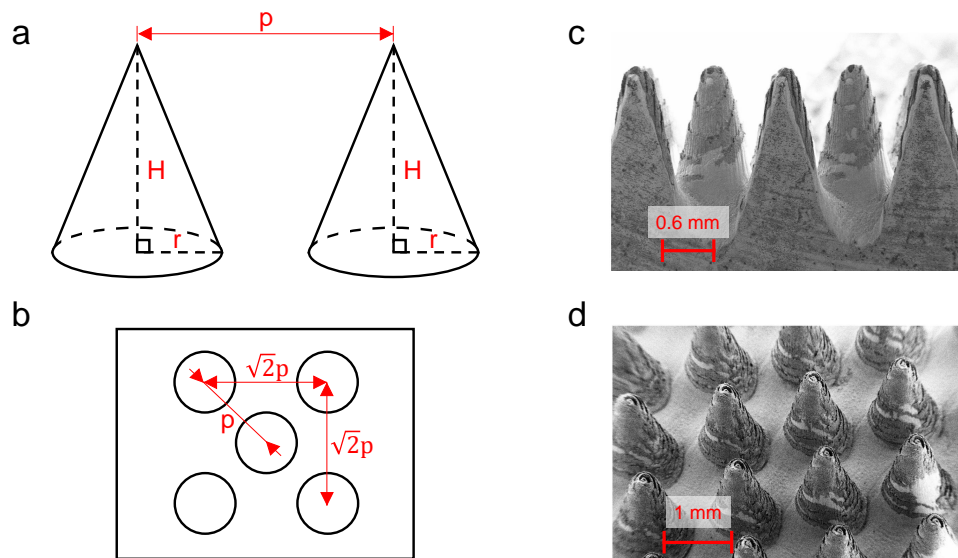
The other parameters are defined similarly to what was previously discussed regarding the ESR patterns. In this case, the parameter  $A/A_n$  can be computed from the geometry of the pattern as

$$\frac{A}{A_n} = \frac{\pi r \sqrt{r^2 + H^2} + p^2 - \pi r^2}{p^2}, \quad (7)$$



while the parameter  $V/(AY_0)$  as

$$\frac{V}{AY_0} = \frac{\pi r^2 H}{(3\pi r\sqrt{r^2 + H^2} + 3p^2 - 3\pi r^2) Y_0}. \quad (8)$$



**Figure 3.** Cones patterns: (a) Schematics of the lateral and (b) top view of the cones pattern. (c) Image of laser-etched cones pattern as obtained by FESEM at  $100\times$  and (d)  $74\times$  magnification: The FESEM pictures are provided by Microla Optoelectronics S.r.l., using  $30\ \mu\text{m}$  aperture size, 7 mm (panel c) and 10 mm (panel d) working distance, and 5 kV electron high tension.

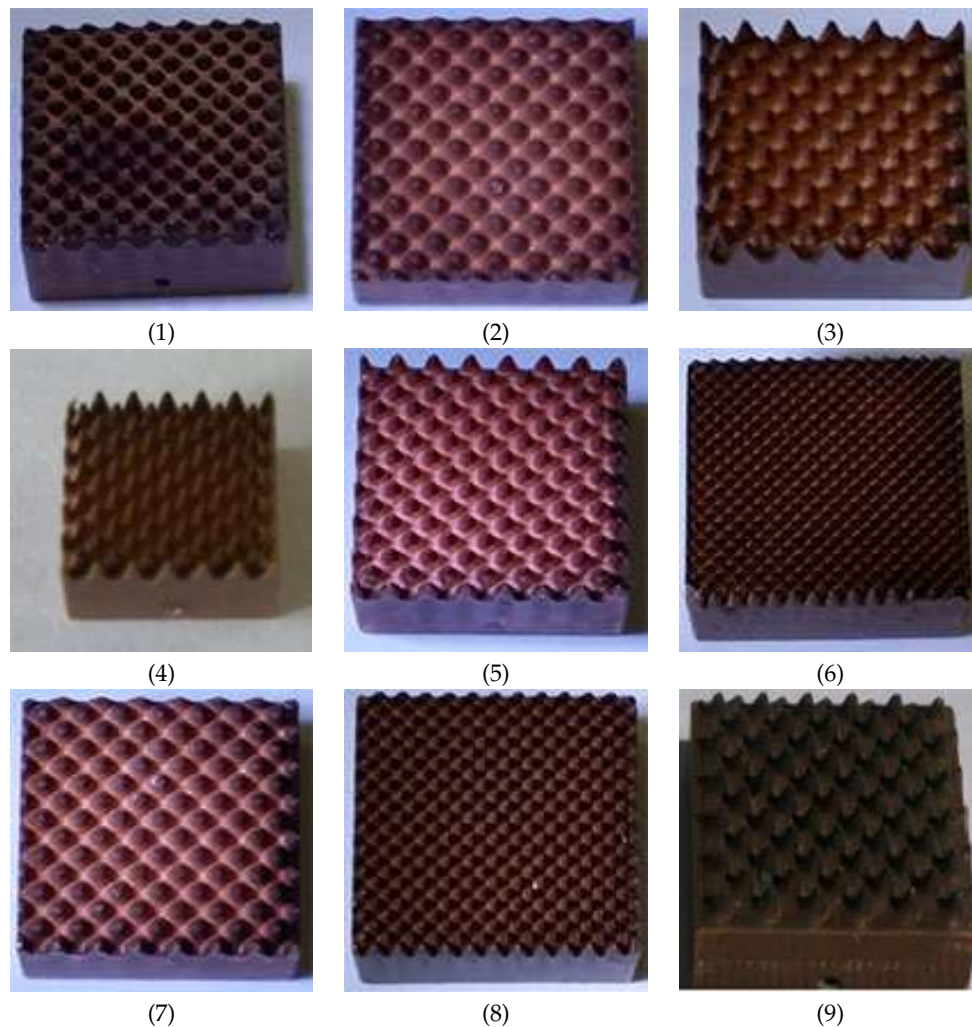
Following the Taguchi method (3 parameters, 3 levels, and 9 tests), we define an adequate design of experiments by considering the possible levels of  $\lambda_p$ ,  $A/A_n$ , and  $V/(AY_0)$  reported in Table 3. As a result, Table 4 and Figure 4 show the actual configuration of the nine manufactured samples.

**Table 3.** Parameters levels for cones samples.

Parameter Level	$\lambda_p$	$A/A_n$	$V/(AY_0)$
Low	0.15	1.50	1.39
Medium	0.21	2.20	1.99
High	0.26	3.00	2.58

**Table 4.** Design parameters and geometric characteristics of the cones patterned samples manufactured by laser etching technique: The characteristics of the samples have been defined according to the Taguchi method and the target levels in Table 3.

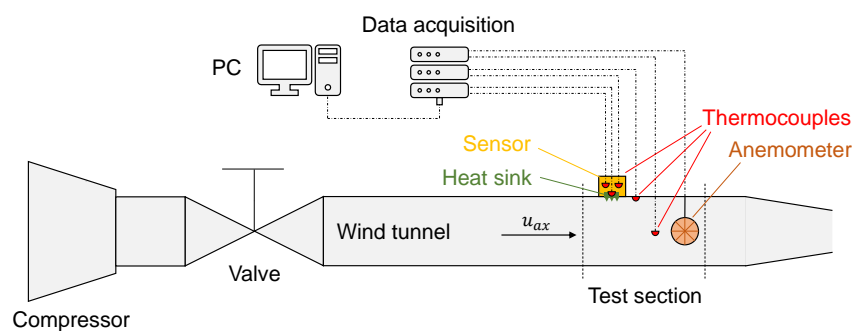
Sample	$\lambda_p$	$A/A_n$	$V/(AY_0)$	$H$ [mm]	$r$ [mm]	$p$ [mm]
1	0.186	1.565	1.650	0.700	0.400	0.950
2	0.174	2.354	2.131	1.450	0.420	1.030
3	0.180	2.954	2.786	2.300	0.510	1.230
4	0.229	1.480	2.155	0.700	0.510	1.090
5	0.223	2.433	2.605	1.430	0.480	1.040
6	0.234	3.165	1.513	1.030	0.260	0.550
7	0.247	1.487	2.315	0.700	0.530	1.080
8	0.270	2.928	1.836	1.000	0.310	0.610
9	0.147	1.714	2.048	1.200	0.496	1.323



**Figure 4.** Pictures of the nine cones patterned samples manufactured by laser etching technique.

### 2.3. Experimental Setup

The convective heat transfer coefficient ( $h$ ) of the flush-mounted ESR and cones patterned samples has been assessed in a wind tunnel calibrated in previous works [38,47] (see the schematic in Figure 5). The wind tunnel facility includes a 5 m long, 228 mm high, and 158 mm wide channel entirely made of steel. The length of the channel is approximately equal to 26 hydraulic diameters, being  $D \cong 187$  mm.



**Figure 5.** Schematic view of the experimental test rig for measuring the convective heat transfer coefficient of the flush-mounted heat sinks at varying Reynolds number.



The axial velocity of the air flow ( $u_{ax}$ ) is measured by a vane anemometer, which is installed right downstream the tested sample. The convective heat transfer coefficient is measured thanks to a sensor based on the concept of thermal guard, of which the complete description is given in Reference [47]. This sensor is composed by a copper box of 20.0 mm  $\times$  20.0 mm  $\times$  8.0 mm, named guard, with a squared and centered hole of 11.1 mm  $\times$  11.1 mm  $\times$  5.0 mm that accommodates the tested sample. The guard is maintained at the same temperature of the tested sample by a first controllable electrical heater. In this way, the heat—which is provided by a second controllable electrical heater placed on the back side of the sample—can only flow through the sample, therefore allowing a precise measure of the convective heat transfer coefficient. Alignment and mounting procedures of the sensor inside the wind tunnel are reported in Reference [38]. Five type K thermocouples monitor the temperatures in the test rig: two for the guard and one each for the sample, the inner wall of the wind tunnel and the air. The coefficient  $h$  can be finally computed from these measured temperatures following the protocol established in Reference [47].

### 3. Results

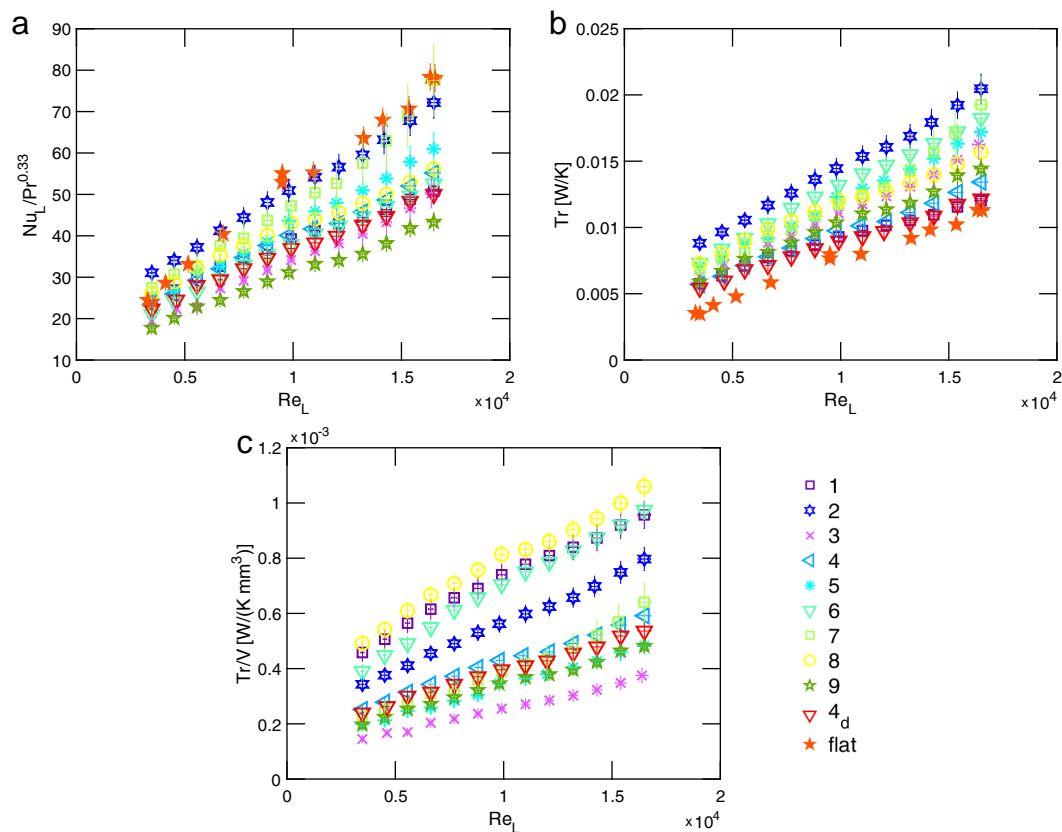
The thermal performance of the laser-etched heat sinks can be conveniently described as a function of the typical dimensionless numbers adopted for convective heat transfer.

The measured air velocity in the tunnel is employed to compute the Reynolds number  $Re_D^{ax} = u_{ax}D/\nu$ , with  $\nu = 1.544 \times 10^{-5} \text{ m}^2 \text{ s}^{-1}$ . Then, the Reynolds number based on the average air velocity is estimated as  $Re_D = uD/\nu = 0.694(Re_D^{ax})^{1.0162}$  in the adopted test rig [47]. In case of flush-mounted heat sinks, the Reynolds number can be also referred to as the heated edge ( $L = 20 \text{ mm}$ , namely the heated edge of the guard) [46]. In the considered experimental conditions, first,  $Re_L^{ax} = u_{ax}L/\nu$  is computed, then, the Reynolds number referred to as the heated edge and average air velocity is estimated as  $Re_L = uL/\nu = 0.669(Re_L^{ax})^{1.0162}$  [47]. Experiments have been carried out with  $Re_L$  in a range approximately equal to 3500–16,500, with an average viscous length equal to  $Y_0 = 50.3 \text{ }\mu\text{m}$  (see Reference [46] for calculation details).

The experimental thermal performance of the heat sinks are expressed here in terms of  $Nu_L/Pr^{0.33}$ ,  $Tr = hA$  (thermal transmittance), and  $Tr/V$ . In detail,  $Nu_L/Pr^{0.33}$  is the ratio between the dimensionless Nusselt ( $Nu_L = hL/\lambda$ ) and Prandtl ( $Pr = \nu/\alpha$ ) numbers, where  $\lambda = 2.622 \times 10^{-2} \text{ W m}^{-1} \text{ K}^{-1}$  is the thermal conductivity of air and  $\alpha = 2.224 \times 10^{-5} \text{ m}^2 \text{ s}^{-1}$  is its thermal diffusivity. The reported error bars of measures refer to both type A and type B uncertainties, calculated according to Reference [38] with significance level equal to 5%.

#### 3.1. Elliptic Scale-Roughened Patterns

All elliptic scale-roughened samples have been tested with the air flowing along the forward direction, i.e.,  $u_{ax}$  directed from left to right in Figure 1a,b, since this orientation has previously demonstrated to achieve higher heat transfer rates [41]. Figure 6 shows the values obtained for  $Nu_L/Pr^{0.33}$ ,  $Tr$ , and  $Tr/V$  at different Reynolds number. As expected, the thermal transmittance of the laser-etched samples is higher than the smooth one, with  $Tr$  enhancements up to 81% for the best performing configuration (sample 2 at  $Re_L = 16,500$ ; see Figure 6b). However, the observed enhancement should be mainly ascribed to the larger heat transfer surface of laser-etched samples ( $A$ ) with respect to the flat one ( $A_n$ ) and not to higher convective heat transfer coefficients.



**Figure 6.** Experimental performance of heat sinks with ESR—shark-skin like—surface patterns at different Reynolds number: (a) Ratio between Nusselt and Prandtl numbers,  $Nu_L/Pr^{0.33}$ ; (b) thermal transmittance,  $Tr$ ; and (c) ratio between thermal transmittance and sample volume,  $Tr/V$ . In the legend, the number of each sample is associated with a symbol; “4d” indicates sample 4 tested in the downward direction with respect to the air flow one (all other points are obtained in the forward direction) and “flat” stands for the reference heat sink with a smooth surface.

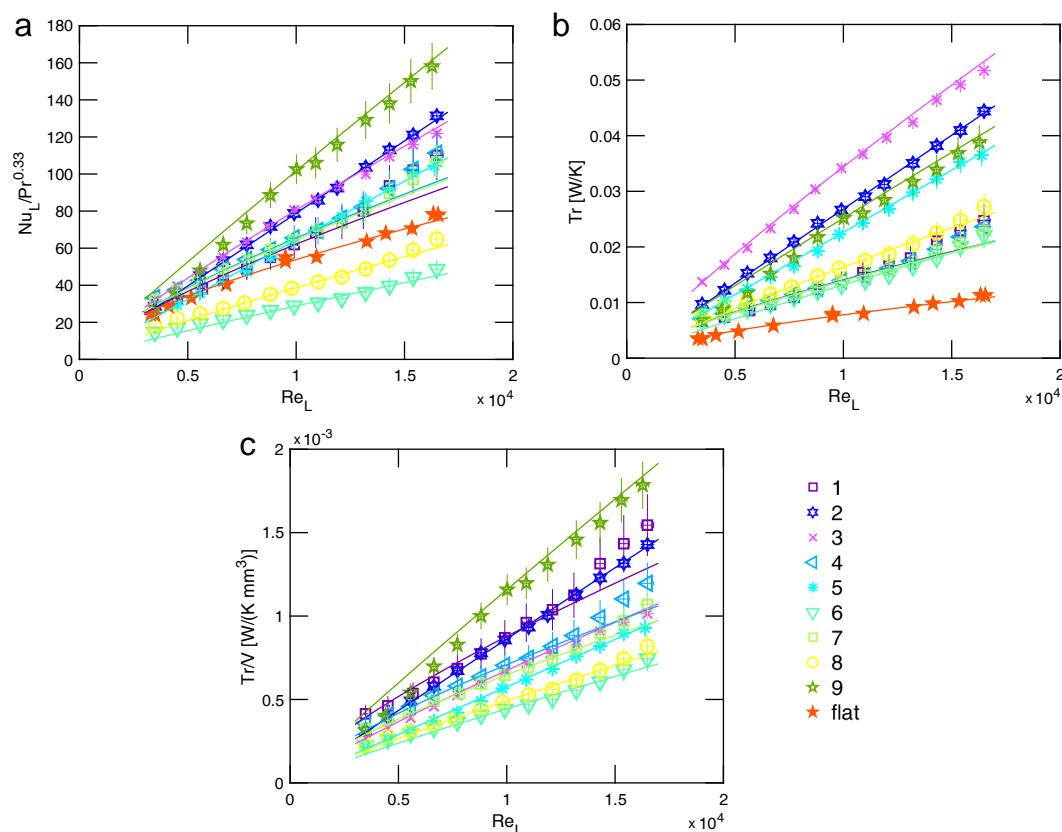
In fact, as noticeable from Figure 6a, the ratio  $Nu_L/Pr^{0.33}$  and thus the Nusselt number of heat sinks with ESR patterns is predominantly lower with respect to the one of flat surface, especially at high  $Re_L$ . On the one side, comparing the  $Nu_L/Pr^{0.33}$  results at a representative low value of  $Re_L \approx 3480$ , the best performing elliptic scale-roughened heat sink is sample 2 (+29% with respect to the  $Nu_L/Pr^{0.33}$  of flat surface at similar testing conditions), while the worst one is sample 9 (−26%). On the other side, considering a representative high value of  $Re_L \approx 16,500$ , the best performing elliptic scale-roughened heat sink is sample 7 (−1% with respect to the  $Nu_L/Pr^{0.33}$  of flat surface at similar testing conditions), while the worst one is sample 9 again (−44%). Therefore, some ESR micro-patterns seem to have a positive effect on the convective heat transfer process at lower  $Re_L$ , whereas they all show progressively lower values of  $Nu_L$  than the flat surface ones with higher  $Re_L$ .

It is also interesting to notice that sample 8 provides the best thermal performance per unit volume of employed material, as visible in Figure 6c. For the sake of completeness, sample 4 has been also tested with air flowing in the downward direction; however, Figure 6a,b confirms that better heat transfer performance can be obtained with the forward direction, as previously noticed in References [41,49].

### 3.2. Cones Patterns

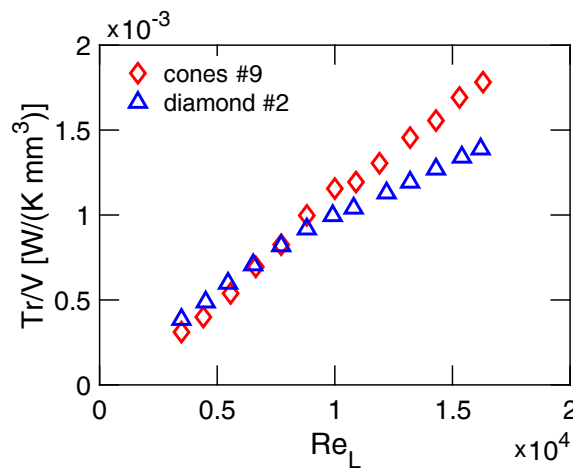
Considering the samples with cones pattern, a significant heat transfer augmentation with respect to flat heat sinks is observed for all the Reynolds number analyzed, with up to 357% enhancement in terms of  $Tr$  (see Figure 7b, sample 3 at  $Re_L = 16,500$ ). In this case, such improved heat transfer is due to

both  $A/A_n > 1$  and higher  $h$ . In fact, most heat sinks with cones pattern (except samples 6 and 8) show increased values of  $Nu_L$  with respect to the flat surface for the whole range of considered Reynolds numbers. In detail, comparing the  $Nu_L/Pr^{0.33}$  results at a representative low value of  $Re_L \approx 3480$ , the best performing cones pattern is sample 4 (+39% with respect to the  $Nu_L/Pr^{0.33}$  of flat surface at similar testing conditions), while the worst one is sample 6 (−39%). Instead, considering a representative high value of  $Re_L \approx 16,500$ , the best performing cones patterned heat sink is sample 9 (+102% with respect to the  $Nu_L/Pr^{0.33}$  of flat surface at similar testing conditions), while the worst one is sample 6 again (−38%). Also with the cones pattern, broad variations of  $Tr/V$  can be observed between the different geometric configurations (Figure 7c), being the sample 9 with the best compromise between heat transfer and volume augmentation.



**Figure 7.** Experimental performance of heat sinks with cones surface patterns at different Reynolds number: (a) Ratio between Nusselt and Prandtl numbers,  $Nu_L/Pr^{0.33}$ ; (b) thermal transmittance,  $Tr$ ; and (c) ratio between thermal transmittance and sample volume,  $Tr/V$ . In the legend, the number of each sample is associated with a symbol and color and “flat” stands for the reference heat sink with smooth surface. Symbols represent experimental data, and lines are model predictions (Equations (9)–(14)).

These results seem to be comparable with those found for heat sinks with other micro-patterns on their surface. Considering, for instance, the heat sinks with diamond shaped micro-protruded patterns tested in Reference [46], a comparison can be made at  $Re_L = 16,500$  between the best performing samples of each pattern:  $Tr$  equal to  $0.052 \text{ W K}^{-1}$  (cones) vs.  $0.085 \text{ W K}^{-1}$  (diamonds);  $Nu_L/Pr^{0.33}$  equal to 158 (cones) vs. 188 (diamonds); and  $Tr/V$  equal to  $1.78 \times 10^{-3} \text{ W K}^{-1} \text{ mm}^{-3}$  (cones) vs.  $1.35 \text{ W K}^{-1} \text{ mm}^{-3}$  (diamonds). These results highlight that, at least for  $Re_L = 16,500$ , diamond patterns lead to higher heat transfer enhancement with respect to cones ones whereas cones micro-protrusions show a higher value of  $Tr/V$  with respect to diamond ones (see Figure 8 for a complete overview on the whole range of tested  $Re_L$ ).



**Figure 8.** Comparison between the best experimental values of  $Tr/V$  for cones (sample 9) and diamonds (sample 2 [46]) micro-protruded heat sinks.

#### 4. Discussion

The experimental characterization of the laser-etched surfaces highlights that both ESR and cones patterns enhance the thermal transmittance of flush-mounted heat sinks. However, while the heat transfer augmentation from ESR patterns is only due to the larger surface, cones patterns also improve the convection process per se, therefore performing better than ESR samples and similarly to diamonds ones [46]. In this section, the improved heat transfer performance of cones patterns are modeled by semi-empirical correlations and the underlying thermal fluid dynamics mechanisms are discussed.

##### 4.1. Semi-Empirical Model of Thermal Transmittance

Following the methodology adopted in Reference [46], a model able to predict the thermal transmittance ( $Tr = hA$ ) of a generic heat sink with cones patterns has been developed. Considering the reference Reynolds number  $Re_{L,R} = 10,000$ ,  $Tr$  can be modeled as the product of two functions, namely

$$Tr = gTr_R. \tag{9}$$

In Equation (9),  $Tr_R$  is the thermal transmittance value at  $Re_{L,R}$ , which is expected to depend on the parameters employed in the design of experiments  $\{\lambda_p, \frac{A}{A_n}, \frac{V}{AY_0}\}$ . On the other hand,  $g$  accounts for values of  $Re$  different from the reference one, and it is modeled as a function of  $\frac{Re_L}{Re_{L,R}}$  and  $\frac{H}{Y_0}$  [46].

First,  $Tr_R$  can be expressed as  $Tr_R = Tr_R^0 + \Delta Tr_R$ , with  $Tr_R^0$  as the thermal transmittance of the heat sink with flat surface at the reference Reynolds number and  $\Delta Tr_R$  as the enhancement provided by the laser etching process. This model of  $Tr_R$  can be also rewritten as

$$Tr_R = Tr_R^0 + V \frac{\Delta Tr_R}{V}, \tag{10}$$

where  $\frac{\Delta Tr_R}{V}$  is correlated with the dimensionless quantities of the design of experiments as

$$\frac{\Delta Tr_R}{V} = c_1 \widehat{\lambda}_p + c_2 \widehat{\frac{A}{A_n}} + c_3 \widehat{\frac{V}{AY_0}} + c_4 \widehat{\lambda}_p^2 + c_5 \widehat{\frac{A}{A_n}}^2 + c_6 \widehat{\frac{V}{AY_0}}^2 + c_7 \widehat{\lambda}_p \widehat{\frac{A}{A_n}} + c_8 \widehat{\lambda}_p \widehat{\frac{V}{AY_0}} + c_9 \widehat{\frac{A}{A_n}} \widehat{\frac{V}{AY_0}}. \tag{11}$$

In Equation (11), the design parameters are normalized with respect to their average value, that is

$$\left\{ \begin{array}{l} \widehat{\lambda}_p = \frac{\lambda_p}{(\lambda_p)_{Avr}}, \quad (\lambda_p)_{Avr} = \frac{1}{9} \sum_{i=1}^9 (\lambda_p)_i \\ \widehat{\frac{A}{A_n}} = \frac{\frac{A}{A_n}}{(\frac{A}{A_n})_{Avr}}, \quad (\frac{A}{A_n})_{Avr} = \frac{1}{9} \sum_{i=1}^9 (\frac{A}{A_n})_i \\ \widehat{\frac{V}{AY_0}} = \frac{\frac{V}{AY_0}}{(\frac{V}{AY_0})_{Avr}}, \quad (\frac{V}{AY_0})_{Avr} = \frac{1}{9} \sum_{i=1}^9 (\frac{V}{AY_0})_i \end{array} \right. \quad (12)$$

where  $i$  stands for the  $i$ th sample. The vector  $\{C\} = \{c_1, c_2, c_3, c_4, c_5, c_6, c_7, c_8, c_9\}$  collects the coefficients of the semi-empirical model in Equation (11). The value of such coefficients can be optimized to best fit the experimental results in Figure 7, leading to  $c_1 = -2.822 \times 10^{-3}$ ,  $c_2 = 2.060 \times 10^{-3}$ ,  $c_3 = 2.379 \times 10^{-3}$ ,  $c_4 = 1.751 \times 10^{-3}$ ,  $c_5 = -0.915 \times 10^{-3}$ ,  $c_6 = -0.036 \times 10^{-3}$ ,  $c_7 = 0.100 \times 10^{-3}$ ,  $c_8 = -1.609 \times 10^{-3} \times 10^{-3}$ , and  $c_9 = -0.480 \times 10^{-3}$ , all expressed in terms of  $W/(K \text{ mm}^3)$ .

Second, the function  $g$  is modeled as

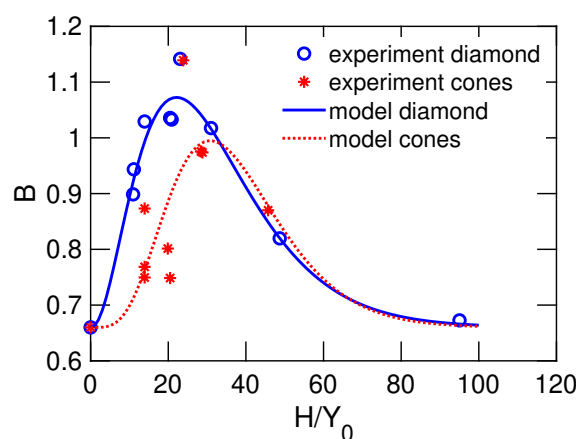
$$g = \left( \frac{Re_L}{Re_{L,R}} \right)^B. \quad (13)$$

Similarly to the previous investigations on diamond shaped micro-protruded patterns for heat sinks [46], Figure 9 shows that the exponent  $B$  in Equation (13) can be correlated with the height of the protrusions ( $H$ ) and the average viscous length ( $Y_0$ ) as

$$B = d_1 \left( \frac{H}{Y_0} \right)^{d_2} \exp \left( -d_3 \frac{H}{Y_0} \right) + d_4, \quad (14)$$

with  $d_1 = 2.887 \times 10^{-6}$ ,  $d_2 = 4.804$ ,  $d_3 = 0.156$ , and  $d_4 = 0.660$  as best fitted coefficients.

The good agreement between the experimental (symbols) and model (lines) results reported in Figure 7 proves that the semi-empirical model in Equations (9)–(14) provide a good approximation of  $Tr$  (and related  $h$  and  $Nu_L$  thermal properties) for the tested cones patterned heat sinks.



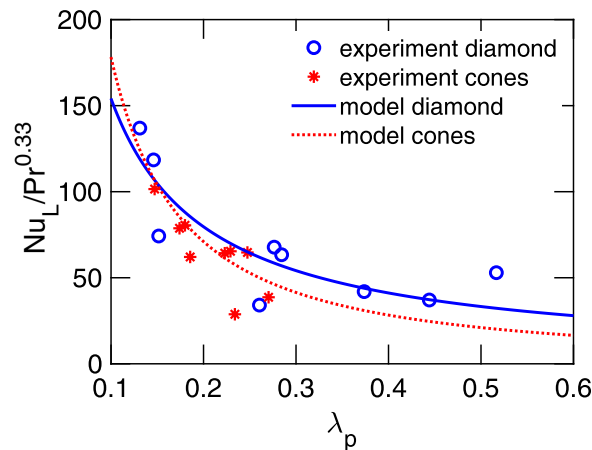
**Figure 9.** Comparison between experimental and modeled (Equation (14)) values of  $B$  for the tested cones and diamonds [46] micro-protruded heat sinks.

#### 4.2. Thermal Fluid Dynamics Features of Cones Patterned Heat Sinks

Finally, the heat transfer performance observed for the cones patterned heat sinks are interpreted in light of their geometric features.



Experiments show that  $\lambda_p$  is the geometric parameter of the cones pattern that most affects the convective heat transfer coefficient of the heat sink. Figure 10 shows that samples with low  $\lambda_p$  are characterized by higher values of  $Nu_L/Pr^{0.33}$ , since sparse patterns can effectively interfere with the boundary layer while not causing air flow stagnation between the micro-protrusions. This appears to be a common feature for cones and diamonds patterns [46]. Instead, higher values of  $\lambda_p$ , i.e., increasing pattern densities, cause air flow stagnation between the micro-protrusions and, thus, detrimental effects on convective heat transfer, and this eventually leads to  $Nu_L$  lower than the one of the reference flat heat sink (see samples 6 and 8 in Figure 7a).



**Figure 10.** Influence of  $\lambda_p$  on  $Nu_L/Pr^{0.33}$  for the cones and diamonds [46] micro-protruded heat sinks tested experimentally, considering an air flow with  $Re_{L,R}$ .

Furthermore, results show that the height of protrusions ( $H$ ) plays a key role in determining  $Tr$ . As represented in Figure 7b, samples 2 and 3—which have the longest  $H$  among the considered cones patterned samples—show the highest values of thermal transmittance. This is due to both the enhanced heat transfer surface and to the fact that taller cones can better penetrate the boundary layer, therefore augmenting convection. On the other side, the highest values of  $Tr/V$  are given by samples 1 and 9 (see Figure 7c), which have lower values of  $H$ : as a matter of fact, the ratio  $A/V$  of cones decreases with longer protrusions.  $H$  is also important to regulate how the fluid flow ( $Re_L$ ) affects  $Tr$ . In fact, Figure 9 highlights that, similarly to diamonds patterns [46], an optimal value of  $H/Y_0$  for the cones height can be found to maximize the enhancement of  $Tr$  with  $Re_L$  (see Equations (9) and (13)), according to a specific fluid flow regime ( $Re_L/Re_{L,R}$ ). The optimal height of cones should be long enough to overcome the viscous sub-layer height of the air flow (that is,  $\geq 5y_0$  [45]) but not too much to fall beyond the viscous wall region (that is,  $\leq 50y_0$  [45]).

## 5. Conclusions

In this work, elliptic scale-roughened and cones patterned heat sinks manufactured by laser etching have been investigated to enhance convective heat transfer in applications requiring efficient heat dissipation, e.g., electronics. The effects of the geometric and thermal fluid dynamics parameters of the heat sinks on their thermal performance have been explored by experiments in a flush-mounted configuration, carried out according to the Taguchi method. A semi-empirical model able to correlate the thermal transmittance of the laser-etched heat sinks with the geometric features of micro-pattern and the fluid flow regime has been implemented and validated against the experiments. Results show that, at the highest Reynolds number tested in the experiments ( $Re_L \approx 16,500$ ), the elliptic scale-roughened patterns present up to a 81% enhancement in thermal transmittance with respect to the corresponding flat surface, mainly because of the larger heat transfer surface. Notably, at similar testing conditions, cones patterns show up to 357% augmentation of thermal transmittance with respect to the

heat sink without micro-protrusions due to both higher heat transfer surface and improved Nusselt number (up to 102% increase). Experimental evidence also shows that the considered microstructured surface patterns are particularly effective in enhancing convective heat transfer at higher Reynolds numbers. By comparing these results with other laser-etched micro-protruded patterns available in the literature (e.g., diamond shaped ones [46]), cones patterns show relatively high values of thermal transmittance with respect to the volume of heat sink, at least for the upper range of Reynolds numbers tested in this study. Interestingly, the convective heat transfer coefficient enhancement of the laser-etched heat sinks with cones pattern is close to the one of flat surfaces manufactured by direct metal laser sintering with controllable artificial roughness [38]. In perspective, these results encourage and guide a broader adoption of designed micro-patterned surfaces obtained by innovative manufacturing techniques for enhancing convective heat transfer in compact heat exchangers.

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