

Life cycle assessment and life cycle costing of advanced anaerobic digestion of organic fraction
municipal solid waste

Original

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Life cycle assessment and life cycle costing of advanced anaerobic digestion of organic fraction municipal solid waste --Manuscript Draft--

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Abstract:	<p>The aim of this study is the evaluation of the environmental sustainability by means of Life Cycle Assessment (LCA) and economic profitability through Life Cycle Costing (LCC) of the 18 AD configurations carried out on Organic Fraction Municipal Solid Waste (OFMSW) at three S:I ratios (1:2, 1:1 and 2:1) for three different inoculum incubation times (0, 5 and 10 d). The adopted approach was the eco-efficiency perspective, coming from the combination of technical, environmental (LCA) and economic (LCC) perspectives. The main findings of the study were that increasing both the S:I ratio and the inoculum incubation time (5 and 10 days) the environmental impacts decreased, and economic profitability increased. In detail, the lowest values of Climate Change were achieved by the AD performed with both inocula WAS and CAS for 10 days at S:I equal to 2:1: 28.67 and 27.72 kg CO₂ eq respectively. The minimum AD plant size for which all the 18 AD configurations was economically profitable after 5 year of amortisation was 30,000 t/y of OFMSW. Capital and operational costs decreased by increasing the incubation time of the inoculum and the S:I ratio, since higher specific biogas rate was reached, and smaller AD bio-reactor volume were adopted because hydraulic retention time decreased.</p>
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1 Highlights

- 2 • Environmental sustainability and economic profitability of anaerobic digestion (AD)
- 3 • Environmental impact drops by increasing S:I ratio and inoculum incubation time
- 4 • Capex and Opex drop by increasing the inoculum incubation time and the S:I ratio
- 5 • AD at the highest S:I ratio and inoculum incubation time reach the sustainability

Author contributions statement

Authors 'contributions are detailed in the following. F. Demichelis carried out Life Cycle Assssment (LCA) and Life Cycle Costing (LCC) studies and writes part of the paper. T. Tommasi supported the study of LCA and LCC. F.A. Deorsola contributed to realise the conceptualization, methodology and data curation of the study and contribute to write and review the manuscript. D. Marchisio reviewed the manuscript. G. Mancini reviewed the manuscript. D. Fino realised the conceptualization, methodology and supervision of the study.

Environmental and Economic sustainability



OFMSW



Collection+
Transport



AD plant

Digestate

Biogas

Energy



Declaration of interests

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

The authors declare the following financial interests/personal relationships which may be considered as potential competing interests:

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1 **Life cycle assessment and life cycle costing of advanced anaerobic digestion of**
2 **organic fraction municipal solid waste**

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13 **Abbreviations**

14 AD anaerobic digestion

15 CAS cow agricultural sludge

16 ESI energy sustainable index

17 LCA life cycle assessment

18 LCC life cycle costing

19 GWP global warming potential

20 MBT mechanical biological treatments

21 MSW municipal solid waste

22 NPV Net Present Value

23 OFMSW Organic fraction municipal solid waste

24 ROI Return On Investment

25 TS Total solids

26 VS Volatile solids

27 WAS Waste activated sludge

28

29 **Abstract**

30 The aim of this study is the evaluation of the environmental sustainability by means of Life Cycle Assessment
31 (LCA) and economic profitability through Life Cycle Costing (LCC) of the 18 AD configurations carried out
32 on Organic Fraction Municipal Solid Waste (OFMSW) at three S:I ratios (1:2, 1:1 and 2:1) for three different
33 inoculum incubation times (0, 5 and 10 d). The adopted approach was the eco-efficiency perspective, coming
34 from the combination of technical, environmental (LCA) and economic (LCC) perspectives. The main findings
35 of the study were that increasing both the S:I ratio and the inoculum incubation time (5 and 10 days) the
36 environmental impacts decreased, and economic profitability increased. In detail, the lowest values of Climate
37 Change were achieved by the AD performed with both inocula WAS and CAS for 10 days at S:I equal to 2:1:
38 28.67 and 27.72 kg CO₂ eq respectively. The minimum AD plant size for which all the 18 AD configurations
39 was economically profitable after 5 year of amortisation was 30,000 t/y of OFMSW. Capital and operational
40 costs decreased by increasing the incubation time of the inoculum and the S:I ratio, since higher specific biogas
41 rate was reached, and smaller AD bio-reactor volume were adopted because hydraulic retention time
42 decreased.

43 The AD plant size, for which maximal revenues and minimal capital and operational costs were detected, was
44 50,000 t/y OFMSW. Among all the AD configurations, the environmental sustainability and economic
45 profitability were reached by test performed with inocula WAS and CAS incubated for 5 and 10 d at the highest
46 S:I ratio 2:1.

47

48 **Keywords:** organic fraction municipal solid waste (OFMSW), anaerobic digestion (AD), Life Cycle Analysis
49 (LCA), Life Cycle Costing (LCC).

50

51 **Introduction**

52 In 2019, the production of Municipal Solid Waste (MSW) in Europe ranged from 280 kg per capita in Romania
53 to 844 kg per capita in Denmark, and in Italy was equal to 500 kg per capita (Eurostat, 2021). In Europe, the
54 Organic Fraction Municipal Solid Waste (OFMSW) represented an average of 27% of MSW, equal to a
55 generation of 177 million tonnes (Eurostat, 2021). The traditional OFMSW treatments consist in mechanical

56 biological treatments (MBT), thermo-valorisation, composting and anaerobic digestion (AD). Among them,
57 anaerobic digestion (AD) is one of the most efficient and environmentally sustainable techniques for organic
58 waste remediation and valorisation (Ardolino et al., 2018). OFMSW is considered as one of the major
59 contributors to climate change, human health risk and ecosystem damages. OFMSW is a biodegradable waste
60 and so it could potentially be employed in renewable energy production processes. AD of OFMSW is a very
61 attractive option to convert the complex organic matter into a renewable and clean energy source, as biogas.
62 AD is a biochemical process by which complex organic matter are transformed into simple soluble compounds
63 in anaerobic environment. The main benefit of AD is the stabilisation of organic matter and pathogens by
64 converting them into biogas under anaerobic condition. The biogas is a gas mainly made up of methane and
65 carbon dioxide. In detail, AD is a multistep biological process made up of hydrolysis, acidogenesis,
66 acetogenesis and methanogenesis. Hydrolysis is the first and rate-limiting step, since it must reduce both
67 organic matter and high molecular compounds as carbohydrate, proteins and lipids respectively into sugars,
68 aminoacids and fatty acids. The AD of OFMSW is generally carried out at liquid state condition, which
69 means total solids (TS) ranged from 0.5 to 10%. In the present study liquid state AD was carried out, in detail
70 at 6% TS. The AD of organic matter is an environmental sustainable technique since is a carbon neutral
71 process, but it has disadvantages as long retention time, low removal efficiency organic compounds, strong
72 sensibility to the variation of pH, alkalinity, temperature, retention time, nitrogen, carbon availabilities and
73 Carbon Nitrogen (C:N) ratios which affects the AD process stability. To evaluate the environmental
74 sustainability of AD process, several studies of Life Cycle Assessment (LCA) were carried out on AD
75 performed with different organic waste as corn silage, dairy manure, food waste (Martinez-Sanchez et al.,
76 2016) and agricultural waste (Ascher et al., 2020). LCA is a methodology to assess environmental impacts
77 which covers all the life cycle of product and process. The aim of the present study is the evaluation of the
78 environmental sustainability through Life Cycle Assessment (LCA) and economic profitability through Life
79 Cycle Costing (LCC) of the AD configurations tested in (Demichelis et al., under review).

80 The adopted approach was the eco-efficiency perspective, coming from the combination of technical,
81 environmental (LCA) and economic (LCC) perspectives. In (Demichelis et al., under review) mesophilic AD
82 was performed on real OFMSW supplied by San Carlo Spa (Fossano, Italy) with two inocula, one coming
83 from the mesophilic digestate of waste activated sludge (WAS) provided by SMAT (a wastewater treatment

84 plant in the north of Italy), and the second from the mesophilic digestate of cow agricultural sludge (CAS)
85 supplied by Cascina La Speranza (Candiolo, Italy) at three substrate inoculum ratios (S:I): 1:2, 1:1 and 2:1 for
86 three inoculum incubation times: 0, 5 and 10 days. Two inocula with different origins were selected to improve
87 the C:N ratio, in particular animal sludge matter provided enhancement of C:N and buffering capacity. The
88 main output of the present study was the evaluation of optimal technical feasibility, environmental
89 sustainability, and economic profitability of AD configurations to scale them at the commercial -industrial
90 scales.

91

92 **2 Materials and methods:**

93 **2.1. Environmental sustainability**

94 Life cycle assessment was performed with SimaPro 9.0 software and it was based on ISO 14040 (2006) and
95 14044 (2006). Ecoinvent 3.0 was employed as database.

96

97 **2.1.1 Goal and scope:**

98 The goal of LCA was the evaluation of the best anaerobic digestion (AD) configurations among the 18 AD
99 configuration tested in (Demichelis et al., under review).

100 In the present study, the concept of best AD configuration means the AD configurations which reached the
101 highest technical-performances, the lowest environmental impacts and the highest economic profitability.

102 The functional unit (FU) was 1 t of wet OFMSW. The produced emissions, the consumed material and the
103 required energy were referred to the FU. The choice of FU equal to 1 t of OFMSW allowed the comparison
104 with other studies available in the scientific literature (Ascher et al., 2020). The boundary conditions included:
105 the collection and the transport of OFMSW to the the AD plant, the transport of inoculum to the AD plant, the
106 AD process and the CHP unit. The OFMSW was collected in the town and then transported to the AD plant.
107 According to (Demichelis et al., under review) AD was performed in batch feeding at 6%TS on real OFMSW
108 supplied by San Carlo Spa (Fossano, Italy), with two inocula, one coming from the mesophilic digestate of
109 waste activated sludge (WAS) provided by SMAT (a wastewater treatment plant in the north of Italy), and the
110 second from the mesophilic digestate of cow agricultural sludge (CAS) supplied by Cascina La Speranza
111 (Candiolo, Italy) at three substrate inoculum ratios (S:I): 1:2, 1:1 and 2:1 for three inoculum incubation times:

112 0, 5 and 10 days. Two inocula with different origins were selected to improve the C:N ratio, in particular
113 animal sludge matter provide enhancement of C:N and buffering capacity. Hence, a total of 18 configurations
114 of AD of OFMSW were tested. The AD was performed under mesophilic conditions 37°C with constant
115 mixing at 300 rpm. AD has two outputs: biogas and digestate. The AD configurations adopted the following
116 code: TX_Y_ZZZ, where X can be 0, 5 or 10 days representing the incubation time of the inoculum, Y is the
117 S:I ratio, in detail 1 for S:I=1:2, 2 for S:I=1:1 and 3 for S:I=2:1 and ZZZ represents the origin of the inoculum
118 WAS or CAS. Biogas was sent to CHP unit to produce electric energy ($\eta = 0.45$) and heat ($\eta = 0.55$), while
119 digestate was not valorised, in order to focus the attention only on the benefits coming from biogas-energy
120 valorisation. The adopted approach was from cradle to gate according to (Wang et al., 2020).

121

122 **2.1.2 Life cycle inventory (LCI)**

123 The LCI defined all inputs and outputs involved in the processes. The primary data came from the study of
124 (Demichelis et al., under review) and in Table 1 these data are scaled up to FU equal to 1 t of OFMSW with a
125 correction factor 0.8 (Perry, 2008). The LHV of methane was assumed equal to 35.9 MJ/m³ according to
126 (González et al., 2020). In Table 1, six AD configurations were yellow coloured since they were energetically
127 self-sufficient with Energy Sustainable Index higher than 1. The secondary data were taken from Ecoinvent
128 3.0. and reported in Table 2. According to (Brander et al., 2019) attributional LCA was applied. In detail,
129 attributional LCA means a modelling approach by which inputs and outputs were attributed to the FU of a
130 product system linking the unit processes of the system according to a normative rule. Collection and transport
131 of OFMSW were equal to 20 and 30 km respectively, while the transport of inocula, both for WAS and CAS
132 was equal to 20 km. Expansion system methodology was applied since electric and heat were re-integrated in
133 the AD system.

134

135 **2.1.3 Life cycle impact assessment (LCIA)**

136 Life cycle impact assessment was performed with the ReCiPe Midpoint (H) method. The AD system was
137 evaluated both as internal processes with energy productions and as external process including OFMSW
138 collection, OFMSW and inocula transportations and energy consumption. Both internal and external processes
139 affected global warming potential (GWP). In the present study, the analysed impact categories were: Climate

140 change (kg CO₂ eq), Ozone depletion (kg CFC-11 eq), Human toxicity, (kg 1,4-DB eq), Cancer effects (CTUh),
141 Acidification (molc H⁺ eq), Terrestrial eutrophication (molc N eq), Marine eutrophication (kg N eq,) and Land
142 use (kg C deficit). The attention will be focused on Climate Change, because in scientific literature several
143 studies were available for comparison.

144

145 **2.1.4 Interpretation data e sensitivity analysis**

146 The last step of LCA was the interpretation of the results to evaluate the achievement of the goal. A double
147 sensitivity analysis was performed to measure and detect possible variation of AD response on environmental
148 impacts. The first sensitive analysis was performed varying selected parameters as kilometre of transport and
149 collection of OFMSW, since recent studies prove that biomass yield density (t/ha·y) varied with biomass
150 supply distance (km) from biorefinery plant location. In detail, the study of (Golecha et al., 2016) stated a
151 mutual influence and dependency between biomass yield density (t/ha·y) and supply distance (km). The second
152 sensitivity analysis for LCA section was applied changing the low heating value (LHV) of biogas of the 18
153 tested AD configurations from -2.5 to+2.5% of CH₄ (% v/v) content, according to (Wang and al., 2020).

	Biogas (NL/kgvs)	CH ₄ (%)	CO ₂ (%)	Inoculum (t)	OFMSW (t)	H ₂ O (m ³)	Energy produced (kWh)	Energy consumed (kWh)	ESI (-)	EE saved (kWh)	ET saved (kWh)
T0_1_WAS	762.5	64.67	35.33	4.4	1	0.1	106.27	326.7	0.33	-99.19	-121.23
T0_2_WAS	731.24	62.76	37.24	2.2	1	0.47	98.91	226.51	0.44	-57.42	-70.18
T0_3_WAS	708.12	62.53	37.47	1.1	1	0.65	95.43	182.89	0.52	-39.36	-48.11
T0_1_CAS	782.58	66.01	33.99	3.74	1	0.76	111.33	326.7	0.34	-96.91	-118.45
T0_2_CAS	755.89	64.84	35.16	1.87	1	0.8	105.63	191.66	0.55	-38.71	-47.32
T0_3_CAS	748.89	61.74	38.26	0.94	1	0.81	99.65	169.83	0.59	-31.58	-38.6
T5_1_WAS	818.52	61.8	38.2	4.4	1	0.1	109.03	274.43	0.4	-74.43	-90.97
T5_2_WAS	835.95	62.8	37.2	2.2	1	0.47	113.15	217.8	0.52	-47.09	-57.56
T5_3_WAS	932.06	64.5	35.5	1.1	1	0.65	129.57	128	1.01	0.71	0.87
T5_1_CAS	840.49	63.82	36.18	3.74	1	0.76	115.61	248.29	0.47	-59.71	-72.97
T5_2_CAS	859.49	65	35	1.87	1	0.8	120.41	165.53	0.73	-20.3	-24.81
T5_3_CAS	948.68	67.57	32.43	0.94	1	0.81	138.16	117.58	1.18	9.26	11.32
T10_1_WAS	849.69	67.9	32.1	4.4	1	0.1	124.35	287.5	0.43	-73.42	-89.73
T10_2_WAS	890.96	68.2	31.8	2.2	1	0.47	130.97	121.97	1.07	4.05	4.95
T10_3_WAS	994.2	69	31	1.1	1	0.65	147.86	117.58	1.26	13.63	16.65

T10_1_CAS	846.41	68.31	31.69	3.74	1	0.76	124.62	222.16	0.56	-43.89	-53.65
T10_2_CAS	892.2	69.85	30.15	1.87	1	0.8	134.32	121.97	1.1	5.56	6.79
T10_3_CAS	997.81	70	30	0.94	1	0.81	150.54	117.58	1.28	14.84	18.13

155 **Table 1:** Primary data of LCI based on (Demichelis et al, under revision) scaled up to the FU = 1t of OFMSW

156

Transport	Transport, freight, lorry 16-32 metric tons, Euro 6
Electricity	Electricity, high voltage (IT) electricity production oil
Heat	Heat, central or small scale, other than natural gas (CH), heat production at heat pump 30kW
Water	Water from natural resource

157 **Table 2:** Secondary data from Ecoinvent 3.0

158 **2.3 Economic analysis**

159 Economic feasibility was studied by Life Cycle Costing (LCC). LCC is an assessment of all costs related to
160 the production of a product or service, considering the whole life cycle from production to usage until disposal.
161 The LCC was carried out in three main modules: data collection, cost estimation and data interpretation. The
162 target of LCC was the evaluation of the economic cost of the whole life cycle of anaerobic digestion process,
163 with the aim to reduce and minimise the cost of production. In this study, the result of LCC is the definition of
164 the economic dimension of the AD process. LCC was performed from the viewpoint of producers. According
165 to LCA (paragraph 2.1.1), the same goal and scope, system boundary and functional unit were adopted to
166 perform LCC to obtain an overall consistent analysis.
167 LCC was calculated considering capital investment, operational costs, profitability of the anaerobic digestion,
168 Net Present Value (NPV), Return On Investment (ROI) and payback time. The LCC was performed on the
169 minimum AD plant size for which economic profitability was achieved.

170 **2.3.1 Capital cost evaluation**

171 Capital cost (Table3) included the purchase of reactors and facilities for the construction and the installation.
172 The cost of land was not considered since the analysis was not geo-referred. In fact, the target of the economic
173 analysis was the evaluation of the economic profitability of the proposed AD configurations. The tax of interest
174 was equal to 2% with a 5-years of amortization. The amortization was calculated with Eq. 1:

175
$$A(\text{euro}) = C_0 \cdot \frac{i \cdot (1+i)^n}{(1+i)^n - 1} \tag{1}$$

176 where A means the amortization cost, C_0 is the capital investment, n the number of years of amortisation and i
177 is the tax of interest.

178

Technique	Unit	Cost(Euro/unit)	References
Grinder	kg/s	2323.3	(Eurostat, 2021)
Bio-digestor	m ³	2514.7	(González et al., 2020)
Stirrer	kW	46465.3	(Akeberg et al., 2000)
Centrifuge	kg/s	116163.2	(Akeberg et al., 2000)
Heat exchanger	m ²	889.96	(Akeberg et al., 2000)

179 **Table 3:** List of capital costs.

180

181 2.3.2 Operational cost evaluation

182 The operational costs (Table 4) included the cost of the collection and transport of OFMSW to the AD plant,
183 the maintenance of the equipment, the disposal of AD residues, the labours and the utilities necessary to run
184 the processes as fuel, steam, heat and electricity.

185

Technique	Operation	Unit	Cost (Euro/unit)	References
Raw material	Collection of OFMSW	Euro/t	0.21	(ISPRA, 2021)
	Inoculum	Euro/m ³	2.10	(Demichelis et al., 2018)
	Process water	Euro/m ³	0.13	(Akeberg et al., 2000)
Water and energy consumption	Power	Euro/kWh	0.034	(Akeberg et al., 2000)
	Electric power	Euro/MW	5.24	(Wingre et al., 2003)
	Steam boiler	Euro/MW	72.80	(Wingre et al., 2003)
	Steam for AD process	Euro/kg	0.2	(Akeberg et al., 2000)
	Waste disposal	Euro/t	40.00	(ISPRA, 2021)
	Labor	Euro/year	44966.40	(ISTAT, 2021)

186 **Table 4:** List of operational costs.

187

188 2.3.3 Revenue and evaluation of profitability

189 The market value of electric energy is 0.20 euro/kWh and thermal energy of 0.201 euro/kWh (Eurostat
190 statistic, 2021). The annual profit was the difference between the revenue and the sum of the amortisation and
191 operational costs.

192 To complete the evaluation of the profitability the NPV, ROI and payback time were calculated.

193 NPV (Eq. 2) pointed out the profitability of the AD configuration considering a plant lifetime of 20 years
194 considering a 5% discount for the future cash flows referring to the present value. According to (Pleissner et
195 al., 2016), NPV > 0 means that AD process is profitable.

196 $NPV (euro) = \sum_{t=1}^T \frac{C_t}{(1+d)^t} - C_0$ (2)

197 where, C_t is the net cash flow during period t , C_0 is the initial capital investment, t is the plant lifetime and d
198 is the discount rate.

199 ROI (Eq. 3) was defined as key parameter to evaluate the performance of the profitability of an investment

200 $ROI (\%) = \frac{\text{Annual net profit}}{\text{Initial total investment}} \cdot 100$ (3)

201 In details, to calculate ROI the annual net profit after 5 years of amortization was considered. Payback time
202 states the time required to regain the funds expended in capital costs.

203

204 **2.3.4 Economic sensitivity analysis**

205 Two sensitivity analysis were performed. The first sensitivity analysis for LCC was performed as sensitivity
206 for LCA, by changing the LHV of CH_4 of the 18 AD configurations tested from -2.5 to +2.5% of CH_4 (% v/v)
207 content, according to (Wang and al., 2020). The second sensitivity analysis was performed by floating the CH_4
208 price of $\pm 20\%$ according to (Li et al., 2020).

209

210 **3.Results:**

211

212 **3.1 Environmental sustainability.**

213 Life Cycle Assessment (LCA) was carried out on the 18 AD configurations tested in (Demichelis et al., under
214 review) and the following impact categories were analysed: Climate change (kgCO₂ eq), Ozone depletion (kg
215 CFC-11 eq), Human toxicity, Cancer effects (CTUh), Acidification (molc H⁺ eq), Terrestrial eutrophication
216 (molc N eq), Marine eutrophication (kg N eq.) and Land use (kg C deficit). Global warming potential (GWP)
217 was significantly affected by OFMSW management practices involving significant GHG emissions. The
218 emissions due to collection and transport of OFMSW, AD of OFMSW and biogas utilisation were summed
219 up. Conventional OFMSW managements were evaluated to underline the pros coming from to the proposed
220 AD management. In details, incineration and landfilling achieved 107 kg CO₂ eq and 209 kg CO₂ eq,
221 respectively, these results agreed with (Cremiato et al., 2018).

222 In the present study, the reduction of GHG emission was due to the use of produced biogas as thermal energy
223 to heat the bio-digester. This pro was detected in the AD configurations with Energy Sustainable Index (ESI)
224 major than 1; the AD performed both with inocula WAS and CAS for incubation time of 5 and 10 d at S:I
225 ratios equal to 1: 1 and 2:1 (Table 1, yellow coloured): T5_3_WAS, T5_3_CAS, T10_2_WAS, T10_2_CAS,
226 T10_3_WAS and T10_3_CAS. In Figure 1, the GWP reached by the 6 AD configuration with ESI major than
227 1 was depicted considering the GWP contribute of each phase of AD process. The highest environmental items
228 were OFMSW and inoculum transport, according to (Golecha et al., 2016).

229 Since the produced biogas was employed as energy vector part of electric and thermal energy were saved and
230 negative Climate change values were evaluated. It is important to underline that many LCA studies about
231 organic waste, food waste and OFMSW were performed in scientific literature, but it is challenging to make
232 analogies and comparisons due to the different system boundaries, FU, and life cycle impact methodologies.

233 Moreover, the most adopted AD system is made up of the following units: AD unit, biogas utilisation with a
234 biogas engine and digestate treatment as fertiliser. In the present study, digestate valorisation was not
235 considered since the attention was focused only on pros and cons of biological waste to energy process based
236 on the experimental results achieved in (Demichelis et al., under review). Table 5 depicts that increasing both
237 the S:I ratio and the inoculum incubation time (5 and 10 days) the environmental impacts decreased, since
238 higher amount of OFMSW was valorised and specific production of biogas with higher methane content was
239 achieved. In details, the environmental impacts of AD performed both with inocula WAS and CAS at the
240 lowest S:I (1:2) and lowest inoculum incubation time (0 days), were higher than the ones achieved by the AD
241 performed both with inoculum WAS and CAS with the highest S:I (2:1) and the highest inoculum incubation
242 time (10 days).

	Climate change	Ozone depletion	Human toxicity, cancer effects	Acidification	Terrestrial eutrophication	Marine eutrophication	Land use
Unit	kg CO ₂ eq	kg CFC-11 eq	CTUh	molc H+ eq	molc N eq	kg N eq	kg C deficit
T10_3_WAS	28.67	3.9E-03	2.1E-07	0.15	0.20	0.02	50.17
T10_2_WAS	38.19	5.2E-06	2.8E-07	0.19	0.27	0.02	68.67
T10_1_WAS	82.61	1.1E-05	6.4E-07	0.45	0.61	0.05	129.27
T5_3_WAS	37.00	5.2E-06	3.0E-07	0.21	0.29	0.03	59.73
T5_2_WAS	62.36	8.0E-06	4.7E-07	0.34	0.45	0.04	88.75
T5_1_WAS	85.63	1.1E-05	6.2E-07	0.43	0.59	0.05	126.77
T0_3_WAS	50.71	6.4E-06	3.8E-07	0.28	0.37	0.03	68.48
T0_2_WAS	64.37	8.2E-06	4.8E-07	0.35	0.46	0.04	90.42
T0_1_WAS	94.67	1.2E-05	7.1E-07	0.51	0.68	0.06	136.78
T10_3_CAS	27.52	3.7E-06	2.0E-07	0.14	0.19	0.02	47.68
T10_2_CAS	36.33	4.9E-06	2.7E-07	0.18	0.26	0.02	63.96
T10_1_CAS	68.40	9.0E-06	5.1E-07	0.36	0.49	0.04	108.61
T5_3_CAS	30.38	4.1E-06	2.2E-07	0.16	0.22	0.02	50.05
T5_2_CAS	49.23	6.4E-06	3.7E-07	0.26	0.35	0.03	74.67
T5_1_CAS	74.43	9.7E-06	5.6E-07	0.39	0.53	0.05	113.61
T0_3_CAS	47.17	6.0E-06	3.5E-07	0.26	0.34	0.03	64.01

T0_2_CAS	55.25	7.1E-06	4.1E-07	0.30	0.40	0.04	79.67
T0_1_CAS	92.51	1.2E-05	6.9E-07	0.50	0.67	0.06	128.63

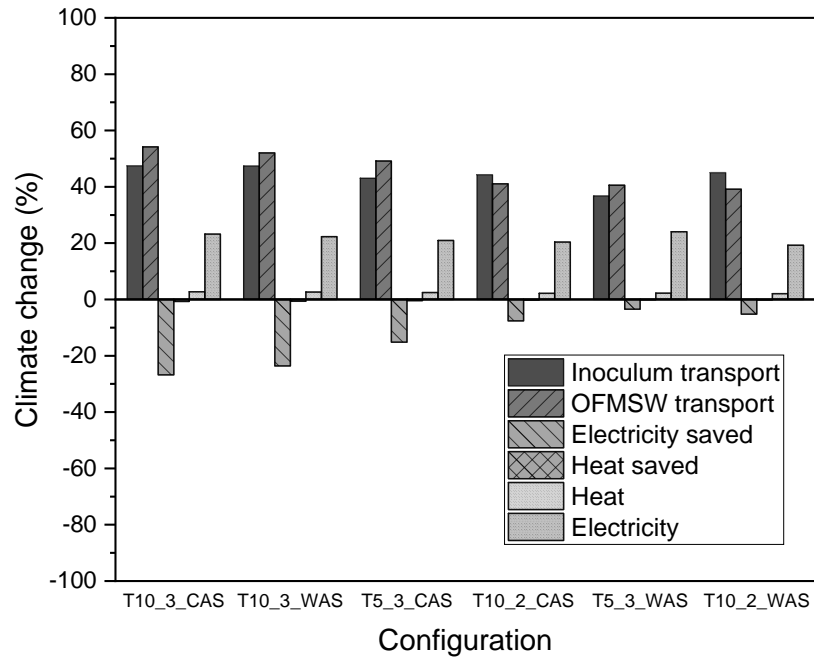
244 **Table 5:** Environmental impacts of the 18 AD configurations

245

246 In detail, the Climate change of AD with inoculum non incubated was + 69.98 % \pm 0.37, Ozone depletion was + 68.29 % \pm 0.24, Human toxicity was +70.61 % \pm
247 0.40, the Acidification was + 71.41 % \pm 0.47, Terrestrial eutrophication, was + 70.45 % \pm 0.41, Marine eutrophication was + 70.48 % \pm 0.41 and Land use was +
248 63.12 % \pm 0.27, higher than AD performed with inocula incubated for 10 d at the highest S:I ratio (2:1). We focused more attention on Climate change, since it is
249 the most studied impact category in scientific literature. For the Climate change impact category, the present study considered the contribution of biogenic carbon,
250 with a factor of biogenic CO₂ equal to 1.

251 In the present study, the highest GWP values were reached by the following configurations: AD performed with inoculum WAS and CAS without incubation (0
252 day) at S:I ratio equal to 1:2: T0_1_WAS reached 94.67 kgCO₂/t OFMSW and T0_1_CAS achieved 92.51 kgCO₂/t. These results agreed with the study of (Ascher
253 et al., 2020) who performed the AD of food waste both neglecting and considering the biogenic CO₂ and reached -97.27 and 140.50 kgCO₂ eq per 1 t of food waste
254 and with the study of (Jin et al., 2015) which reached 96.97 kgCO₂/t of food waste in mesophilic liquid AD, with S:I ratio equal to 1:2. In Climate change category
255 (Figure 1, in which are reported only the AD configurations with ESI >1), the inoculum played a key role, since decreasing the S:I ratio (1:2) the amount of inoculum
256 increased, increasing the reactor volume and the CO₂ emissions rather than AD configurations with higher S:I (1:1 and 2:1). Moreover, increasing both the S:I ratio
257 and the incubation time, the specific biogas production and the CH₄ content in the biogas increased, with a consequential decrease of CO₂ emissions and thermal
258 energy required to heat the bio-digester, since biogas was sent to CHP unit. The GWP values of T10_3_WAS and T10_3_CAS were 28.67 and 27.52 kg CO₂,
259 respectively according to (Fei et al., 2021) which reached 29.24 kg CO₂ per 1 t of food waste treated with solid and liquid AD processes. The AD performed both

260 with CAS and WAS incubated for 5 days at S:I equal to 1:2 (T5_1_WAS and T5_1_CAS) agreed with the study of (Fei et al., 2021) which reached 77.9 kg CO₂
261 per 1 t of food waste treated with solid and liquid AD processes.



262

263 **Figure 1:** Climate change values of the AD configuration with ESI major than 1

264 According to (Ascher et al., 2020) the CHP unit contribute to GWP ranged between 20-30% of total GWP
 265 estimated.

266 Usually, dairy waste management consists in stockpiling and land application which caused 307 and 204 kg
 267 CO₂ eq per ton respectively, according to (Adghim et al., 2020). In the present study, 9 AD configurations
 268 adopted as inoculum the digestate coming from cow agricultural sludge (CAS) and the reached GWP witnessed
 269 the positive valorisation of both matrix CAS (as inoculum) and OFMSW (as substrate), which achieved a
 270 minimum GWP with T10_3_CAS (27.52 kg CO₂ eq) and maximum T0_1_CAS (92.52 kg CO₂ eq). Moreover,
 271 the AD performed with inoculum CAS achieved GWP lower than the one using WAS as inoculum, in the
 272 range of - 4.18 to - 16.51%. This trend was in line with the study of (Cristóbal et al., 2018).

273 Considering the ESI (Table 1) and Climate change values (Table 5 and Figure 1) of all AD configurations with
 274 ESI major than 1; the decrease of kgCO₂ eq emissions matched with the increase of ESI values. In terms of kg
 275 CO₂ eq released, the best AD configurations were AD performed with both CAS and WAS inoculum incubated
 276 for 10 day at S:I ratio equal to 2:1 (T10_3_CAS and T10_3_WAS), AD with both CAS and WAS incubated
 277 for 10 d at S:I ratio equal to 1:1 (T10_2_CAS and T10_2_WAS), and AD with both CAS and WAS incubated
 278 for 5 d at S:I ratio equal to 2:1 (T5_3_CAS and T5_3_WAS). These trends agreed with multi-criteria decision
 279 ranking reported in (Demichelis et al., under review) performed with ELECTRE II. The AD performed both

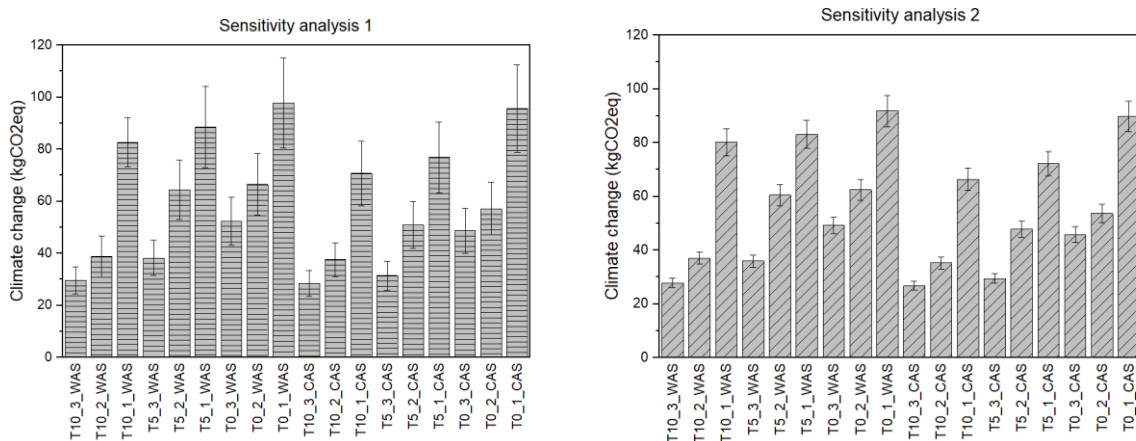
280 with inocula CAS and WAS at the highest S:I ratio (2:1) for the highest inocula incubation time (10 d) reached
 281 the lowest Human toxicity, Ozone depletion, Cancer effect, Acidification, Terrestrial eutrophication, Marine
 282 eutrophication, and Land uses values. These values agreed with (Fei et al., 2021). These outputs were due to
 283 the higher valorisation of OFMSW reached working at higher S:I ratio and the correct disposal of digestate.
 284 According to (Martinez-Sanchez et al., 2016) the main contribution to the above-mentioned impact categories
 285 was the application of digestate as fertiliser.

286

287 3.2.2 Environmental sensitivity analysis

288 Two sensitivity analysis were performed. The first sensitive analysis was performed varying the following
 289 parameters: kilometre of transport and collection of OFMSW, since recent studies prove that biomass yield
 290 density (t/ha·y) varied with biomass supply distance (km) from biorefinery plant location. The transport of
 291 OFMSW was increased and decreased respectively of plus and minus 10 km. In detail, according to the study
 292 of (Golecha et al., 2016) a mutual influence and dependency between biomass yield density (t/ha·y) and supply
 293 distance (km) was detected and the trend of GWP of the 18AD configurations did not change, but increasing
 294 the transport (km) the GWP increase about 23-18% (Figure 2). The second sensitivity analysis for LCA was
 295 applied changing the LHV of biogas of the 18 tested AD configuration of $\pm 2.5\%$ of CH₄ (%v/v) content,
 296 according to (Wang et al., 2020). Sensitivity analysis, performed by changing the LHV of CH₄, witnessed that
 297 GWP values ranged from -1.68. to +5.65 %, but the trend of the tested 18 AD configurations did not change
 298 (Figure 2). To conclude, the environmental analysis proved that increasing both the S:I ratio and the inoculum
 299 incubation time the environmental impacts decreased.

300



301 **Figure 2:** Sensitivity analysis. Sensitivity analysis 1 obtained by changing the transports of inoculum and
 302 OFMSW +10 km and -10 km. Sensitivity analysis 2 obtained by changing the LHV of methane, +2.5 % -2.5
 303 %.

304

305 **3.3 Economic sustainability**

306 To develop economic analysis Life Cycle Costing was performed and a quantitative cost engineering technique
 307 was applied, in detail analytical technique, which considers product as a decomposition of a series of
 308 elementary operations and activities. In this way, the costs were estimated as a sum of all the components, both
 309 for investment and operational costs. The analytical technique was adopted since it was the most accurate and
 310 consistent approach for cost estimation, according to (Altavilla et al., 2015).

311 Value analysis was carried out and it should maximize the difference between value and cost, trying to reduce
 312 waste, which is an element or part of the process that does not add value.

313 Capital and operational costs, revenues, incomes, ROI, NPV and payback time were calculated. The study was
 314 carried out on AD plant of 30,000 t of OFMSW per year since it was the minimum size for which all the 18
 315 AD configurations were profitable after 5 years of amortisation.

316

317 **3.3.1 Capital cost**

318 The AD plant had a service life equal to 20 years and 5 years of amortisation of capital cost according to (Li
 319 et al., 2020) AD feed mood was carried out in batch series, since the inoculum played a key role as proved in
 320 (Demichelis et al., under review) reaching methane yields +38.2 % v/v higher than traditionally AD of
 321 OFMSW. The capital costs included bio-reactor construction, CHP unit, and plant costs, which were both the
 322 direct and the indirect costs to realise the plant as buildings, purchase of equipment, instrumentation, and
 323 facilities according to (Li et al., 2020).

324

	HRT (d)	Inoculum (t)	H ₂ O (m ³)	Working.volume reactor(m ³)	Volume reattor(m ³)
T0_1_WAS	27	132000	2998.88	14849.9	18562.37
T0_2_WAS	27	66000	14000	9900	12375
T0_3_WAS	28	33000	19500	7700	9625

T5_1_WAS	20	132000	2998.88	10999.93	13749.91
T5_2_WAS	18	66000	14000	6600	8250
T5_3_WAS	16	33000	19500	4400	5500
T10_1_WAS	18	132000	2998.88	9899.93	12374.92
T10_2_WAS	16	66000	14000	5866.67	7333.33
T10_3_WAS	16	33000	19500	4400	5500
T0_1_CAS	27	133980	22755.1	16806.16	21007.7
T0_2_CAS	25	66990	23877.55	10072.3	12590.37
T0_3_CAS	27	33495	24438.78	7914.04	9892.55
T5_1_CAS	20	133980	22755.1	12449.01	15561.26
T5_2_CAS	21	66990	23877.55	8460.73	10575.91
T5_3_CAS	15	33495	24438.78	4396.69	5495.86
T10_1_CAS	16	133980	22755.1	9959.21	12449.01
T10_2_CAS	15	66990	23877.55	6043.38	7554.22
T10_3_CAS	19	33495	24438.78	5569.14	6961.42

325 **Table 6:** Detail of AD plant for size 30,000 t/y (the minimum size economic profitable for all the 18 AD
326 configuration tested).

327

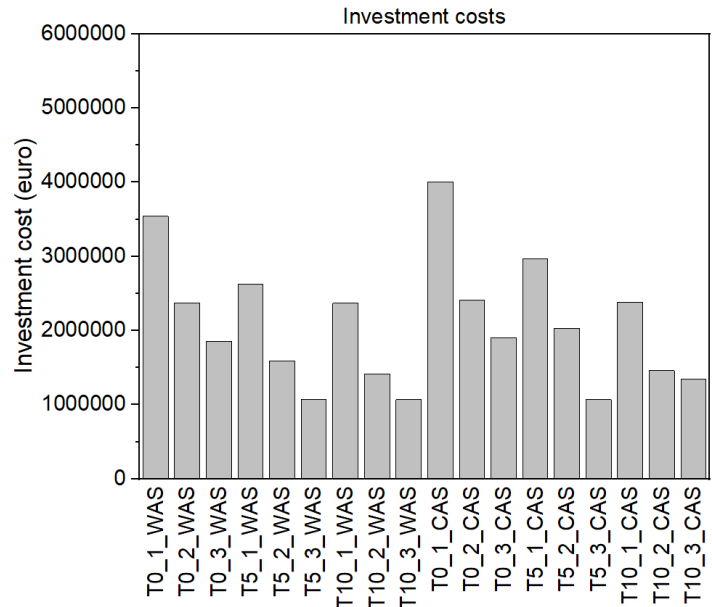
328 In Table 6, the features of AD bio-reactor of a plant of 30,000 t of OFMSW per year and 2105.4 t of digestate
329 was reported.

330 30,000 t of OFMSW per year was studied since was the minimum size for which all the 18 AD configuration
331 were profitable after 5 years of amortisation.

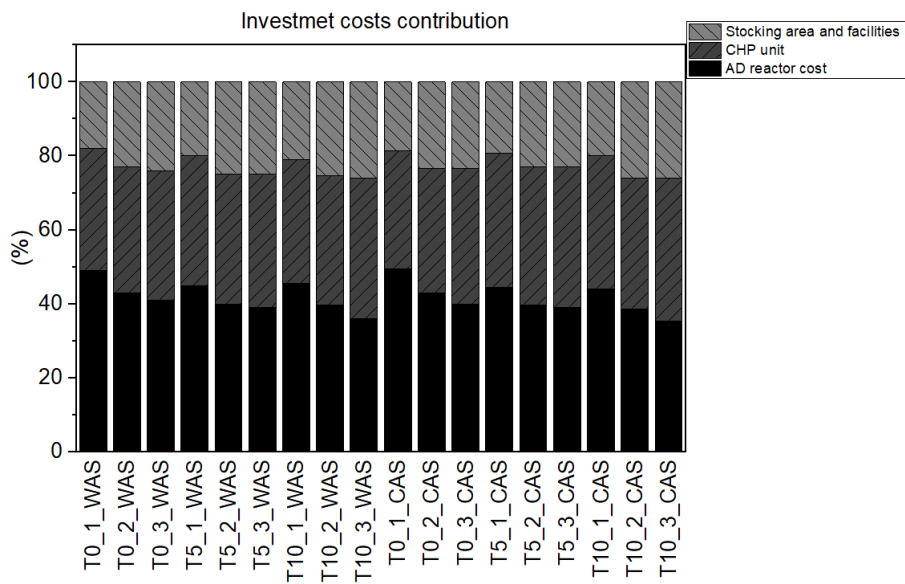
332 The capital costs of the 18 AD configurations are depicted in Figure 3 as total investment costs (euro) and
333 percentage contribute of each item (%). In detail, increasing the incubation time of the inoculum (5 and 10 d)
334 and the S:I ratio both with CAS and WAS, the bio-reactor size decreased, because the HRT of the process
335 decreased, and consequentially its purchase decreased from 49.00 % (T0_1_WAS) to 35.33% (T10_3_CAS)
336 of total capital cost. Increasing the S:I ratio (1:1 and 2:1) and the inoculum incubation (5 and 10 d) the CHP
337 unit cost contribution increased, since higher biogas rate was achieved. The capital costs of AD performed

338 both with WAS and CAS inocula incubated for 10d at S:I ratio equal to 2:1 agreed with the ones reached by
 339 (Patinvoh et al., 2017) with dry AD.

340 The capital costs of AD performed with inocula incubated for 5 and 10 d at higher S:I ratio (1:1 and 2:1) were
 341 like the ones obtained with dry AD (Qian et al., 2015).



342



343

344 **Figure 3:** Capital costs (euro) and contribution percentage in capital costs (%)

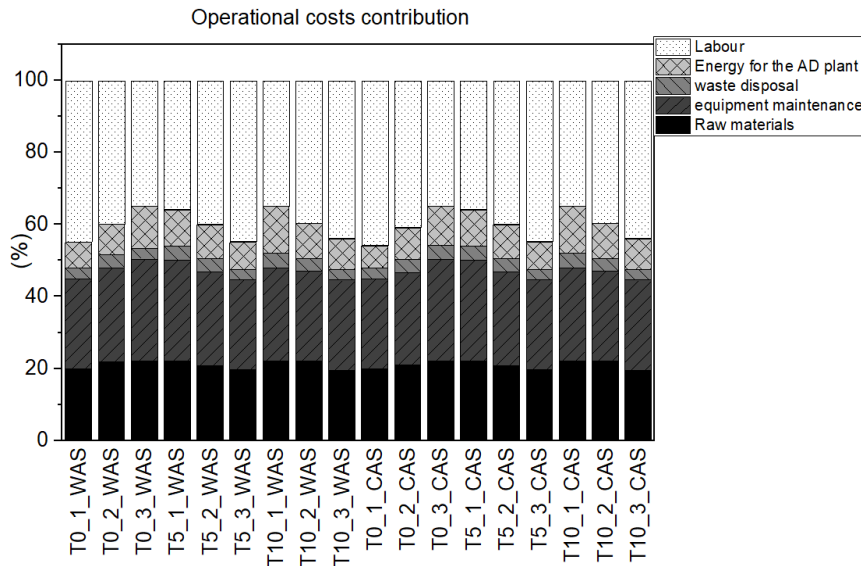
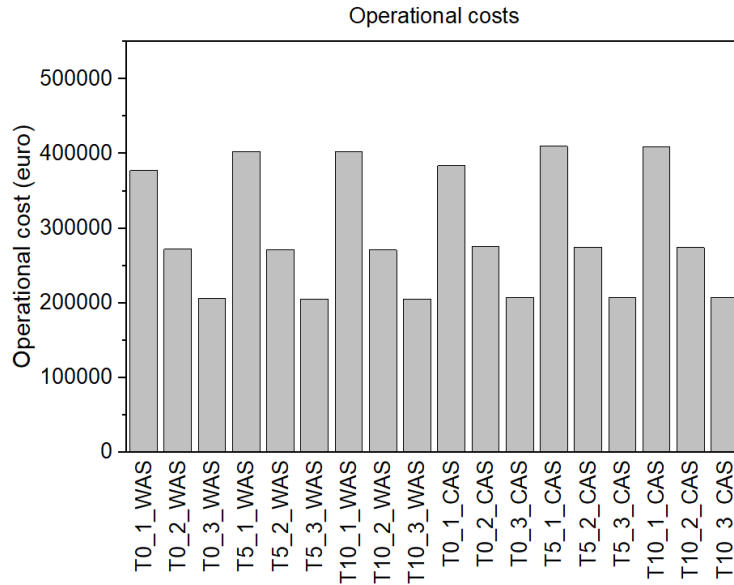
345

346 **3.3.2 Operational costs**

347 Operational costs included the cost of the raw material (i.e. transport of inoculum, the collection and transport
348 of OFMSW to the AD plant), the equipment maintenance, the disposal of waste and residues, the labours and
349 the utilities necessary to run the processes as fuel, steam, heat and electricity.

350 The operational costs of the 18 AD configurations are depicted in Figure 4 as total operational costs (euro) and
351 percentage contribute of each items (%). The costs of raw materials, equipment maintenance, waste disposal
352 and labour costs were constant among the 18 configurations. The key item was the energy (electrical and
353 thermal) costs. In details, two trends were detected. The first trend was: for AD performed with non incubated
354 inoculum the energy required increase by increasing the S:I ratio, since low specific biogas rate and long HRT
355 were reached. This trend agreed with liquid AD performed by (Li et al., 2020).

356 The second trend was: for AD performed with incubated inoculum, the required energy decreased by
357 increasing the S:I ratio, since high specific biogas rate and short HRT were reached. This trend agreed with
358 (Qian et al., 2015).



359

360

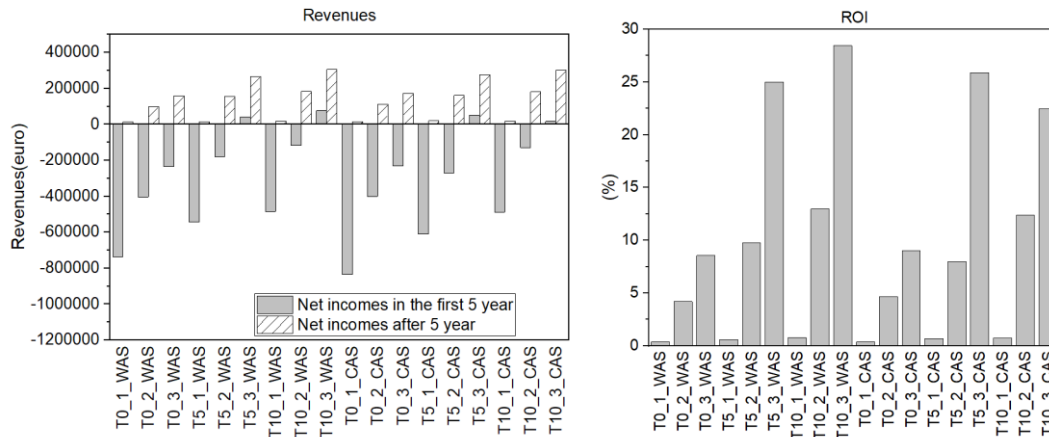
361 **Figure 4:** Operational costs (euro) and percentage contribution (%)

362

363 **3.3.3 Revenues**

364 Figure 5 depicts the incomes of the 18 AD configurations due to the differences between biogas trade and
 365 capital and operational costs, before and after 5 years of amortization and ROI after 5 years of amortization.
 366 In the first 5 years of life AD plant the only profitable configurations were AD performed with both inocula
 367 CAS and WAS incubated for 5 and 10 d at the highest S:I (2:1), respectively: T5_3_WAS, T10_3_WAS
 368 T5_3_CAS, T10_3_CAS. After 5 years of amortization all the 18 AD configurations were profitable and
 369 among them the most profitable were: T10_3_WAS, T10_3_CAS. followed by T5_3_CAS and T5_3_WAS.

370 The incomes achieved by these configurations agreed with wet AD performed (Demichelis et al., 2018) for
 371 AD plant. To scrutinize the economic assessment of the above mentioned profitable configurations, Net
 372 Present Value (NPV), Return of Investment (ROI) and payback time were calculated (Table 7).



373

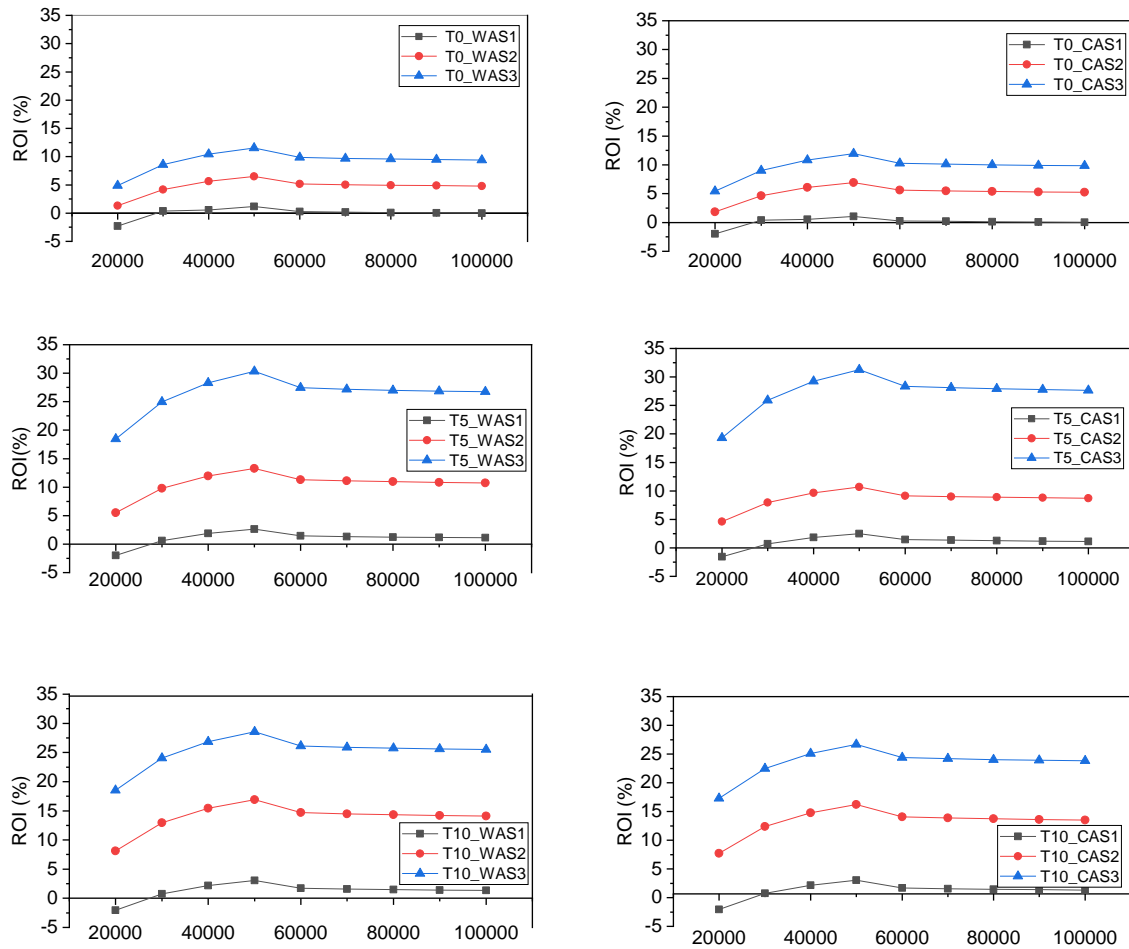
374 **Figure 5:** Revenues (euro) and ROI (%)

AD configurations	ROI (%)	payback time (y)	NPV (euro)
T5_3_WAS	24.99	10	2,348,887.37
T10_3_WAS	28.45	11	2,810,068.86
T5_3_CAS	25.89	10	2,467,367.73
T10_3_CAS	22.47	12	2,534,258.31

375 **Table 7:** Economic key indicator to evaluate the profitability of the 18 AD configurations

376

377 In particular, only four AD configuration (the AD performed with inocula WAS and CAS incubated for 5 and
 378 10 d at the highest S:I ratio) had payback time minor of 20 y (the life service of the AD plant), NPV positive
 379 and ROI higher than 20%. Among them, the T5_3_WAS reached best fit NPV, ROI and payback time,
 380 respectively 2,810,068.86 euro, 28.45% and 11 y. The minimum size for which all the 18 AD configuration
 381 were profitable after 5 years of amortization was 30,000 t/y of OFMSW. To identify the best fit between
 382 capital, operational costs and revenues the study of ROI was performed for AD plant size from 20,000 t/y to
 383 100,000 t/y (Figure 6). The best fit of economic assessment was detected for AD plant size equal to 50,000 t/y
 384 according to (Demichelis et al., 2018) (Arias et al., 2020).



385

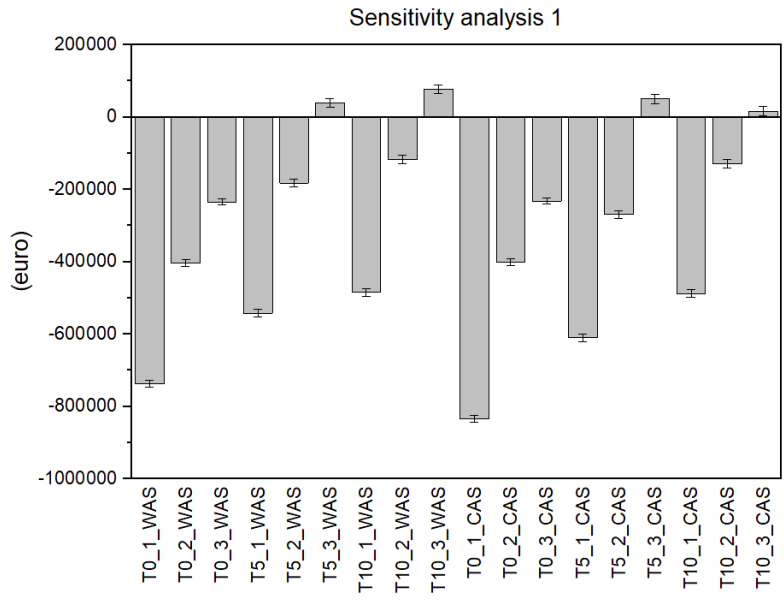
386 **Figure 6:** Evaluation of the AD plant size to obtain the maximal benefit CAPEX and OPEX. On x -coordinate
 387 is reported the t of OFMSW per year considered.

388

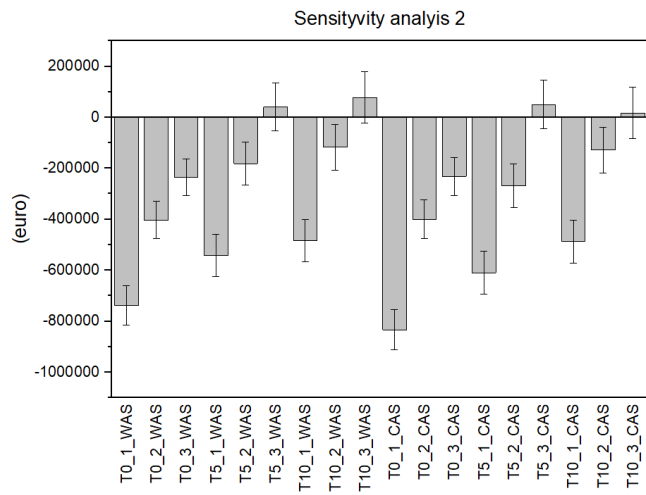
389 3.3.4 Economic sensitivity analysis

390 Two sensitivity analysis were performed. The first economic sensitivity analysis (Figure 7) was carried out as
 391 the sensitivity for LCA, by changing the LHV of biogas of the 18 tested AD configuration from -2.5 to+2.5 %
 392 of CH₄ (%v/v) content, according to (Wang et al., 2020). The sensitivity analysis was performed considering
 393 the net revenues in the first 5 years of amortisation. Even if, the LHV of CH₄ was increased and decreased of
 394 ± 2.5 %, the AD configuration economic profitable in the first 5 years of amortisation were T5_3_WAS,
 395 T10_3_WAS, T5_3_CAS, T10_3_CAS. These results confirmed the outputs of economic assessment
 396 described in sections 3.3.1, 3.3.2 and 3.3.3. In detail, among the profitable configurations: 1) increasing the
 397 LHV of +2.5 % the revenues in the first 5 years of amortization was increased in the range from +22.42 % to
 398 +42.71 %, respectively for T5_3_WAS and T10_3_CAS.; 2) decreasing the LHV of -2.5 % the revenues in

399 the first 5 years of amortization was decreased from 21.73% to 31.7 % respectively for T5_3_WAS and
400 T10_3_CAS. The second sensitivity analysis (Figure 7) was performed by floating the biogas price of $\pm 20\%$
401 according to (Li et al., 2020).
402 Even if, the price of CH₄ was increased and decreased of $\pm 20\%$, the AD configuration economic profitable in
403 the first 5 year of amortisation were T5_3_WAS, T10_3_WAS T5_3_CAS, T10_3_CAS. Among the
404 profitable configurations: 1) increasing the price of CH₄ of +20 % the revenues in the first 5 years of
405 amortization were increased in the range from 20.11 % to 41.54 %, respectively for T5_3_WAS and
406 T10_3_CAS; 2) decreasing the price of CH₄ of -20% the revenues in the first 5 years of amortization were
407 decreased from 19.8 % to 29.72 % respectively for T5_3_WAS and T10_3_CAS. To conclude the economic
408 sensitivity analysis, the following state can be asserted: by changing the LHV of CH₄ about $\pm 2.5\%$ and the
409 price of CH₄ in the range of $\pm 20\%$, the AD configuration economically profitable were always: T5_3_WAS,
410 T10_3_WAS T5_3_CAS, T10_3_CAS.



411



412

413 **Figure 7:** Economic sensitivity analysis. Sensitivity analysis 1 obtained by changing the LHV of CH₄ about
 414 ± 2.5 %. The second sensitivity analysis was performed changing the price of CH₄ in the range of ± 20 %. The
 415 sensitivity analysis was carried out on net revenues before 5 years of amortisation.

416

417 **Conclusions**

418 The aim of the present study was the evaluation of the environmental sustainability through Life Cycle
 419 Assessment (LCA) and economic profitability through Life Cycle Costing (LCC) of the 18 AD configurations
 420 carried out on OFMSW at three S:I ratio (1:2, 1:1 and 2:1) for three different inoculum incubation times (0, 5
 421 and 10 d). The adopted approach was the eco-efficiency perspective, coming from the combination of

422 technical, environmental (LCA) and economic (LCC) perspectives. From environmental perspective:
423 increasing both the S:I ratio and the inoculum incubation time (5 and 10 days) the environmental impacts
424 decreased, since higher amount of OFMSW was valorised and specific production of biogas with higher
425 methane content was achieved. The lowest values of Climate change were achieved by T10_3_WAS and
426 T10_3_CAS: 28.67 and 27.72 kgCO₂ eq, respectively. LCC was developed to evaluate the economic
427 profitability of the 18 AD configurations tested. The minimum AD plant size for which all the 18 AD
428 configurations were profitable after 5 year of amortisation was 30,000 t/y of OFMSW. Capital and operational
429 costs decreased by increasing the incubation time of the inoculum and the S:I ratio, since a higher specific
430 biogas rate was reached, and smaller AD bio-reactor volume was adopted since HRT decreased. The AD plant
431 size, for which maximal revenues and minimal capital and operational costs were evaluated, was 50,000 t/y
432 OFMSW. To conclude, the AD configurations which reached both the environmental sustainability and
433 economic profitability were: the AD performed both with inoculum WAS and CAS incubated for 5 and 10 d
434 at the highest S:I ratio 2:1: T5_3_WAS, T5_3_CAS, T10_3_WAS and T10_3_CAS.

435

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440

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Dear Editor,

We kindly ask you to consider the submission of our manuscript entitled “*Life cycle assessment and life cycle costing of advanced anaerobic digestion of organic fraction municipal solid waste*” for publication in the **CHEMOSPHERE**, Elsevier.

The present study evaluated environmental sustainability and economic profitability of optimised anaerobic digestion of organic fraction municipal solid waste (OFMSW) supplied by a real OFMSW treatment plant, to produce methane.

The aim of this study is the evaluation of the environmental sustainability by means of Life Cycle Assessment (LCA) and economic profitability through Life Cycle Costing (LCC) of the 18 AD configurations carried out on Organic Fraction Municipal Solid Waste (OFMSW) at three S:I ratios (1:2, 1:1 and 2:1) for three different inoculum incubation times (0, 5 and 10 d). The adopted approach was the eco-efficiency perspective, coming from the combination of technical, environmental (LCA) and economic (LCC) perspectives. We believe that these results can be of great significance to any readership and make a profound resonance on hot topics such as OFMSW valorisation, through anaerobic digestion and biogas production, considering as fundamental pillar the sustainability. LCA and LCC are performed through SimaPro software. Sensitivity analysis is performed both for environmental and economic assessment to prove the robustness of the results.

I declare that this work is linked to a work presented at THESSALONIKI 2021 8th International Conference on Sustainable Solid Waste Management, and it has been selected for the special issue “Recent Advancements in Anaerobic Digestion” of Chemosphere.

Yours sincerely, on behalf of all the authors,
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