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Electrochemical characterization of -Fe<sub>2</sub>O<sub>3</sub> and a reduced graphene oxide composite as a sustainable anode material for Na-ion batteries / Staffolani, A., Sbrascini, L., Bottoni, L., Minnetti, L., Darjazi, H., Trapananti, A., Paparoni, F., Rezvani, S.J., Minicucci, M., Harfouche, M., Nobili, F.. - In: ENERGY ADVANCES. - ISSN 2753-1457. - 3:7(2024), pp. 1726-1736. [10.1039/d4ya00335g]

*Availability:*

This version is available at: 11583/2996493 since: 2025-01-10T10:33:58Z

*Publisher:*

Royal Society of Chemistry

*Published*

DOI:10.1039/d4ya00335g

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Cite this: *Energy Adv.*, 2024,  
3, 1726

# Electrochemical characterization of $\gamma$ -Fe<sub>2</sub>O<sub>3</sub> and a reduced graphene oxide composite as a sustainable anode material for Na-ion batteries†

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In this paper we report the synthesis and characterization of a  $\gamma$ -Fe<sub>2</sub>O<sub>3</sub>/reduced graphene oxide composite anode for Na-ion batteries. The nanocomposite anode is synthesized by a facile and green method. Structural and morphological characterization highlights a small  $\gamma$ -Fe<sub>2</sub>O<sub>3</sub> particle size and their successful embedding in the carbonaceous matrix. Electrochemical characterization reveals a high specific capacity of  $\approx 300$  mA h g<sup>-1</sup> at 1000 mA g<sup>-1</sup>, while at 5 A g<sup>-1</sup> a capacity of 113 mA h g<sup>-1</sup> is retained. Cyclic voltammetry at different scan rates, impedance spectroscopy, and *ex situ* Raman measurements evidence a redox pseudocapacitive behavior and full reversibility of the conversion reaction. The green synthesis coupled to the high specific capacity and rate capability make the proposed  $\gamma$ -Fe<sub>2</sub>O<sub>3</sub>/rGO nanocomposite a very promising candidate anode material for sustainable Na-ion batteries.

Received 27th May 2024,  
Accepted 10th June 2024

DOI: 10.1039/d4ya00335g

rsc.li/energy-advances

## 1. Introduction

Energy storage systems (ESSs) are playing a major role in the green transition from fossil fuels to renewable energy sources.<sup>1,2</sup> Indeed, due to the fitful nature of these energy sources, efficient and sustainable ESSs are needed as a key enabling technology to ensure a constant supply of electrical energy. Li-ion batteries are playing a major role thanks to their high energy density, high energy efficiency, and cycle life

compared to other available electrochemical energy storage technologies.<sup>1–3</sup> However, further improvements are needed to reach complete electrification of transport and replacement of fossil fuels for energy production. In this regard, researchers focused their efforts on studying novel electrode materials able to satisfy the requirements in terms of performance and sustainability. Coupled to this, further concerns are related to availability of raw materials such as Li<sup>4,5</sup> and Co.<sup>6</sup> Furthermore, the recycling rate of lithium from spent batteries is still rather low ( $\approx 1\%$ ).<sup>7</sup> For these reasons, alternative alkali-ion rechargeable batteries based on Na and K are being developed. Sodium is the 4th most abundant element in the earth crust, with reservoirs spread everywhere across the world. Furthermore, sodium and lithium share similar chemical properties, thus the know-how acquired on LIBs can be easily transferred to the sodium counterpart.<sup>8</sup> However, some differences, such as the different standard reduction potential ( $-3.04$  V vs. SHE for Li<sup>+/</sup>Li couple and  $-2.71$  V vs. SHE for Na<sup>+/</sup>Na) and ionic radius (0.7 Å vs. 1 Å for Li<sup>+</sup> and Na<sup>+</sup>, respectively), could lead to lower energy density and rate performances of NIBs compared to LIBs. These differences in the charge carriers also reflect on other electrochemical properties and processes, such as diffusion, electrode/electrolyte interphase formation and stability, and (in)activity towards certain materials. Indeed, while in LIBs graphite and silicon are considered the state-of-the-art anode materials, in NIBs their ability to accept Na<sup>+</sup> ions is rather low,

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† Electronic supplementary information (ESI) available. See DOI: <https://doi.org/10.1039/d4ya00335g>

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and thus poor performances are commonly observed.<sup>9,10</sup> Commonly studied anode materials are hard carbons and transition metal oxides (TMOs). TMOs can react with Na<sup>+</sup> by three different reaction paths, *i.e.*: (i) insertion reaction, (ii) mixed conversion-alloying reaction, and (iii) conversion reaction. In the first case, materials such as Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub> and Na<sub>2</sub>Ti<sub>3</sub>O<sub>7</sub> can reversibly insert the alkali-ion ensuring a good capacity retention with small volume change.<sup>11,12</sup> However, the specific capacity of these materials is low due to the low amount of cation which can be inserted in the crystal host structure. The second case includes materials such as SnO<sub>2</sub>, GeO<sub>2</sub>, and Sb<sub>2</sub>O<sub>3</sub> which, after the conversion step, can form binary alloys with Na.<sup>13,14</sup> As a result, very high specific capacities are observed; however, the structural stresses due to the volume expansion during Na-metal alloying can lead to extremely poor capacity retention. The latter case includes oxides of metals which are not able to form a binary alloy with sodium and can only exploit the multiple electron transfer given by the conversion reaction. However, poor capacity retention due to the structural rearrangement and high voltage hysteresis are commonly observed.

Iron oxides have attracted much interest in both LIBs and NIBs systems thanks to their high theoretical specific capacity (ranging from 744 mA h g<sup>-1</sup> for FeO<sup>15</sup> up to 1007 mA h g<sup>-1</sup> for Fe<sub>2</sub>O<sub>3</sub><sup>16</sup>) as well as their abundance, cost, and nontoxicity.<sup>17</sup> However, the issues connected with the continuous structural rearrangements, and the subsequent poor capacity retention, must be overcome to enable their practical application in commercial NIBs. Common strategies involve the preparation of nanostructured materials and/or nanocomposite materials. Nanostructured materials can offer the advantages of better rate performances and capacity retention given by higher specific surface area, shorter diffusion path, smaller volume changes. Several morphologies, such as 0-D nanoparticles,<sup>18</sup> nanotubes,<sup>19</sup> and chain-like particles,<sup>20</sup> have shown remarkable improvements.

The preparation of nanocomposite materials with an active or inactive matrix can effectively mitigate the stresses due to the structural rearrangements upon cycling. Carbon-based materials are among the mostly used buffering matrixes, thanks to their remarkable electronic conductivity and low cost.<sup>21–23</sup> Graphene has already been studied as an active material thanks to its high electronic conductivity, reliable mechanical properties, and high aspect ratio.<sup>24,25</sup> However, its use in ESSs is still questioned by drawbacks such as high cost and tendency to restack to form amorphous carbon, and eventually graphite.<sup>26</sup> Nevertheless, its use in nanocomposite formulations can buffer the volume changes and improve the mechanical stability of the electrode. Furthermore, its utilization in composites easily results in enhancement of overall electrode conductivity. For these reasons, graphene has already been used as containment matrix for conversion and conversion-alloying materials for both LIBs and NIBs systems.<sup>27</sup> Nevertheless, some drawbacks regarding the synthesis of iron oxide/graphene-based composite materials need to be overcome. In most cases, hydrothermal and high temperature calcinations are used, which can hinder the potential scale-up of the synthesis process.<sup>28</sup>

Herein, we report a facile two-step synthesis of 5-nm  $\gamma$ -Fe<sub>2</sub>O<sub>3</sub> particles by coprecipitation and their embedding into a matrix of reduced graphene oxide (rGO), without the use of high temperature treatments. The resulting composite material is a  $\gamma$ -Fe<sub>2</sub>O<sub>3</sub>:rGO ratio of 80:20 (m/m) which can ensure good electrochemical performances at a reasonable cost. Electrodes are prepared with PAA as a green and high-elastic-modulus binder.<sup>29</sup> Thanks to the synergistic effect of the combination of  $\gamma$ -Fe<sub>2</sub>O<sub>3</sub> with rGO, the composite material exhibits high specific capacity and excellent rate capability. An extensive electrochemical and structural characterization is reported. Finally, *ex situ* Raman measurements shed light on the reaction mechanism of  $\gamma$ -Fe<sub>2</sub>O<sub>3</sub> in NIBs configuration.

## 2. Experimental

### 2.1 Materials

PAA ( $M_w$  450 000 g mol<sup>-1</sup>), FeCl<sub>2</sub>·4H<sub>2</sub>O (>99%), FeCl<sub>3</sub>·6H<sub>2</sub>O (<99%), propylene carbonate (PC, anhydrous 99.7%), dimethyl carbonate (DMC, anhydrous <99%), NaClO<sub>4</sub> (>98%), hydrazine hydrate, and concentrated NH<sub>4</sub>OH were purchased from Sigma-Aldrich. Ethylene carbonate (EC, battery grade) was purchased from Solvionic (Toulouse, France). Graphene oxide (C:O ratio of 5:4.3) was purchased from Nanoinnova technologies SL. All reactants were used as received.

### 2.2 $\gamma$ -Fe<sub>2</sub>O<sub>3</sub>/rGO synthesis

The nanocomposite anode material was prepared according to a similar method previously described in a previous report.<sup>30</sup> Briefly, the synthesis involves firstly the coprecipitation of iron oxide nanoparticles, and then their embedding into reduced graphene oxide. Stoichiometric amounts of FeCl<sub>2</sub>·4H<sub>2</sub>O and FeCl<sub>3</sub>·6H<sub>2</sub>O (molar ratio 1:2) were dissolved in 40 mL of distilled water. After the complete dissolution of the salts, 100 mL of 10% NH<sub>4</sub>OH were added under vigorous stirring giving a black precipitate. The solution was then heated at 70 °C, and further 30 mL of concentrated NH<sub>4</sub>OH were added. The reaction was kept at 70 °C for 8 h. Eventually, the obtained iron oxide, in the form of a black powder, was washed thoroughly with distilled water, acetone, and ethanol. The powder was dried in vacuum oven at 50 °C. Afterwards, 200 mg of graphene oxide were dispersed in 150 mL of distilled water for 1 h to obtain a homogeneous dispersion. 500 mg of the synthesized iron oxide powder was subsequently added to the dispersion and further sonicated for 1 h. 10 mL of hydrazine hydrate were added to the above dispersion to reduce the graphene oxide matrix (an ice bath was used to control the heat of reaction). The dispersion was kept under sonication for another 2 h, followed by vacuum filtration with Millipore (0.2  $\mu$ m GTTP) and washed with distilled water, acetone, and ethanol. Eventually, the obtained composite powder was dried under vacuum at 50 °C. Reference rGO was synthesized with the same procedure without the addition of iron oxide nanoparticles.



### 2.3 Structural, chemical, morphological characterization

The structure of the obtained materials was characterized by using a Horiba iH320 Raman spectrometer equipped with a 532 nm laser source, and a Philipps diffractometer equipped with a Cu-K $\alpha$  source ( $\lambda = 1.540 \text{ \AA}$ ). The carbon content in the composite material was assessed by using a Perkin-Elmer STA6000 TGA-DTA. Morphological characterization was performed by a ZEISS Sigma Series 300 field-emission scanning electron microscope (FE-SEM) and by a ZEISS EM 910 TEM microscope equipped with a tungsten thermionic electron gun operating at 100 kV.

The chemical and structural features of the as prepared composite powder was assessed by X-ray absorption spectroscopy (XAS) measurements, performed at beamline XAFS/XRF beamline of the SESAME synchrotron source.<sup>31</sup> The beamline was equipped with a fixed-exit double-crystal Si(111) monochromator installed between two cylindrically bent mirrors, both set to work at a grazing incidence angle of 2.8 mrad on the Si coated stripes for harmonic rejection. Fe K-edge spectra were collected in transmission mode by using ion chambers located downstream and upstream the sample. Sample powders, in amount giving an edge jump at the Fe K edge close to 1.0, were mixed with cellulose and measured in the form of 13 mm diameter pellets.

Measurements were compared with spectra of  $\alpha$ -Fe $_2$ O $_3$ ,  $\gamma$ -Fe $_2$ O $_3$  and Fe $_3$ O $_4$  commercial powders collected at SAMBA beamline (SOLEIL synchrotron), also in transmission mode. Spectra of metallic Fe foil were measured for initial energy calibration (first inflection point set at 7112 eV) and simultaneously with any sample (by using a third ion chamber) for the proper monitoring of the energy scale.

### 2.4 Electrode processing

The electrode layer was prepared by doctor blade technique. The slurry was prepared by mixing  $\gamma$ -Fe $_2$ O $_3$ /rGO active material: conductive carbon SUPERC 65 (Timcal C-Energy<sup>TM</sup>): polyacrylic acid (PAA,  $M_w = 450\,000 \text{ g mol}^{-1}$ ) in 70:20:10 m/m ratio. Firstly, the polymer binder was dissolved in ethanol. In the meantime, the active material and the carbon additive were finely grounded in an agata mortar. The mixed powders were added to the binder solution and stirred by a magnetic stirrer overnight. The obtained slurry was casted onto 10  $\mu\text{m}$  copper foil by doctor-blade, with a wet thickness of 150  $\mu\text{m}$ . The electrode layer was then dried at 70  $^\circ\text{C}$  for 2 h. Circular electrodes of  $\varnothing = 9 \text{ mm}$  were cut using an electrode puncher (EL-CELL). Eventually, the electrodes were pressed at 4.7 tons  $\text{cm}^{-2}$ , weighted, and vacuum dried at 120  $^\circ\text{C}$  overnight. The electrodes resulted in an average loading of active material  $\approx 1.5 \text{ mg cm}^{-2}$ .

### 2.5 Electrochemical characterization

For all the electrochemical measurements, the  $\gamma$ -Fe $_2$ O $_3$ /rGO electrodes have been used as working electrodes in three-electrode cells. Na metal disks have been used as counter and reference electrodes, 1 M NaClO $_4$  EC : PC 1 : 1 (v : v) as electrolyte

and Whatman GF/A glass fiber disc as separator. Swagelok-type cells have been used for cyclic voltammetry, galvanostatic cycling, and rate capability. Prior any electrochemical characterization, the cells underwent an open circuit voltage period of 12 h. Cyclic voltammeteries (CV) have been acquired in the potential range  $0.02 < E < 3 \text{ V}$  at scan rates ranging from  $100 \mu\text{V s}^{-1}$  up to  $500 \mu\text{V s}^{-1}$  with  $50 \mu\text{V s}^{-1}$  increment steps. Galvanostatic cycles have been performed with specific current ranging from 100 up to 5000  $\text{mA g}^{-1}$  within the voltage window  $0.020 < E < 3.000 \text{ V}$ . ECC-ref cells (EL-CELL GmbH, Hamburg) have been used for electrochemical impedance spectroscopy (EIS) in potentiostatic mode. EIS measurements have been acquired every 10th cycle, by applying a sinusoidal perturbation of  $\Delta E = \pm 5 \text{ mV}$  over bias potential  $E = 0.5 \text{ V}$ , in a frequency range  $7 \text{ mHz} < f < 200 \text{ kHz}$  with 10 points per decade and logarithmic spacing. All the potential values are referred to the Na $^+$ /Na redox couple ( $E^\circ = -2.71 \text{ vs. SHE}$ ).

*Ex situ* Raman measurements have been performed on samples which had been brought to selected states of charge (SOC) during the first cycle, by galvanostatic (dis)charge at 500  $\text{mA g}^{-1}$  followed by 6 h-constant voltage step to ensure electrode equilibration. Subsequently, the cells were disassembled in glovebox under Ar atmosphere, then the electrodes were washed three times with dimethyl carbonate (anhydrous DMC, Sigma-Aldrich) to remove electrolyte components which could interfere with the Raman analysis, and finally put between two microscope slides sealed with epoxy resin.

All the cell assembly/disassembly procedures were carried out by using an Ar-filled glovebox (Jacomex GP-Campus) with H $_2$ O and O $_2$  < 1 ppm.

## 3. Results and discussion

### 3.1 Structural, morphological, and thermal characterization

The Raman spectrum of  $\gamma$ -Fe $_2$ O $_3$ /rGO composite powder is shown in Fig. 1a. The observed Raman pattern is consistent with the literature findings of maghemite Fe $_2$ O $_3$ <sup>32</sup> and of carbonaceous materials.<sup>33</sup> Specifically, the peak located at  $667 \text{ cm}^{-1}$  can be ascribed to the A $_{1g}$  mode of  $\gamma$ -Fe $_2$ O $_3$ ,<sup>32</sup> while the peak located at  $271 \text{ cm}^{-1}$  can be ascribed to the T $_{1g}$  mode of  $\gamma$ -Fe $_2$ O $_3$ .<sup>32</sup> Three characteristic peaks of carbonaceous materials are observed in the Raman pattern. Specifically, the D-band and

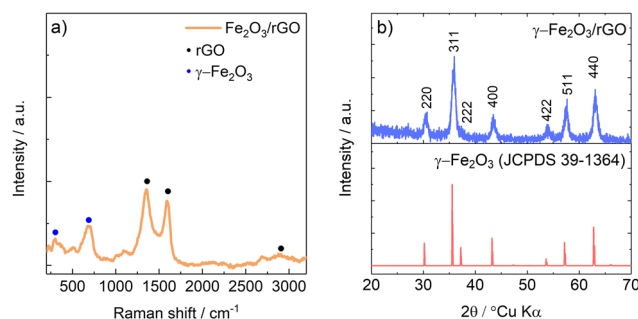


Fig. 1 (a) Raman spectra of  $\gamma$ -Fe $_2$ O $_3$ /rGO. (b) Experimental diffractograms of  $\gamma$ -Fe $_2$ O $_3$ /rGO with reference JCPDS card of  $\gamma$ -Fe $_2$ O $_3$ .



G-band located at 1302 and 1581  $\text{cm}^{-1}$ , respectively, clearly show the recovery, upon GO reduction, of the  $\text{sp}^2$  carbon pattern with defects.<sup>33</sup> The high  $I_D/I_G$  ratio ( $\approx 1.31$ ) suggests a high number of structural defects on rGO surface.

In Fig. 1b, the experimental diffractogram of  $\gamma\text{-Fe}_2\text{O}_3/\text{rGO}$  shows a diffraction pattern which can be ascribed to spinel  $\gamma\text{-Fe}_2\text{O}_3$  maghemite with space group  $P4_132$  (JCPDS 39-1364). No signals of rGO were detected by XRD probably because of the larger scattering factor of Fe respect to C and, as shown in the TGA in Fig. S2 (ESI<sup>†</sup>), by the low amount of rGO compared to iron oxide.

It should be noted that, as reported in literature,  $\text{Fe}_3\text{O}_4$  and  $\gamma\text{-Fe}_2\text{O}_3$  share an almost identical structure, with the latter being considered an Fe(II)-deficient magnetite.<sup>32</sup> This means that neither Raman spectroscopy nor X-Ray diffraction can differentiate the two different oxidation state. Thus, X-ray absorption spectroscopy in the near edge region (XANES) has been performed to assess the oxidation state of iron in the oxide powder. The results are shown in Fig. 2. The comparison of XANES spectra measured on the as prepared composite, with those of reference compounds, confirms that  $\gamma\text{-Fe}_2\text{O}_3$  is the main phase formed within the sample, ruling out the presence of  $\alpha\text{-Fe}_2\text{O}_3$  or  $\text{Fe}_3\text{O}_4$ .

In Fig. 3a the SEM micrographs of  $\gamma\text{-Fe}_2\text{O}_3/\text{rGO}$  are shown. Formation of large aggregates of  $\gamma\text{-Fe}_2\text{O}_3$  nanoparticles is evidenced, probably given by the magnetic stirring. However, at higher magnification the particle size can be visually estimated in the range 5–10 nm. The morphology of the bare  $\gamma\text{-Fe}_2\text{O}_3$  nanoparticles has been confirmed also by TEM, shown in Fig. 3e, in which aggregates of spherical particles with a 10 nm diameter were observed.

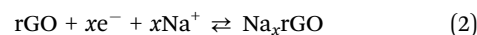
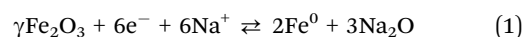
On the other hand, at high magnification (Fig. 3b) it is possible to confirm the effective embedding of the nanoparticles into the rGO matrix. Furthermore, as depicted in Fig. S1 (ESI<sup>†</sup>), the carbon flakes observed in Fig. 3a and b are

mainly composed by stacked carbon layers and embedded  $\gamma\text{-Fe}_2\text{O}_3$  particles. The distribution of iron oxide through the carbonaceous matrix has been confirmed also by both EDS elemental mapping and TEM (Fig. 3c–f). Especially on Fig. 3f, it is possible to observe both small and large clusters of  $\gamma\text{-Fe}_2\text{O}_3$  embedded in the carbon nanosheet.

The thermal gravimetric analysis, shown in Fig. S2 (ESI<sup>†</sup>), evidenced a weight loss of 19% above approximately 375  $^\circ\text{C}$  due to the oxidation of rGO to  $\text{CO}_2$ , resulting in an estimated of 79:21  $\gamma\text{-Fe}_2\text{O}_3$ :rGO mass ratio.

### 3.2 Electrochemical characterization

Fig. S3 (ESI<sup>†</sup>) shows the cyclic voltammetry of  $\gamma\text{-Fe}_2\text{O}_3/\text{rGO}$ . In the first cathodic scan two features of electrochemical processes involving the composite active material are evidenced: a broad peak at 0.75 V (A), which can be assigned to the conversion reaction of  $\gamma\text{-Fe}_2\text{O}_3$  (eqn (1)),<sup>34,35</sup> and a sharp peak (B) at low potential assigned to  $\text{Na}^+$  ions storage by rGO (eqn (2)).<sup>36</sup>



It should be noted that part of the electrochemical activity evidenced by the large shoulder (A) is related to the irreversible reduction of the electrolyte at the interface with carbon and formation of the solid electrolyte interphase (SEI), which is expected at  $E < 0.8$  V for Na-ion cells.<sup>37</sup> During the anodic scan, three features are clearly discernible: a sharp peak (B') at low potential given by the release of  $\text{Na}^+$  ions from the rGO matrix, and two broad peaks (A' and A'') at 0.8 and 1.4 V vs.  $\text{Na}^+/\text{Na}$ , respectively, which can be attributed to the oxidation of  $\text{Fe}^0$  to  $\text{Fe}^{2+}$  and  $\text{Fe}^{3+}$ .<sup>34,35</sup>

The charge/discharge capability of the  $\gamma\text{-Fe}_2\text{O}_3/\text{rGO}$  nanocomposite and capacity retention for more than 120 cycles were assessed by galvanostatic cycles in the  $0.02 < E < 3$  V potential range. Fig. 4a and b reports the specific capacity values obtained at 500 and 1000  $\text{mA g}^{-1}$  specific currents, as well as the Coulombic efficiency. At both specific currents applied, the capacity decay evidenced during the initial cycles is related to the irreversible SEI formation and the partly irreversible  $\gamma\text{-Fe}_2\text{O}_3$  conversion which take place during electrode discharge. Specifically, the largest irreversibility is evidenced in both conditions during the first cycle, where the Coulombic efficiency values are 53.75% and 42.85% for 500 and 1000  $\text{mA g}^{-1}$ , respectively. A progressively decrease of irreversibility is observed through the following cycles, up to around the 20th cycle where the reversible capacity stabilizes for both currents applied at  $\approx 300$   $\text{mA h g}^{-1}$ , with an average efficiency of 98.8% and 97.7% at 500 and 1000  $\text{mA g}^{-1}$ , respectively. The  $E$  vs.  $Q$  galvanostatic profiles (Fig. 4c and d) confirm the first-cycle irreversibility of the electrodes. No clear plateaus are evidenced by the charge/discharge profiles of the first two cycles, suggesting that completion of the several phase transitions, related to the (de)conversion processes, is kinetically hindered. To better characterize the several processes taking place, reversibly and

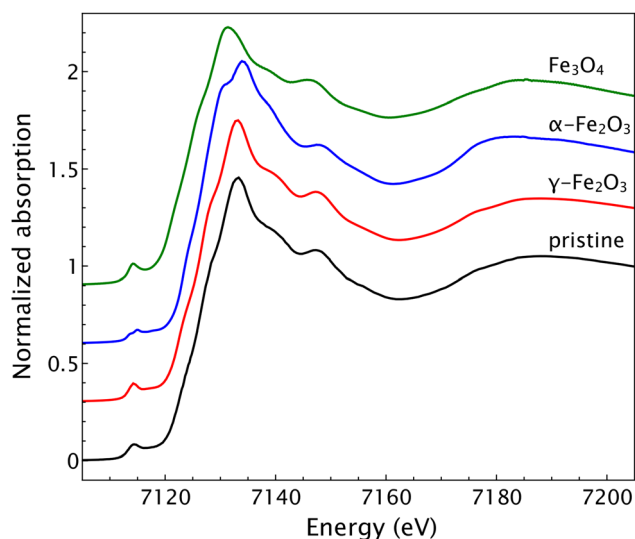


Fig. 2 XANES spectra of the pristine composite powder with spectra of reference compounds  $\gamma\text{-Fe}_2\text{O}_3$ ,  $\alpha\text{-Fe}_2\text{O}_3$  and  $\text{Fe}_3\text{O}_4$ .



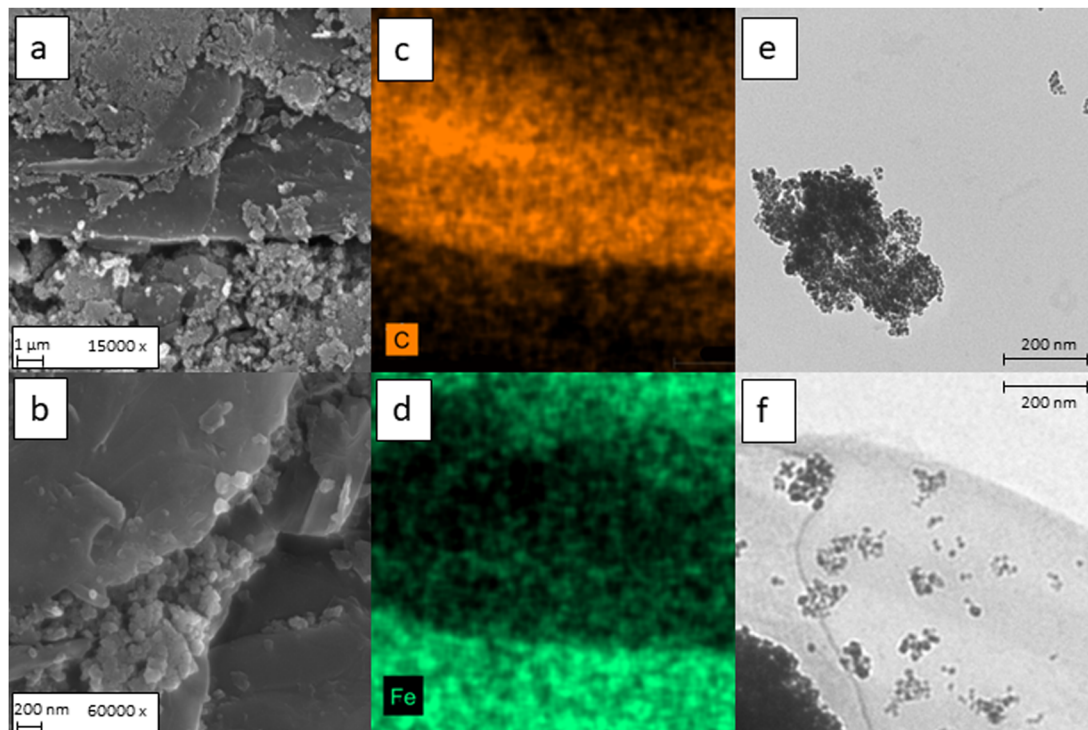


Fig. 3 SEM micrographs of  $\gamma\text{-Fe}_2\text{O}_3/\text{rGO}$  at (a) 15000x and (b) 60000x. EDS mapping at 15000x with highlighted (c) carbon and (d) iron. TEM micrographs of (e) bare  $\gamma\text{-Fe}_2\text{O}_3$  and (f)  $\gamma\text{-Fe}_2\text{O}_3/\text{rGO}$  taken at 63000x.

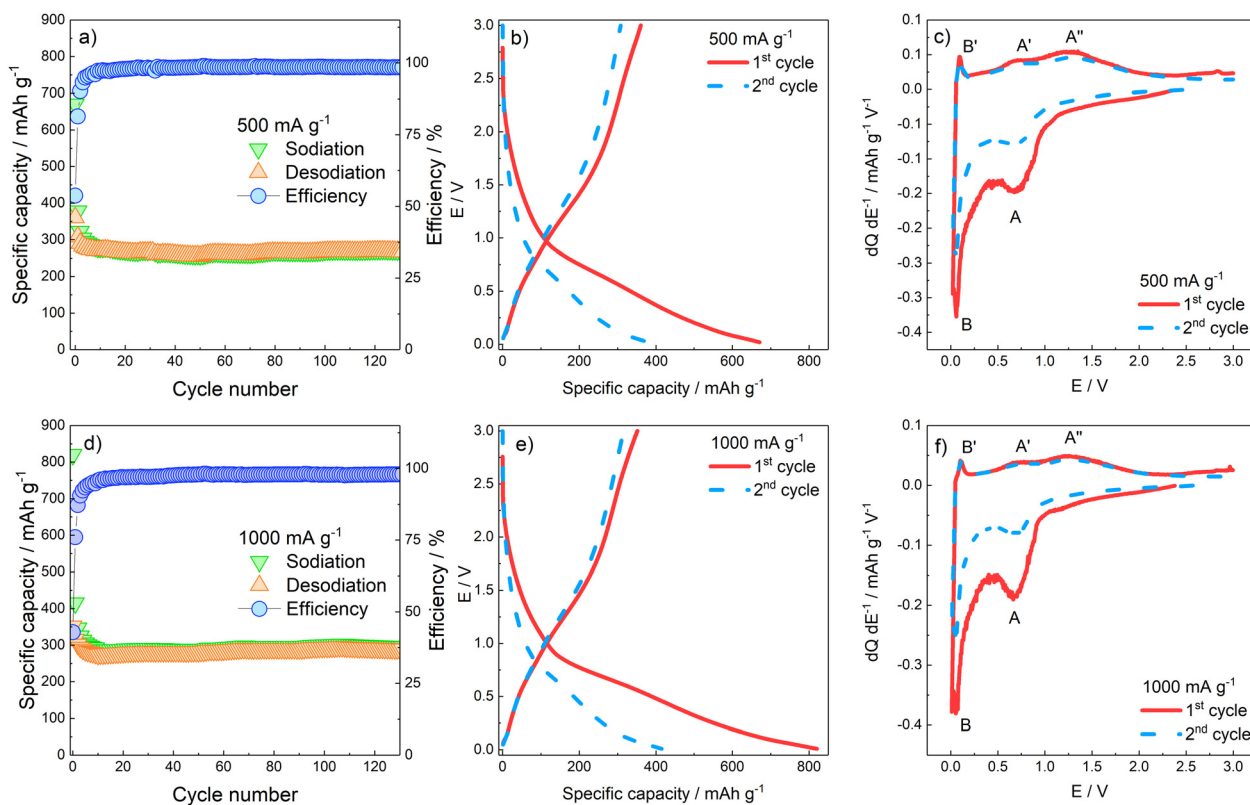


Fig. 4 (a) Galvanostatic cycles obtained at (a) 500 and (b) 1000  $\text{mA g}^{-1}$ . Galvanostatic  $E$  vs.  $Q$  profiles obtained at (c) 500  $\text{mA g}^{-1}$  and (d) 1000  $\text{mA g}^{-1}$ . Galvanostatic differential  $E$  vs.  $dQ/dE^{-1}$  profiles obtained at (e) 500  $\text{mA g}^{-1}$  and (f) 1000  $\text{mA g}^{-1}$ .



irreversibly, on rGO and  $\gamma\text{-Fe}_2\text{O}_3$  components, differential analysis has been performed by plotting the  $dQ/dE^{-1}$  vs.  $E$  graphs calculated on the data of the galvanostatic  $E$  vs.  $Q$  profiles. The  $dQ/dE^{-1}$  vs.  $E$  profiles in Fig. 4e and f confirm that in the first cycle, at both current applied, a large contribution to the specific capacity at  $E < 1$  V (peak A) is given by SEI formation and conversion reaction of  $\gamma\text{-Fe}_2\text{O}_3$ ; on the other hand, during the oxidation the electrode does not yield the same amount of charge, confirming irreversibility of SEI formation and, partially, of the conversion reaction.

The rate performance of  $\gamma\text{-Fe}_2\text{O}_3/\text{rGO}$  was assessed by applying a rate capability protocol. The electrode underwent charge/discharge at specific current values of 100, 200, 500, 1000, 2000, 5000  $\text{mA g}^{-1}$  (5 cycles at each current). Subsequently, a specific current of 100  $\text{mA g}^{-1}$  was applied to verify the capacity retention of the material. The results of the rate capability tests are shown in Fig. 5 and summarized in Table 1.

The rate capability results confirm that the composite material can withstand high current rates. As expected, the specific capacity decreases as the specific applied current increases. Nevertheless, around 50% and 40% of the capacity initially delivered at 100  $\text{mA g}^{-1}$  (A) is still delivered at the very high specific currents of 2000  $\text{mA g}^{-1}$  (E) and 5000  $\text{mA g}^{-1}$  (F), respectively. When the current is restored to the initial value (G) of 100  $\text{mA g}^{-1}$ , an average capacity of 280  $\text{mA h g}^{-1}$  over 40 cycles is retained, corresponding to the initial reversible capacity. Some cycles exhibit high spikes in the delivered capacity, as well as in the galvanostatic differential profiles, during oxidation, suggesting minor breakage/reformation of the SEI, and thus release of  $\text{Na}^+$  ions which are then plated on the counter electrode. This behaviour is consistent with the

**Table 1** Specific capacities and efficiencies of  $\gamma\text{-Fe}_2\text{O}_3/\text{rGO}$  at different current rates. The values are calculated as the average capacity over 5 cycles delivered at each current during the sodiation step

	C-rate ( $\text{mA g}^{-1}$ )	Capacity ( $\text{mA h g}^{-1}$ )	Efficiency (%)
A	100	274.3	98.88
B	200	220.0	99.08
C	500	191.4	99.07
D	1000	174.1	99.27
E	2000	138.6	99.21
F	5000	112.6	99.11
G	100	280.6	99.66

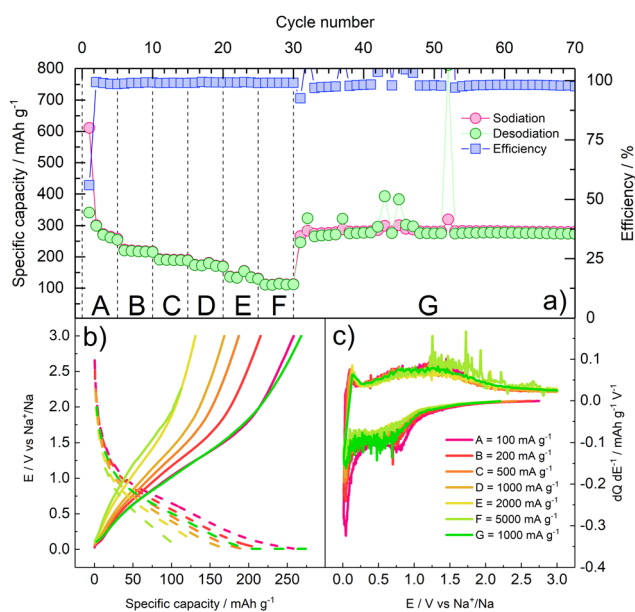
well-known instability of passivation layer on NIB anodes.<sup>38</sup> Furthermore, the capacity obtained at 0.5 and 1  $\text{A g}^{-1}$  is lower than the one observed in Fig. 4, suggesting that cycling at lower current rates in the initial cycles may have fostered the formation of a thicker SEI, affecting the electrode performance.

Finally, long-term cyclability of the electrode has been assessed by running 1000 charge/discharge cycles at 1  $\text{A g}^{-1}$  specific current in the potential range  $0.02 \text{ V} < E < 3 \text{ V}$ . As shown in Fig. S4 (ESI<sup>†</sup>), the electrode delivers an initial discharge capacity around 300  $\text{mA h g}^{-1}$ , with slow fading upon long-term cycling. In fact, 250  $\text{mA h g}^{-1}$  and 200  $\text{mA h g}^{-1}$  are retained after 500 and 1000 cycles, respectively, resulting in a capacity retention of 66% at the end of the experiment. The Coulombic efficiency is stabilized at values approaching 100% after 25 cycles.

For sake of comparison, we have performed a long-term cycling test in the same condition for electrodes containing bare  $\gamma\text{-Fe}_2\text{O}_3$  and bare rGO as active materials, obtained by the same synthetic procedure reported in Section 2.2 without the rGO embedding step. The experiments resulted in poorer cycling behaviour for the bare components than the composite (Fig. S5, ESI<sup>†</sup>), with measured specific capacities of  $\approx 120 \text{ mA h g}^{-1}$  for both  $\gamma\text{-Fe}_2\text{O}_3$  and rGO, and failure of the rGO cell at the 350th cycle.

It should be noted that the charge/discharge capacity values obtained by the  $\gamma\text{-Fe}_2\text{O}_3:\text{rGO}$  80:20 composite under investigation outperform the results reported by several authors<sup>36,39–41</sup> with rGO-enriched compositions (up to pure rGO) at comparable cycling rates. These results suggest that the  $\gamma\text{-Fe}_2\text{O}_3:\text{rGO}$  80:20 composition represents an optimal trade-off between performances and sustainability. The results are summarized in Table S1 (ESI<sup>†</sup>).

The electrode morphology was assessed before and after 100 cycles by SEM and EDS elemental mapping. The results are shown in Fig. S6 (ESI<sup>†</sup>). The pristine  $\gamma\text{-Fe}_2\text{O}_3/\text{rGO}$  electrode (Fig. S6 and S6c, ESI<sup>†</sup>) is characterized by the active material powder attached to the current collector. Several large aggregates are clearly visible in the micrograph, probably due to the magnetic stirring during the preparation of the slurry. The EDS elemental mapping revealed no unexpected elements apart from Cr, given by the metallization before the SEM measurement. However, the cycled  $\gamma\text{-Fe}_2\text{O}_3/\text{rGO}$  electrode (Fig. S6b, ESI<sup>†</sup>) presented a very different morphology, with the active material being covered by an almost uniform layer. This layer could be both the SEI layer and the  $\text{Na}_2\text{O}$  coming from the



**Fig. 5** Rate capability of  $\gamma\text{-Fe}_2\text{O}_3/\text{rGO}$ . (a) cycle number vs. specific capacity/efficiency; (b) galvanostatic  $E$  vs.  $Q$  profiles at each current value; (c) differential  $E$  vs.  $dQ/dE^{-1}$  profiles at each current value. The current values applied at each step are detailed in Table 1.



conversion reaction. However, by only SEM is not possible to discern among the two options. In Fig. S6d (ESI<sup>†</sup>), it is possible to confirm the presence of the elements Na and Cl coming from the electrolyte and, probably, from the Na<sub>2</sub>O from the conversion reaction. Thus, the mentioned layer could be both the SEI layer along with the irreversibly formed Na<sub>2</sub>O, which can explain the large irreversible capacity observed in the initial cycles in Fig. 4.

### 3.3 Interfacial and transport properties characterization

The interfacial and transport properties were characterized by means of cyclic voltammetry at different scan rates, potentiostatic electrochemical impedance spectroscopy, and *ex situ* Raman spectroscopy.

As the scan rate increases, the exchanged current proportionally increases (Fig. 6a). Indeed, the  $I$  vs.  $\nu^{1/2}$  plot (peak A has been considered for the calculation) underlines a linear relationship ( $R^2 = 0.99838$ ) which suggests a diffusion-controlled behaviour (Fig. 6b). However, if both faradaic charge transfer ( $i_{\text{Far}}$ ) and capacitive ( $i_{\text{Cap}}$ ) contributions to the overall current are taken into account, the delivered current can be approximated by the empirical relationships reported in eqn (3), where the terms  $a$  and  $b$  are dimensionless adjustable parameters:<sup>42</sup>

$$i(\nu) = i_{\text{Far}} + i_{\text{Cap}} = a\nu^b \quad (3)$$

when  $b = 0.5$  the process is purely faradaic and controlled by solid-state diffusion, while when  $b = 1$  the process is purely capacitive. Intermediate values  $\approx 0.75 < b < 1$  are commonly assigned to a pseudocapacitive process, or, as in this case, to a redox pseudocapacitive process, *i.e.* to a near-surface adsorption of ionic species concurrent with a faradaic process.<sup>42</sup> In Fig. 6c, the  $E$  vs.  $b$  plot is reported.

During the reduction (sodiation)  $b$  is between 0.5 and 1. Particularly, at  $E$  values corresponding to the CV peaks A and B,  $b$  approaches 0.5, consistently with a predominant faradaic process. At  $E$  values far from the faradaic reactions,  $b$  approaches 1, evidencing the occurrence of surface charge storage processes. During the oxidation scan, at potentials close to 0, where desodiation does not take place,  $b$  is close to 1 evidencing a purely capacitive process;  $b$  approaches 0.75

in the  $E$  region of peaks A' and A'', meaning that the process is, at least partially, faradaic as expected.<sup>42</sup> Furthermore, the contribution of diffusive processes vs. pseudocapacitive processes at each applied scan rate was calculated.<sup>43</sup> The results are shown in Fig. S7 (ESI<sup>†</sup>). As demonstrated in Fig. 6, the peak current has a linear relationship with the increase of the  $\nu^{1/2}$ ; however, the overall contribution to the capacity is given by the pseudocapacitive feature of the active material. Indeed, as the scan rate increases, also the pseudocapacitive contribution increases from 55% at 0.1 mV s<sup>-1</sup> up to 81% at 0.5 mV s<sup>-1</sup>.

To further characterize the kinetics of the redox processes, impedance spectra were acquired over the bias potential  $E = 0.5$  V vs. Na<sup>+</sup>/Na in the 2nd cycle and then every 10th cycles. The Nyquist plots, as well as the fit results, are shown in Fig. 7.

The Nyquist plot related to the 2nd cycle (Fig. 7a) is characterized, at a first approximation, by three main features, *i.e.*: (i) an intercept with the real axis at high frequencies, (ii) a large, suppressed semicircle at medium-to-high frequencies, and (iii) a straight line at low frequencies. The impedance dispersions have been modelled by the Equivalent Circuit method<sup>44</sup> and the relevant parameters have been calculated by NLLS fitting performed with Relaxis3 software (rhd instruments). The high-frequency intercept, describing ion migration through the electrolyte, can be modelled as a purely resistive element  $R_{\text{el}}$ . The medium-to-high frequency arc describes the migration of Na<sup>+</sup> ions through the SEI layer and the faradaic charge transfer process. These two processes can be modelled by two distinct resistive elements ( $R_{\text{SEI}}$  and  $R_{\text{ct}}$ , respectively), and are accompanied by an accumulation of charges around the surface of the SEI layer and of the active material particles, which can be modelled by parallel capacitors elements ( $C_{\text{SEI}}$  and  $C_{\text{dl}}$ , respectively). Finally, the low-frequency straight line represents a semi-infinite diffusion to a blocking electrode ( $W$  impedance in series with  $C_i$  intercalation capacitance). This results into an equivalent circuit  $R_{\text{el}}(R_{\text{SEI}}C_{\text{SEI}})[(R_{\text{ct}}W)C_{\text{dl}}]C_i$ , written in Boukamp's notation,<sup>45</sup> which models the dispersion acquired in the 2nd cycle. During the data fitting procedure, the pure capacitive elements  $C$  have been substituted by constant phase elements  $Q$ , to consider electrode inhomogeneities and roughness.<sup>44</sup> A drastic change in the shape of the

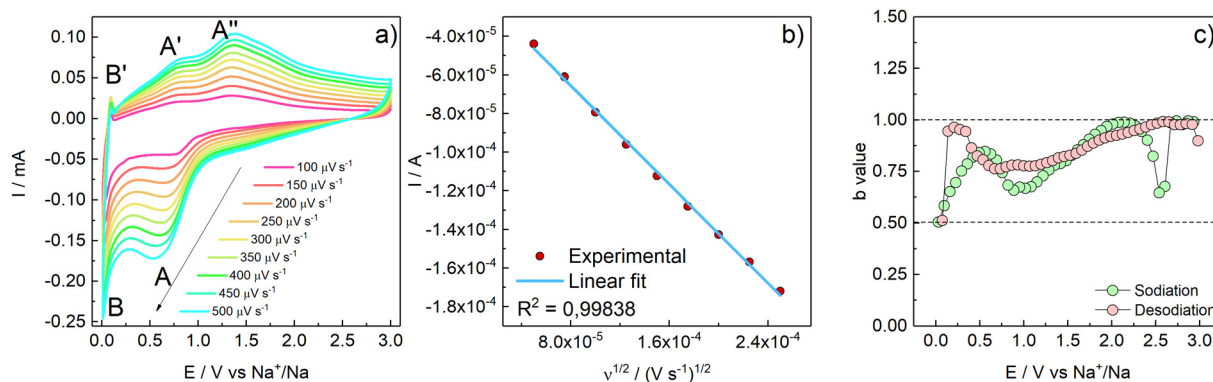


Fig. 6 (a) Cyclic voltammograms acquired at different scan rates from 100 up to 500  $\mu\text{V s}^{-1}$  (50  $\mu\text{V s}^{-1}$  increment steps). (b)  $I$  vs.  $\nu^{1/2}$  plot with linear fit of peak A. (c) calculated  $b$ -values vs.  $E$ .



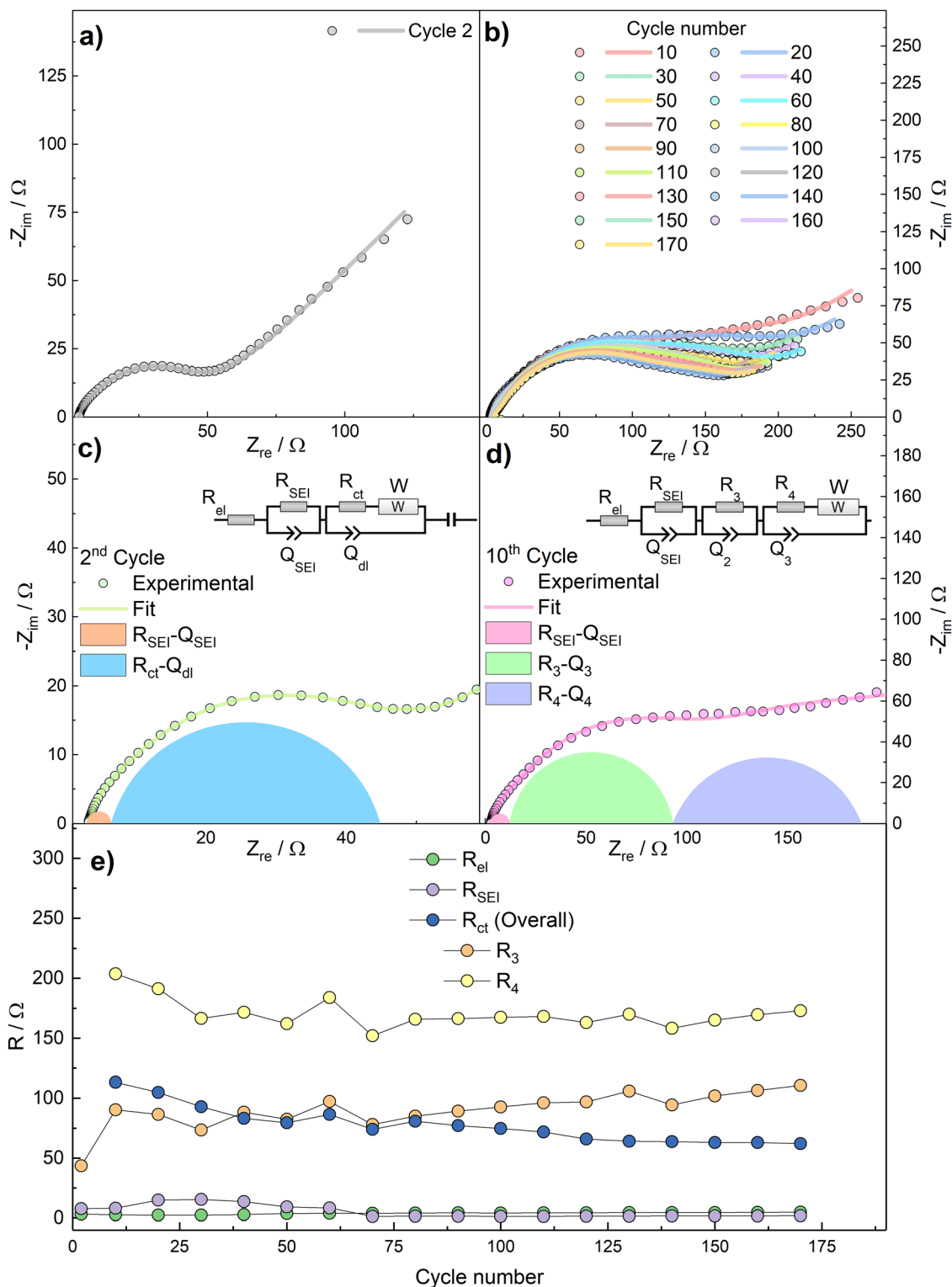


Fig. 7 Nyquist plot as well as fit of (a) 2nd cycle and (b) from 10th cycle onwards. Panel (c) and (d) graphic demonstration of the fit of the 2nd and 10th cycles, respectively. (e) Fit results obtained by using the equivalent circuit models in panels (c) and (d).

impedance spectra occurs during subsequent cycles (Fig. 7b). This phenomenon, as well as the measured specific capacity lower than the theoretical one, can be explained by the irreversible formation of a dense  $\text{Na}_2\text{O}$  layer over the active material

during the conversion reaction, which acts as a hindrance to  $\text{Na}^+$  transport. This behaviour has already been evidenced for  $\text{SnO}_2$  electrodes in NIBs configuration,<sup>46</sup> in which a specific capacity well below the theoretical one was obtained and



ascribed to sodium oxide formation. Therefore, the data from 10th cycle onwards have been more accurately fitted by deconvoluting the ( $R_{ct}C_{dl}$ ) arc into two ( $R_3C_3$ ) and ( $R_4C_4$ ) features, which take into account the formation of a further interface between the active material and the  $\text{Na}_2\text{O}$  layer, thus resulting into the equivalent circuit  $R_{el}(R_{SEI}C_{SEI})(R_3C_3)[(R_4W)C_4]C_i$ . The deconvolution of the Nyquist plots for 2nd and 10th cycles are shown in Fig. 7c and d.

Fig. 7e reports the values of  $R_{el}$ ,  $R_{SEI}$ ,  $R_{ct}$  as calculated by using the models in Fig. 7c (2nd cycle) and Fig. 7d (10th and subsequent cycles). In the latter case, the distinct  $R_3$  and  $R_4$  contributions to overall  $R_{ct}$  are reported as well.

$R_{el}$  electrolyte resistance is practically constant upon cycling, as expected.  $R_{SEI}$  shows an increasing trend during the initial cycles which can be assigned to breakage and reconstruction of a partly unstable SEI layer. This phenomenon can explain the decreasing capacity and the poor coulombic efficiencies observed in the initial cycles in Fig. 4. However, as the Coulombic efficiency increases, the values of  $R_{SEI}$  decrease and finally stabilize. This behaviour could be tentatively explained by: anisotropic growth and subsequent stabilization of the passivation layer, and the lower stability of the  $\text{Na}^+$ -ion SEI than the  $\text{Li}^+$ -ion counterpart.<sup>38</sup> The sharp increase of overall  $R_{ct}$  after the 2nd cycle can be explained with the aforementioned formation of the dense  $\text{Na}_2\text{O}$  interlayer.

In order to verify the reversibility of the  $\text{Na}^+$  uptake/release processes, *ex situ* Raman has been performed at selected potential values during the first discharge and charge half-cycles. The points highlighted in Fig. 8b represent the following

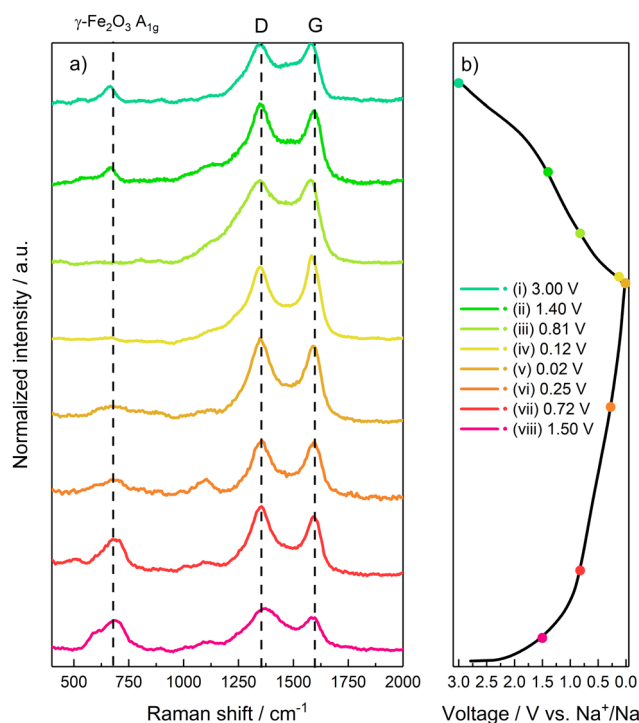


Fig. 8 *Ex situ* Raman characterization. (a) Raman spectrum acquired during the sodiation/desodiation. (b) Galvanostatic profiles with highlighted acquisitions points.

electrode states: (i) fresh electrode before conversion process and SEI formation ( $E = 1.5$  V); (ii) initial stages of  $\gamma\text{-Fe}_2\text{O}_3$  conversion and SEI formation ( $E = 0.72$  V); (iii) final stages of SEI formation and initial stages of Na-C processes ( $E = 0.25$  V); (iv) electrode fully discharged and sodiated by  $\gamma\text{-Fe}_2\text{O}_3$  conversion and Na-C uptake ( $E = 0.02$  V); (v) electrode after release of most of Na by C matrix ( $E = 0.12$  V); (vi) intermediate stages of Fe oxides formation ( $E = 0.81$  V); (vii) final stages of active material oxidation ( $E = 1.4$  V); (viii) fully charged and desodiated electrode ( $E = 3$  V).

During the electrode discharge/sodiation (Fig. 8a), all the spectra show the carbon-related D and G bands, given by graphene and SuperC65 additive. In spectra (i) and (ii) a peak located at  $667\text{ cm}^{-1}$  can be ascribed to the  $A_{1g}$  mode of  $\gamma\text{-Fe}_2\text{O}_3$ , due to the stretching of the Fe-O bond in the  $\text{FeO}_4$  tetrahedra.

Upon further discharge, as evidenced at points (iii) and (iv), the intensity of the  $\gamma\text{-Fe}_2\text{O}_3$ -related peak  $A_{1g}$  progressively decreases, becoming only a small hump at full discharge ( $E = 0.02$  V). This result confirms the conversion of  $\gamma\text{-Fe}_2\text{O}_3$  to  $\text{Fe}^0$  nanoparticles and  $\text{Na}_2\text{O}$ . However, the  $A_{1g}$  signal is still present even at the low cut-off voltage, thus evidencing that the conversion reaction does not go to completion, as confirmed by a practical capacity lower than the theoretical value. Once again, this behaviour could be tentatively explained by the formation of the  $\text{Na}_2\text{O}$  interlayer, as suggested by EIS, which could increase electrode polarization, thus forcing the cell to reach the low-potential cut-off before the conversion reaction is completed. The two constant peaks located at  $250\text{ cm}^{-1}$  and  $1000\text{ cm}^{-1}$  (labelled as \*) can be indexed to both inorganic SEI components such as  $\text{Na}_2\text{CO}_3$  or organic alkyl carbonates.<sup>47</sup> Specifically, the band located at  $1100\text{ cm}^{-1}$  can be ascribed to the stretching  $\nu$  C-O-C bonds in alkyl carbonates.

During charge (desodiation step) (Fig. 8a) a reverse behaviour can be observed through points (v) to (viii). Particularly, points (vii) and (viii) evidence the growth of the  $\gamma\text{-Fe}_2\text{O}_3$ -related  $A_{1g}$  peak, suggesting an oxidation of  $\text{Fe}^0$  to mixed  $\text{Fe}^{2+}/\text{Fe}^{3+}$  oxidation state, and thus the reversibility of the conversion reaction to  $\gamma\text{-Fe}_2\text{O}_3$ .

## 4. Conclusion

We have demonstrated that  $\gamma\text{-Fe}_2\text{O}_3$  nanoparticles, synthesized by a green and facile coprecipitation method, are a suitable anode material for Na-ion batteries. When composite electrodes with high iron oxide loading ( $\gamma\text{-Fe}_2\text{O}_3$ :rGO ratio of 80:20) are cycled in Na-ion half-cells with  $\text{NaClO}_4$ -based electrolyte, specific capacities values about  $300\text{ mA h g}^{-1}$  are obtained at specific currents in the order of  $500\text{--}1000\text{ mA g}^{-1}$ . Furthermore, outstanding rate capability is demonstrated, with specific capacity values of  $140$  and  $110\text{ mA h g}^{-1}$  obtained at  $2$  and  $5\text{ A g}^{-1}$ , respectively.

The investigation of transport properties pursued by cyclic voltammetry at different scan rates evidenced a diffusion-controlled behaviour, with predominant faradaic mechanism concurrent with a near-surface adsorption of ionic species.



Impedance analysis revealed a relevant contribution to the electrode polarization by a Na<sub>2</sub>O interlayer, formed upon conversion, and its interface with active material. *Ex situ* Raman spectroscopy shed light onto the reversibility of the conversion process, evidencing that the conversion of iron oxide to metal iron is not complete upon discharge, while  $\gamma$ -Fe<sub>2</sub>O<sub>3</sub> is formed back as the end member of the charge process.

These findings evidence that the proposed  $\gamma$ -Fe<sub>2</sub>O<sub>3</sub>/rGO composite is a very promising, sustainable, and reliable candidate anode material for Na-ion batteries.

## Author contributions

All authors contributed to this work. All authors approved the final version of the manuscript. A. S. and F. N. conceptualized the work and wrote the manuscript draft. A. S. and L. S. performed the synthesis of the material. L. M. performed the TEM measurements. L. S., L. M., L. B., H. D. contributed to the analysis and discussion. A. S. and M. M. performed the *ex situ* Raman measurements. A. T., M. H., F. P., and S. J. R. performed the synchrotron measurements.

## Conflicts of interest

There are no conflicts to declare.

## Acknowledgements

The support of ENEA and MiSE (Agenzia Nazionale per le Nuove Tecnologie, l'Energia e lo Sviluppo Sostenibile e Ministero per lo Sviluppo Economico) is gratefully acknowledged under the Project 'Sistemi di Accumulo di Energia per il Sistema Elettrico', funded by PAR2019-2021 Program. This study was carried out within the MOST e Sustainable Mobility Center and received funding from the European Union Next-GenerationEU (PIANO NAZIONALE DI RIPRESA E RESILIENZA (PNRR) e MISSIONE 4 COMPONENTE 2, INVESTIMENTO 1.4 e D.D. 1033 17/06/2022, CN00000023). This manuscript reflects only the authors' views and opinions, neither the European Union nor the European Commission can be considered responsible for them. Prof. Jusef Hassoun and Dr. Vittorio Marangon are kindly acknowledged for the TEM measurements.

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