

# Supplementary Material

N-doped sponge-like biochar: A promising CO<sub>2</sub> sorbent for CO<sub>2</sub>/CH<sub>4</sub> and  
CO<sub>2</sub>/N<sub>2</sub> gas separation

*Mirtha A. O. Lourenço<sup>1,2\*</sup>, Tânia Frade<sup>3</sup>, Marta Bordonhos<sup>2,3</sup>, Micaela Castellino<sup>4</sup>,  
Moisés L. Pinto<sup>3</sup>, Sergio Bocchini<sup>1,4</sup>*

<sup>1</sup> Istituto Italiano di Tecnologia - IIT, Centre for Sustainable Future Technologies (CSFT), Via Livorno 60, 10144-Torino, Italy

<sup>2</sup> CICECO - Instituto de Materiais de Aveiro, Departamento de Química, Universidade de Aveiro, Campus Universitário de Santiago, 3810-193, Aveiro, Portugal

<sup>3</sup> CERENA, Departamento de Engenharia Química, Instituto Superior Técnico, Universidade de Lisboa, 1049-001, Lisboa, Portugal

<sup>4</sup> Department of Applied Science and Technology (DISAT), Politecnico di Torino, Corso Duca degli Abruzzi 24, 10129-Torino, Italy

\*Corresponding author: [mirtha@ua.pt](mailto:mirtha@ua.pt)

## Materials characterization

The thermogravimetric analysis coupled with Fourier transform infrared spectroscopy (TGA-IR) was carried out on about 3 mg of each sample using a TG 209 F1 Libra® (NETZSCH GmbH), at 5 °C/min heating rate, from 25 °C to 400, 600 or 800 °C under N<sub>2</sub> flow (40 cm<sup>3</sup>/min), depending on the pyrolysis process to mimic. A step at 200 °C for 120 min is performed for the preparation of all samples. Experimental error was estimated to be typically less than 0.05 mg (approximately ± 2.5%). Gas transmittance spectra of the evolved gases were collected on a Bruker Tensor II equipped with IR gas cell (TGA-IR) heated at 200 °C to avoid condensation of degraded products. The instruments were coupled by Netzsch FT-IR Coupling Systems transfer line heated at 230 °C. In order to have a stable infrared (IR) background, the line was cleaned using vacuum during 3 cycles of vacuum/refill with N<sub>2</sub>. IR spectra of the evolved gases were sampled at 3 °C (ca. 10 s) intervals. The FTIR analysis was collected in the absorbance mode in the range 650 – 4400 cm<sup>-1</sup>. The different gases were compared with reference spectra from data bases: ammonia (NH<sub>3</sub>) [1], water (H<sub>2</sub>O) [2], carbon monoxide (CO) [3], carbon dioxide (CO<sub>2</sub>) [4], and acetic acid [5].

Elemental analyses CHN was performed with a Fisons Instruments EA-1108 CHNS-O Element Analyzer. The complete oxidation of the sample was achieved at 1000 °C. The resulting combustion gases were carried with helium (99.99%) to the chromatographic column where they were separated and quantitatively detected.

X-ray photoelectron spectroscopy (XPS) was performed with a PHI 5000 Versaprobe spectrometer (Physical Electronics, Chanhassen, US), equipped with monochromatic Al K-alpha X-ray source (1486.6 eV). A charge compensation system, based on an electron gun and Ar<sup>+</sup> ion gun, was used to neutralize surface charging. Survey and high resolution (HR) spectra are acquired using pass energy (PE) values of 187.85 and 23.50 eV, respectively. The

calibration of the binding energy (BE) scale was achieved by fixing the C–C sp<sup>2</sup> component of the C1s region of the photoelectron spectrum to 284.5 eV. Casa XPS Version 2.3.18 dedicated software was used to analyze the spectra. The Shirley background function [6] was subtracted from HR spectra to remove the background signal.

TGA was performed on a Thermogravimetric Analyzer (TGA) NETZSCH TG209 F1Libra instrument. Approximately 3 mg of sample in alumina pans are heated from 30 to 1000 °C under N<sub>2</sub> flux (20 mL/min), nitrogen flow is used as protection gas (20 mL/min).

77 K (–196 °C) Nitrogen adsorption/desorption isotherms were acquired using an Autosorb iQ equipment (Quantachrome Instruments, USA). The samples are degassed at 120 °C for 8 h.

The biochar morphology was observed by using Field Emission Scanning Electron Microscopy (FESEM) with a Zeiss Supra 40 microscope (Zeiss, Oberkochen, Germany).

## **Gas adsorption experiments**

### *Volumetric apparatus*

The adsorption isotherms of carbon dioxide (CO<sub>2</sub>; Air Liquide ALPHAGAZ, 99.998 %), methane (CH<sub>4</sub>; Air Liquide ALPHAGAZ, 99.995 %), and nitrogen (N<sub>2</sub>; Air Liquide ALPHAGAZ, 99.999 %) were measured on the chitosan-based materials, at 0 °C (only for CO<sub>2</sub>), 25 and 35 °C and pressures up to 1000 kPa, using the volumetric method. The samples were degassed at 120 °C for 30 min, at heating rate of 5 °C/min, under vacuum of 10<sup>–6</sup> hPa, after a pre-activation of 12 h, at the same conditions. The gas adsorption was measured on a lab-made stainless steel volumetric apparatus, equipped with a pressure transducer. A stirred thermostatic bath was used to control the temperature of the sample and the adsorption system.

Each experimental pure component adsorption isotherm was fitted using the Virial model and the non-ideality of the gas phase was considered using the second and third virial coefficients. Mean selectivity values were estimated using a method proposed by Myers [7] and the implementation was described in previous works [8,9]. The heats of adsorption for CO<sub>2</sub> were calculated via the Clausius–Clapeyron approach with the virial coefficients estimated from the isotherms at 25 and 35 °C [10].

### *Dynamic Vapor Sorption*

Pure CO<sub>2</sub> adsorption isotherm was performed using a Surface Measurement System, Dynamic Vapor Sorption (DVS) Instrument. The best performing materials was selected and previously activated under vacuum of 10<sup>-4</sup> hPa at 120 °C for 30 min before starting each measurement. The CO<sub>2</sub> gas was used as provided by Rivoira (Italy), with a purity of 99.99%. The isotherm temperature was kept at 30 °C with increasing pressure ( $P/P_0 = 5\%$  each step) up to 89 kPa in semi-static conditions (max flowrate = 50 mL·min<sup>-1</sup>); each step was kept up to equilibrium (criterion  $dm/dt = 0.001 \text{ \%}\cdot\text{min}^{-1}$ ). The desorption measurement was performed by reducing the pressure ( $P/P_0 = 5\%$  each step) applying the criterion  $dm/dt = 0.001 \text{ \%}\cdot\text{min}^{-1}$  to reach the equilibrium.

Pure CO<sub>2</sub> adsorption isobar was also performed using the same instrument. The pressure was kept at 89 kPa in semi-static conditions (maximum flowrate = 50 mL·min<sup>-1</sup>) with an increasing temperature of 10 °C for each step until 80 °C; each isotherm was kept up to equilibrium (criterion  $dm/dt = 0.01 \text{ \%}\cdot\text{min}^{-1}$ ). The reversing procedure was made by decreasing the temperature in 10 °C for each step until 30 °C, and an equilibrium criterion  $dm/dt$  of 0.01 %·min<sup>-1</sup>.

The reusability of the most promising sample was tested by 10 consecutive CO<sub>2</sub> adsorption-desorption cycles. Each cycle combines a CO<sub>2</sub> adsorption measurement at 20 kPa and 30 °C

(with a flowrate =  $50 \text{ mL} \cdot \text{min}^{-1}$  and an equilibrium criterion =  $0.02 \% \cdot \text{min}^{-1}$ ) and a desorption measurement at  $80 \text{ }^\circ\text{C}$  under vacuum of  $10^{-4} \text{ hPa}$  (criterion  $\text{dm}/\text{dt} = 0.02 \% \cdot \text{min}^{-1}$ ).

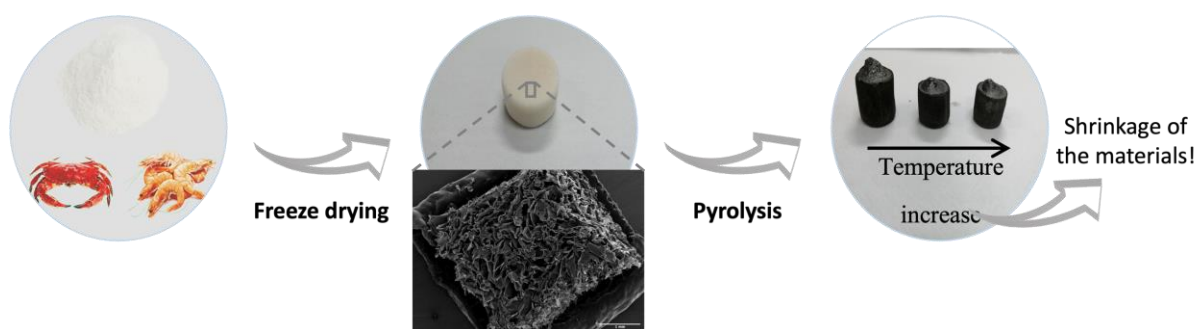
The water vapor adsorption isotherm was performed at  $30 \text{ }^\circ\text{C}$  using the same equipment. The water vapor is taken from the vapor in equilibrium in a flask filled with ultrapure water (Milli-Q). The pressure was increased up to  $\sim 4 \text{ kPa}$ , by introducing a water vapor pressure of  $\sim 1.06 \text{ kPa}$  each step (with a max target vapor flow =  $15 \text{ sccm}$  and an equilibrium criterion  $\text{dm}/\text{dt} = 0.001 \% \cdot \text{min}^{-1}$ ). The desorption measurement was made by decreasing the pressure ( $1.06 \text{ kPa}$  each step) and applying an equilibrium criterion  $\text{dm}/\text{dt} = 0.001 \% \cdot \text{min}^{-1}$ .

The CTO\_P600 sample was also tested in the  $\text{H}_2\text{O}/\text{CO}_2$  adsorption isotherms at  $30 \text{ }^\circ\text{C}$  under continuous gas flow. In this case, the water vapor generated was combined with a separate stream of pure  $\text{CO}_2$  before being introduced into the balance. The partial pressure of the gases was controlled by altering the flow rates of these two streams and hence the ratio of the total pressure. Three cycles were conducted to examine various  $\text{H}_2\text{O}/\text{CO}_2$  ratios (maximum total pressure =  $\sim 3.8 \text{ kPa}$ , 1<sup>st</sup> cycle =  $\sim 1.06 \text{ kPa}$  and  $\sim 2.76 \text{ kPa}$ , 2<sup>nd</sup> cycle =  $\sim 2.12 \text{ kPa}$  and  $\sim 1.70 \text{ kPa}$ , and 3<sup>rd</sup> cycle =  $\sim 3.18 \text{ kPa}$  and  $\sim 0.64 \text{ kPa}$  of  $\text{H}_2\text{O}$  and  $\text{CO}_2$ , respectively), and the equilibrium criterion used was  $\text{dm}/\text{dt} = 0.001\% \cdot \text{min}^{-1}$ . The desorption procedure was performed under the reverse conditions of the adsorption measurement.

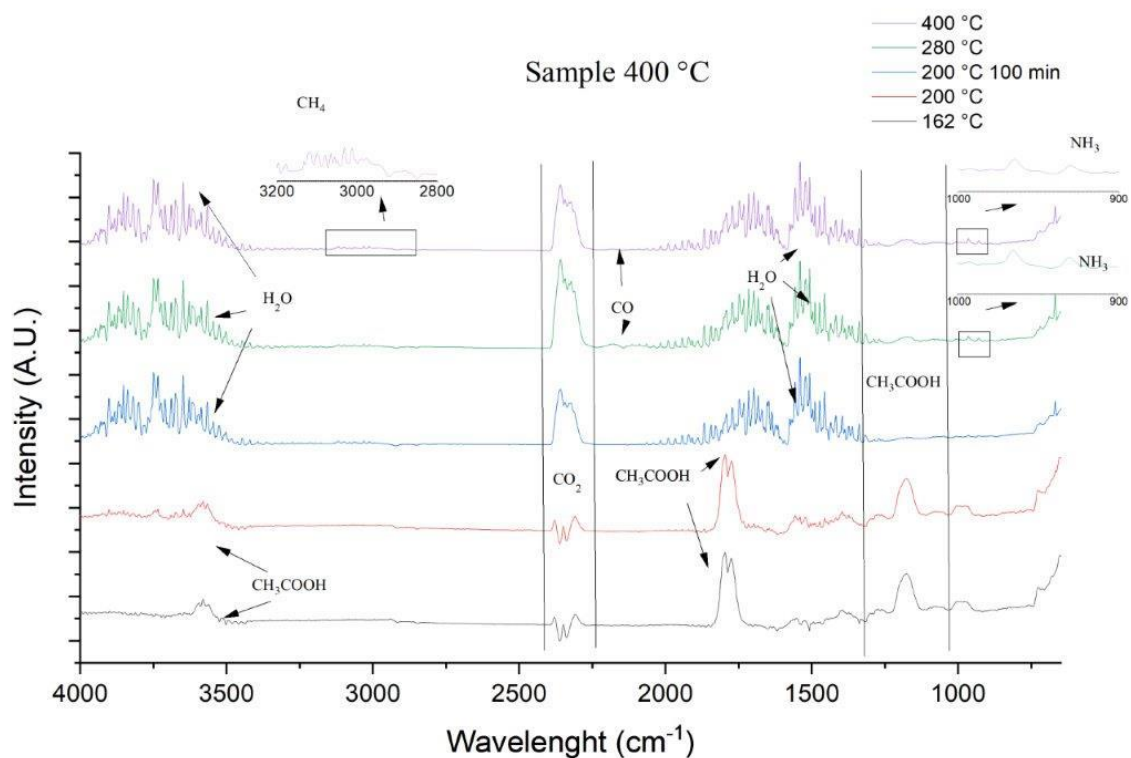
### *TGA*

The  $\text{CO}_2$  adsorption performance over  $\text{N}_2$  gas was evaluated using a TGA (NETZSCH TG 209F1 Libra) apparatus using the same procedure previously described in reference [11]. The measurements were performed at  $35 \text{ }^\circ\text{C}$  and environmental pressure ( $\sim 100 \text{ kPa}$ ). The samples ( $\sim 10 \text{ mg}$ ) were degassed through 3 consecutive cycles of vacuum and pure  $\text{N}_2$ , followed by heating the samples until  $120 \text{ }^\circ\text{C}$  (heating rate =  $40 \text{ }^\circ\text{C} \cdot \text{min}^{-1}$ ) under vacuum for 30 min. After cooling to  $35 \text{ }^\circ\text{C}$  (cooling rate =  $2 \text{ }^\circ\text{C} \cdot \text{min}^{-1}$ ), the biochar samples were exposed to pure  $\text{N}_2$

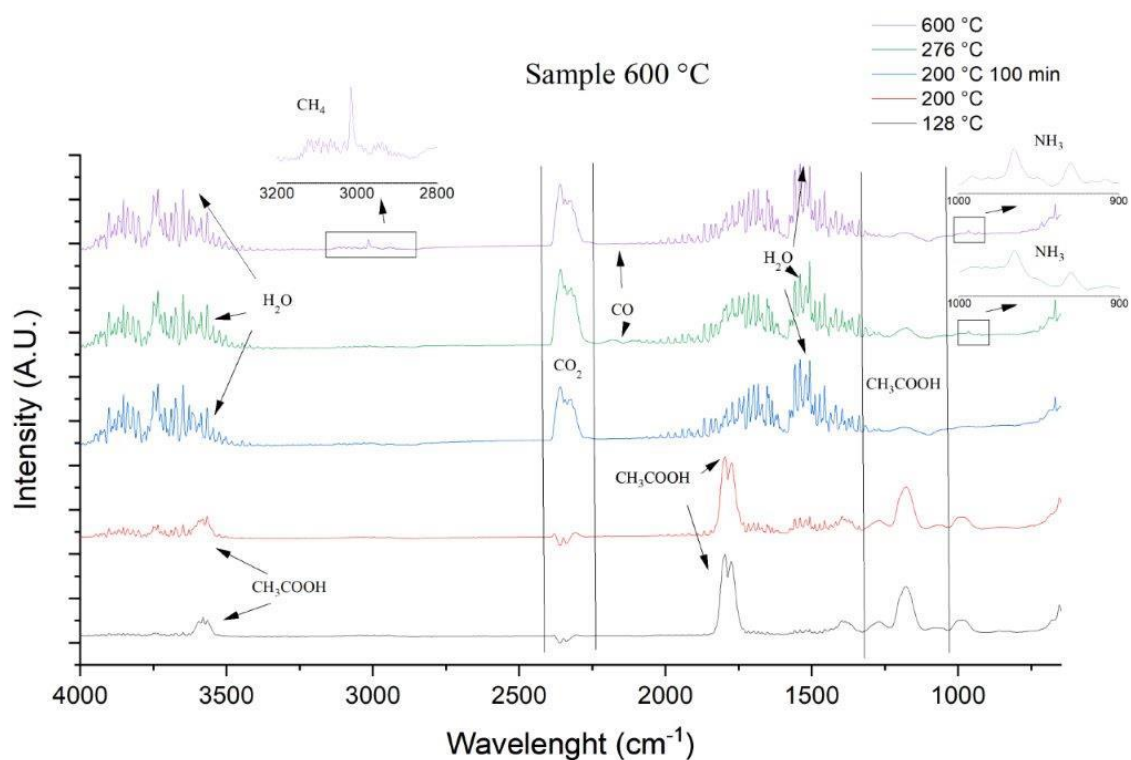
(flowrate =  $40 \text{ mL} \cdot \text{min}^{-1}$ ) at atmospheric pressure for 30 min, until weight stabilization. Then, the  $\text{N}_2$  gas was swept with a mixture of  $\text{CO}_2/\text{N}_2$  (20 vol.% of  $\text{CO}_2$ , total flowrate =  $40 \text{ mL} \cdot \text{min}^{-1}$ ) for 120 min. Both  $\text{CO}_2$  and  $\text{N}_2$  flow rates were kept constant. The weight difference between the initial and final moment of the  $\text{CO}_2$  adsorption indicates the  $\text{CO}_2$  amount adsorbed by the materials. Finally, the desorption of the  $\text{CO}_2$  was studied under pure  $\text{N}_2$  (flowrate =  $40 \text{ mL} \cdot \text{min}^{-1}$ ) at atmospheric pressure with increasing temperature until  $100 \text{ }^\circ\text{C}$  (heating rate =  $40 \text{ }^\circ\text{C} \cdot \text{min}^{-1}$ ).



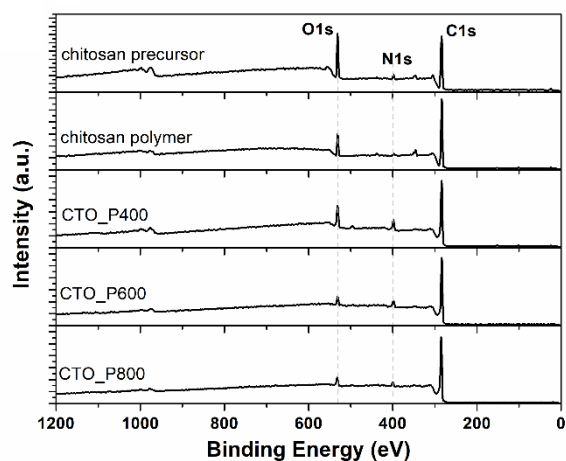
**Scheme S1.** Schematic representation of the synthesized biochar materials and SEM image of the chitosan aerogel material.



**Figure S1.** IR spectra of the developed gases at 162, 200, 200 (at 100 min.), 280 and 400 °C under  $\text{N}_2$  flow, acquired during the pyrolysis process to obtain CTO\_P400 sample.



**Figure S2.** IR spectra of the developed gases at 128, 200, 200 (at 100 min.), 276 and 600 °C under  $\text{N}_2$  flow, acquired during the pyrolysis process to obtain CTO\_P600 sample.

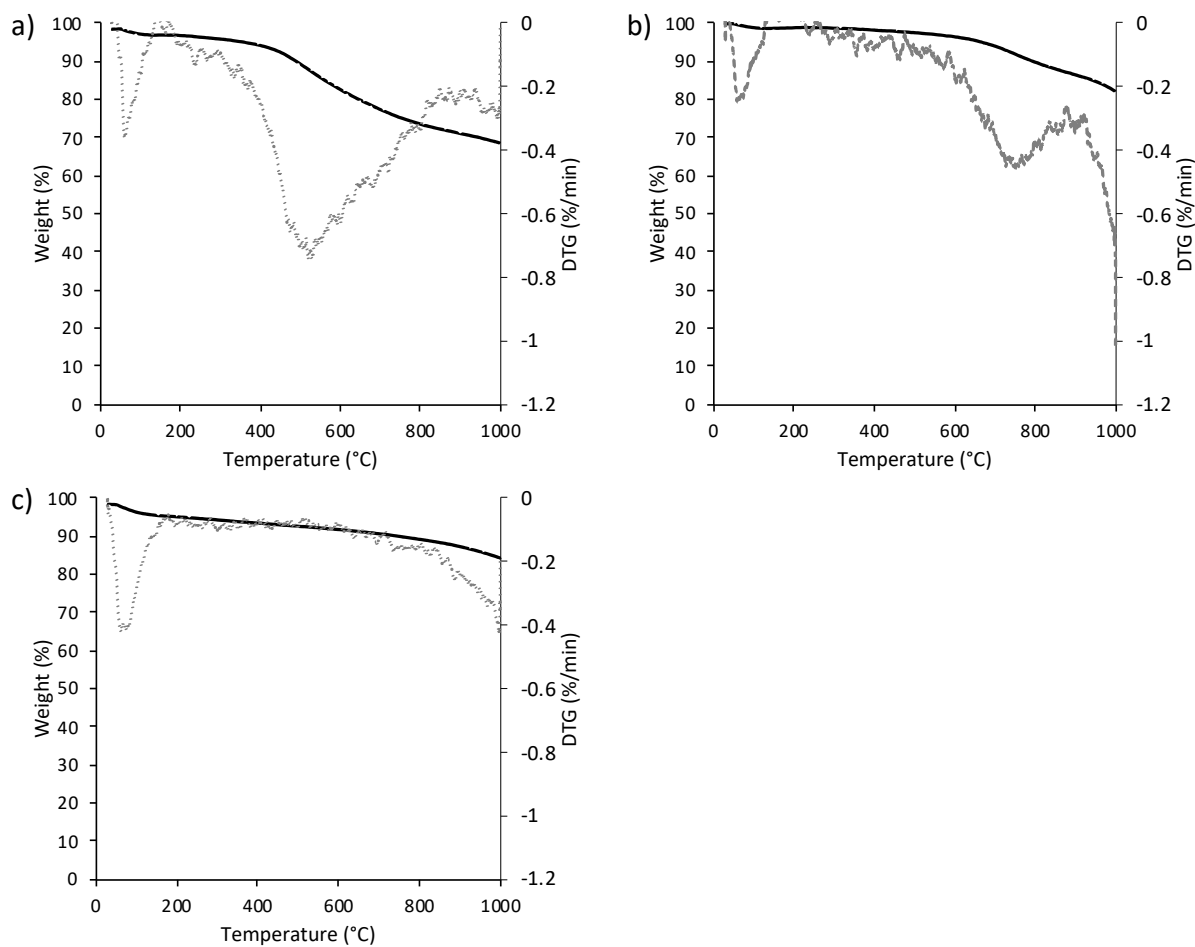


**Figure S3.** XPS survey spectra for chitosan precursor and polymer samples and pyrolyzed samples (CTO\_P400, CTO\_P600, CTO\_P800) from top to bottom.

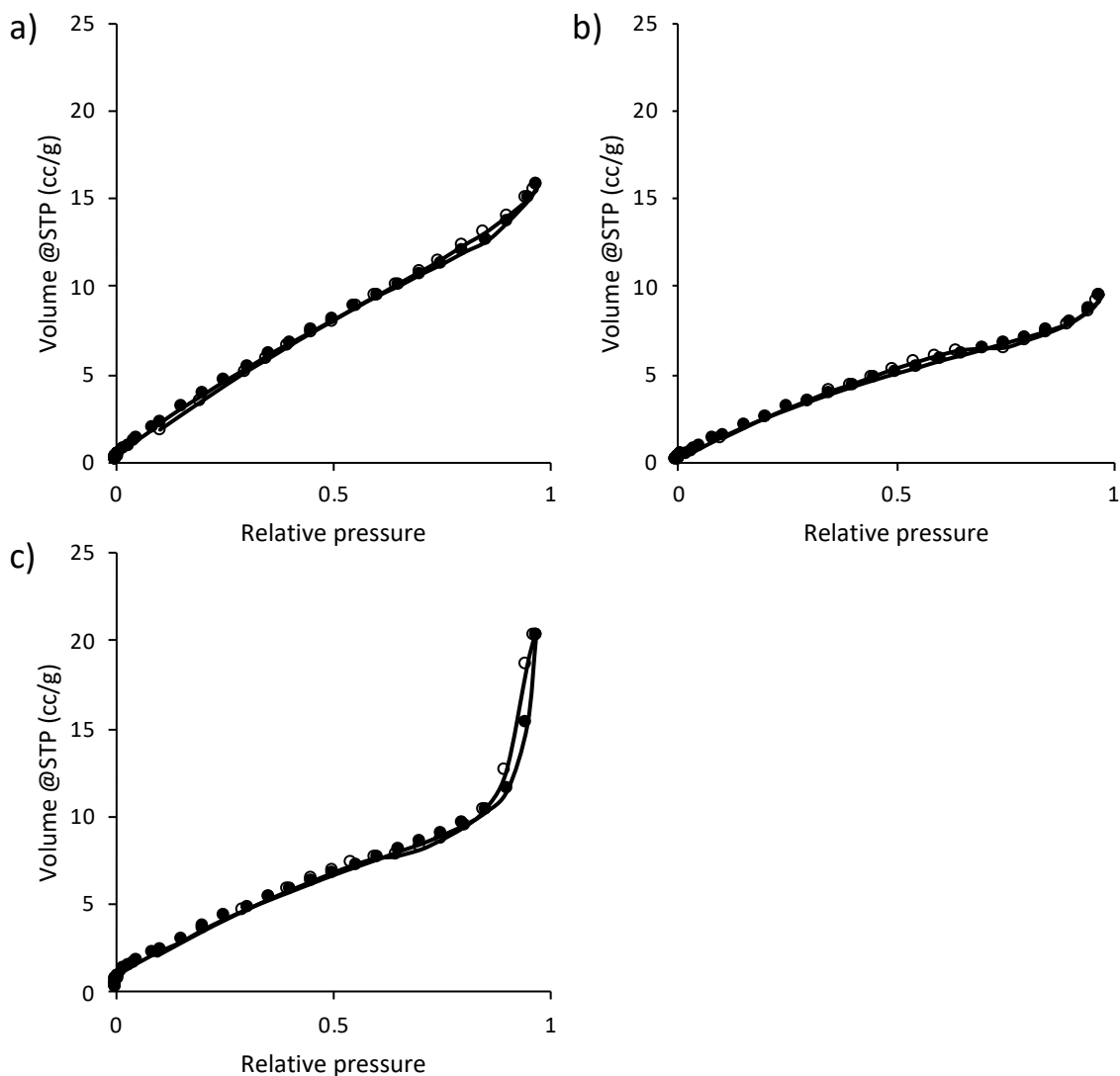
**Table S1.** Elemental analyses of the pyrolyzed chitosan.

Sample	% N	% C	% H
CTO_P400	9.87	64.44	3.59
CTO_P600	8.88	71.55	<2
CTO_P800	6.40	70.20	<2





**Figure S4.** TGA of a) CTO\_P400, b) CTO\_P600, and c) CTO\_P800 under N<sub>2</sub> atmosphere.

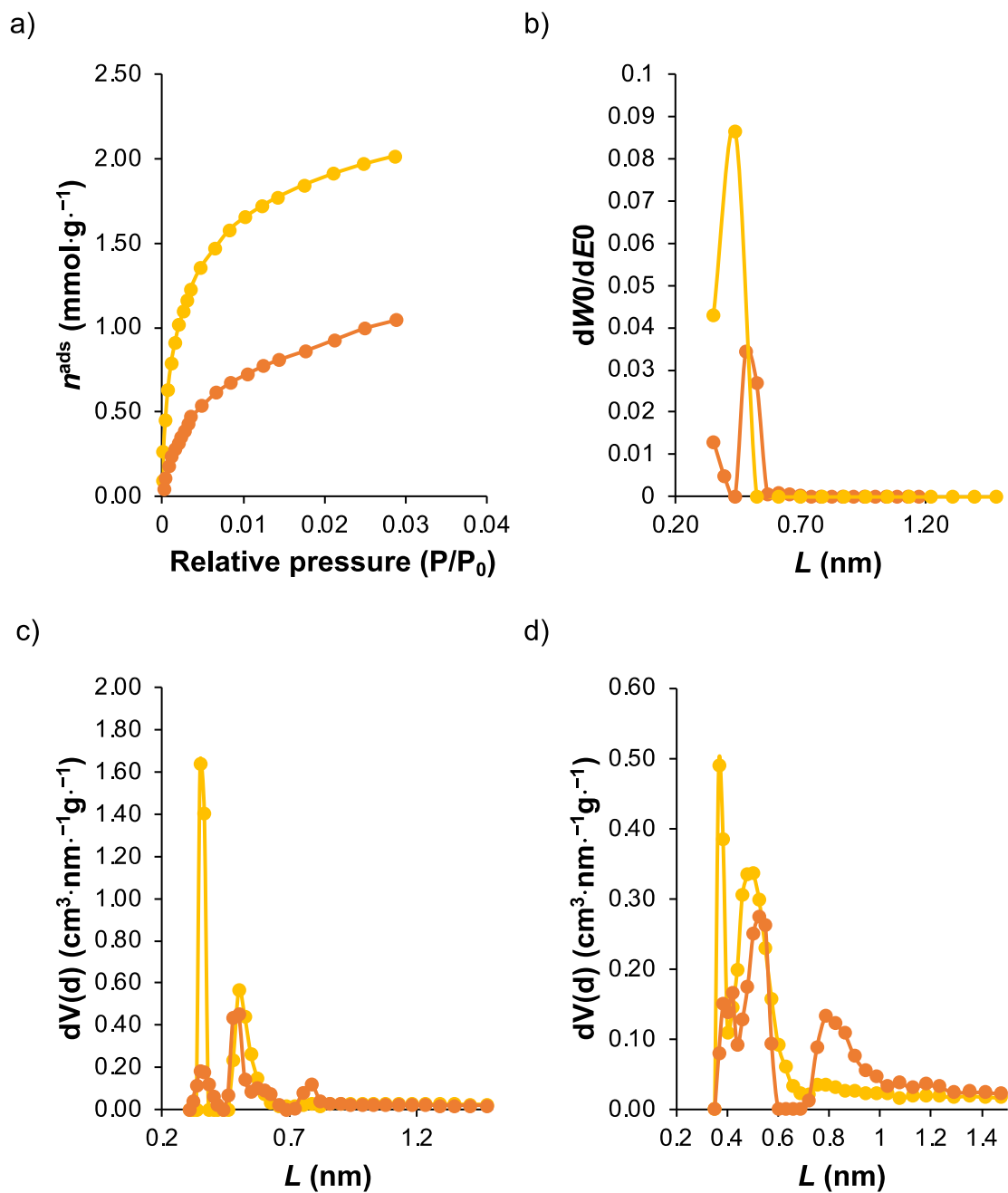


**Figure S5.** 77 K (−196 °C) N<sub>2</sub> adsorption-desorption isotherms of a) CTO\_P400, b) CTO\_P600, and c) CTO\_P800 (filled symbols correspond to adsorption process, empty symbols correspond to desorption process).

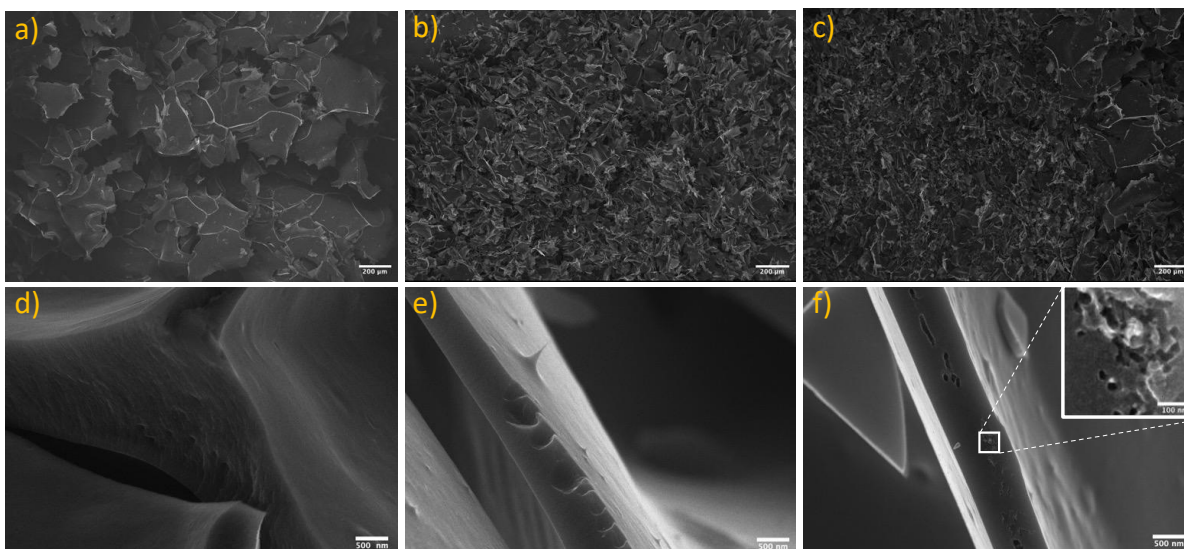
**Table S2.** Textural parameter determined by 77 K (−196 °C) N<sub>2</sub> adsorption-desorption isotherms and 0 °C CO<sub>2</sub> adsorption isotherms of CTO\_Px.

Sample	$S_{BET}$ (m <sup>2</sup> ·g <sup>−1</sup> ) <sup>a</sup>	$R^b$	$V_p$ (cm <sup>3</sup> ·g <sup>−1</sup> ) <sup>c</sup>	$S_{BET}^{micro}$ (m <sup>2</sup> ·g <sup>−1</sup> ) <sup>d</sup>	$R^b$	$DR, V_p^{micro}$ (cm <sup>3</sup> ·g <sup>−1</sup> ) <sup>e</sup>	$NLDFT, V_p^{micro}$ (cm <sup>3</sup> ·g <sup>−1</sup> ) <sup>e</sup>	$MC, V_p^{micro}$ (cm <sup>3</sup> ·g <sup>−1</sup> ) <sup>e</sup>
CTO_P400	18.54	0.9877	0.023	133	0.9993	0.080±0.0014	0.068±0.0004	0.077±0.0006
CTO_P600	11.55	0.9874	0.013	260	0.9992	0.134±0.0027	0.111±0.0061	0.102±0.0013
CTO_P800	14.58	0.9987	0.030	-	-	-	-	-

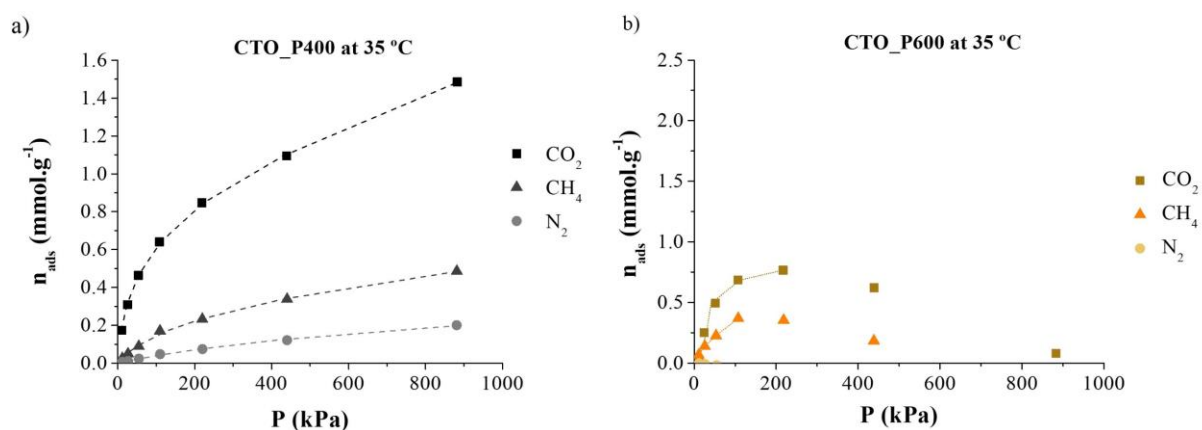
<sup>a</sup> Brunauer-Emmett-Teller (BET) Specific surface area determined by using 77 K (−196 °C) N<sub>2</sub> adsorption isotherms; <sup>b</sup> Correlation coefficient; <sup>c</sup>  $V_p$  denotes pore volume determined from 77 K (−196 °C) N<sub>2</sub> adsorption isotherms; <sup>d</sup> BET Specific surface area determined by using 0 °C CO<sub>2</sub> adsorption isotherms and applying the nonlocal density functional theory (NLDFT); <sup>e</sup> pore volume determined from 0 °C CO<sub>2</sub> adsorption isotherm and applying Dubinin-Radushkevich (DR), NLDFT and Monte Carlo (MC) models.



**Figure S6.** a) CO<sub>2</sub> adsorption isotherm at 0 °C and pore size distribution curves determined using the b) DR, c) NLDFT, and d) MC models on CTO\_P400 (orange) and CTO\_P600 samples (yellow).



**Figure S7.** FESEM images of a) CTO\_P400, b) CTO\_P600, and c) CTO\_P800 acquired at a magnification of 500x, and d) CTO\_P400, e) CTO\_P600, and f) CTO\_P800 obtained at a magnification of 50000x.

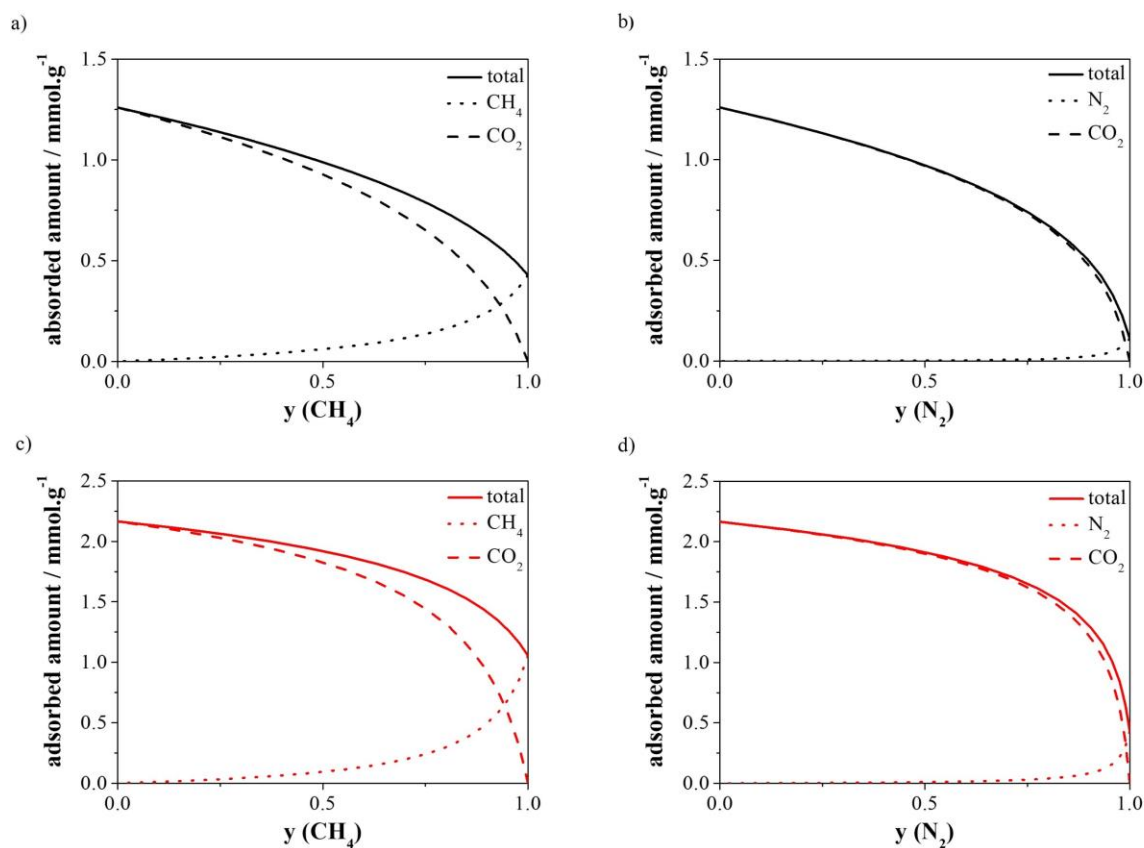


**Figure S8.** Adsorption isotherms of pure CO<sub>2</sub> (square symbols), CH<sub>4</sub> (triangle symbols), and N<sub>2</sub> (circle symbols) gases at 35 °C in the pyrolyzed samples at: **a)** 400 °C (CTO\_P400) and **b)** 600 °C (CTO\_P600). The dashed lines represent the fits of the Virial isotherm model to the experimental data.

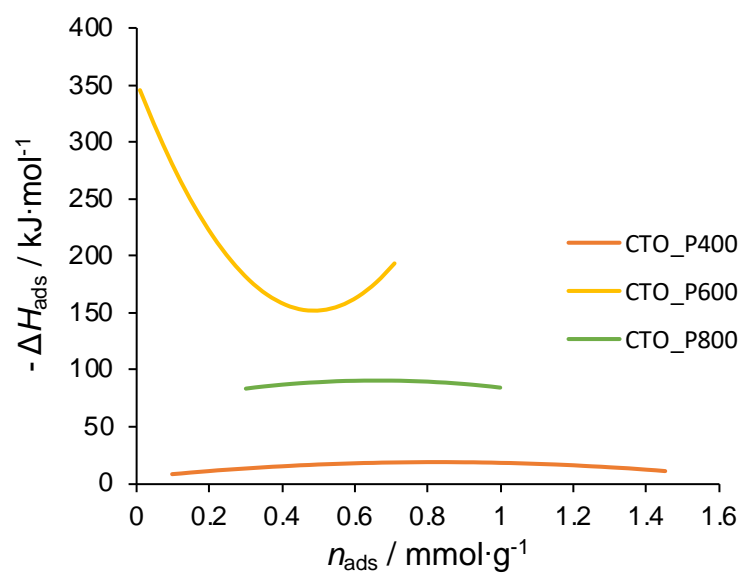
**Table S3.** Virial coefficients ( $C_1$  and  $C_2$ ) and Henry constants ( $K$ ) for the adsorption of methane, carbon dioxide and nitrogen at 35 °C on the studied materials.

Gas	Sample	$K$ (mol.kg <sup>-1</sup> .kPa <sup>-1</sup> )	$C_1$ (kg.mol <sup>-1</sup> )	$C_2$ (kg.mol <sup>-1</sup> ) <sup>2</sup>	$C_3$ (kg.mol <sup>-1</sup> ) <sup>3</sup> *
CH <sub>4</sub>	CTO_P400	$2.61 \times 10^{-3}$	4.32	-2.28	---
	CTO_P600	$7.56 \times 10^{-3}$	3.08	-2.52	---
	CTO_P800	---	---	---	---
CO <sub>2</sub>	CTO_P400	$3.25 \times 10^{-2}$	3.25	-0.87	---
	CTO_P600	$1.43 \times 10^{-3}$	-9.93	11.42	---
	CTO_P800	$1.24 \times 10^{-1}$	3.38	-0.79	---
N <sub>2</sub>	CTO_P400	$4.49 \times 10^{-4}$	3.48	---	---
	CTO_P600	---	---	---	---
	CTO_P800	---	---	---	---

\* The third virial coefficient ( $C_3$ ) was neglected for all fitted adsorption isotherms.



**Figure S9.** Adsorbed amount of (a) and (c) CH<sub>4</sub>/CO<sub>2</sub> and (b) and (d) N<sub>2</sub>/CO<sub>2</sub> mixtures as a function of the CH<sub>4</sub> and N<sub>2</sub> molar fraction in the gas phase, respectively, at 500 kPa and 25 °C, for CTO\_P400 (black lines) and CTO\_P600 (red lines) materials.



**Figure S10.** Heats of adsorption for CO<sub>2</sub> calculated via the Clausius–Clapeyron approach with the virial coefficients estimated from the isotherms at 25 and 35 °C.

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